



**MADE EASY**

India's Best Institute for IES, GATE & PSUs

Important Questions  
for **GATE 2022**

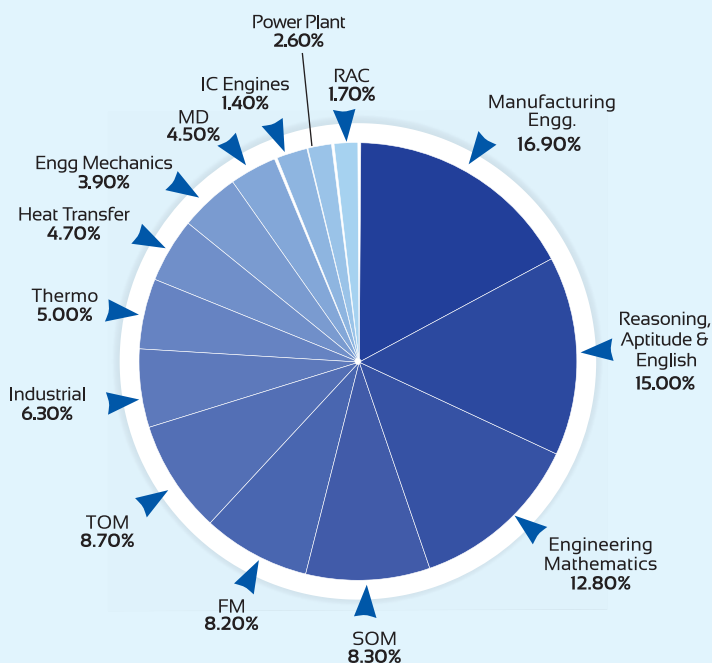
**MECHANICAL  
ENGINEERING**

**Day 7 of 8**

**Q.151 - Q.175 (Out of 200 Questions)**

**Thermodynamics + Engg.  
Mechanics + Industrial Engg.**

**SUBJECT-WISE WEIGHTAGE ANALYSIS OF GATE SYLLABUS**



Subject	Average % (last 5 yrs)
Manufacturing Engineering	16.90%
Reasoning, Aptitude & English	15.00%
Engineering Mathematics	12.80%
Strength of Materials	8.30%
Theory of Machines	8.70%
Fluid Mechanics & Hydraulic Machines	8.20%
Industrial Engineering	6.30%
Thermodynamics	5.00%
Heat Transfer	4.70%
Engineering Mechanics	3.90%
Machine Design	4.50%
Internal Combustion Engines	1.40%
Power Plant Engineering	2.60%
Refrigeration & Air Conditioning	1.70%
<b>Total</b>	<b>100%</b>

### Thermodynamics + Engg. Mechanics + Industrial Engg.

**Q.151** The specific internal energy of a certain fluid is related as follows:

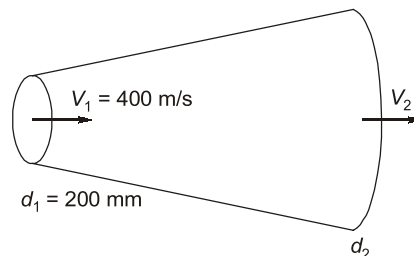
$$u = 196 + 0.718T \text{ kJ/kg}$$

where  $T$  is in  $^{\circ}\text{C}$ .

A system composed of 2 kg of the this fluid expands in a frictionless piston and cylinder arrangement from an initial state of 1 MPa,  $100^{\circ}\text{C}$  to a final temperature of  $30^{\circ}\text{C}$ . If there is no heat transfer, what is the net work for the process is

- |              |                 |
|--------------|-----------------|
| (a) 140 kJ   | (b) - 100.52 kJ |
| (c) 50.26 kJ | (d) 100.52 kJ   |

**Q.152** Air flows through a supersonic adiabatic nozzle as shown in figure. The inlet conditions are 7 kPa and  $420^{\circ}\text{C}$ . The nozzle exit diameter is adjusted such that the exit velocity of air is 700 m/s. The exit diameter of the nozzle is



- |            |            |
|------------|------------|
| (a) 151 mm | (b) 175 mm |
| (c) 212 mm | (d) 230 mm |

**Q.153** Two vessels,  $A$  and  $B$ , each of volume  $3 \text{ m}^3$  are be connected together by a tube of negligible volume. Vessel  $A$  contains air at 7 bar,  $95^{\circ}\text{C}$  while vessel  $B$  contains air at 3.5 bar,  $205^{\circ}\text{C}$ . What is the final temperature of mixing air when vessel  $A$  is connected to vessel  $B$ ? Assume the mixing to be complete and adiabatic.

- |              |              |
|--------------|--------------|
| (a) 402.72 K | (b) 375.75 K |
| (c) 398.56 K | (d) 423 K    |

**Q.154** Consider the following statements:

1. The work done during isothermal process for steady flow and non-flow is the same [i.e.  $-\int v dp = \int p dv$  for isothermal process]
2. Heat transferred during polytropic process on vapour is same for flow process and non-flow process.
3. Throttling process is work producing irreversible adiabatic leading to increase in entropy of the system.
4. Universal gas constant of a perfect gas increases with increase in molecular weight.

Of these statements

- |                         |                            |
|-------------------------|----------------------------|
| (a) 1 and 2 are true    | (b) 2 and 3 are true       |
| (c) 2, 3 and 4 are true | (d) 1, 2, 3 and 4 are true |

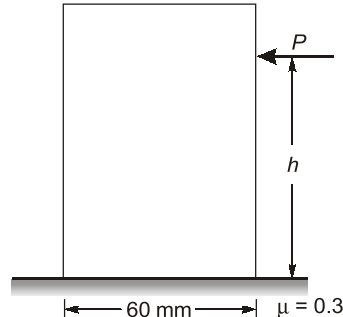


- Q.160** A body of mass 4 kg and  $C_p = 2 \text{ kJ/kgK}$  is at 500 K. If the atmospheric temperature is 250 K, the maximum work obtainable from the body till it comes to equilibrium with atmosphere is \_\_\_\_\_ kJ.
- Q.161** One kg of air is compressed polytropically from ambient condition (pressure 1 bar and temperature of 300 K) to the pressure of 8 bar and temperature of 600 K. What will be the irreversibility of the process?  
Assume,  $R = 0.287 \text{ kJ/kg}$ ,  $c_p = 1.004 \text{ kJ/kgK}$ ,  $c_v = 0.716 \text{ kJ/kgK}$ .
- (a) 6.43 kJ/kg (b) 12.86 kJ/kg  
(c) 8.43 kJ/kg (d) 10.45 kJ/kg
- Q.162** A system is initially at 1200 K and a thermal reservoir at 300 K is available. What will be the maximum amount of work that can be recovered as the system is cooled down to the temperature of the reservoir?  
[Heat capacity of the system at constant volume,  $C_v = 0.05 T^2 \text{ J/K}^3$ ]
- (a) 18.23 MJ (b) 18.23 kJ  
(c) 36.21 kJ (d) 58.215 J
- Q.163** Air initially at 1 bar, 300 K and occupying a volume of  $0.18 \text{ m}^3$  undergoes two processes. The air is compressed isothermally until the volume is halved and then undergoes a constant pressure process until the volume is halved again. Assuming ideal gas behaviour, what will be the total work (in kJ) for the two processes?
- (a) 51.25 (b) 86.50  
(c) 21.47 (d) 42.46
- Q.164** Dry saturated steam enters a frictionless adiabatic nozzle with negligible velocity at a temperature of  $300^\circ\text{C}$ . It is expanded to a pressure of 5 MPa. The exit velocity of steam will be  
Relevant steam table extract is given below

Saturated Temperature ( $^\circ\text{C}$ )	Saturated Pressure (MPa)	Enthalpy (kJ/kg)		Entropy (kJ/kg $^\circ\text{C}$ )		Specific Volume ( $\text{m}^3/\text{kg}$ )	
		$h_f$	$h_g$	$S_f$	$S_g$	$V_f$	$V_g$
300	8.6	1345	2751	3.2552	5.7081	0.0014	0.0216
263.91	5	1154.5	2794.2	2.9206	5.9735	0.0012	0.0394

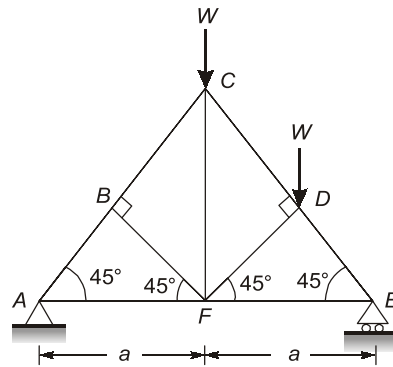
- (a) 445.7 m/s (b) 842.8 m/s  
(c) 941.5 m/s (d) 245.5 m/s

**Q.165** A block is of width 60 mm and weight  $W$ . A force  $P$  is applied to block at height  $h$ . Coefficient of friction between block and floor is 0.3. Upto what height  $h$  force can be applied so that the block slips without tipping?



- (a) 120 mm  
(b) 110 mm  
(c) 105 mm  
(d) 95 mm

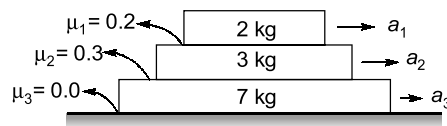
**Q.166** A truss  $ABCDEF$  carries vertical loads  $W$  each at joints  $C$  and  $D$ . The magnitude and nature of force in member  $AB$  is



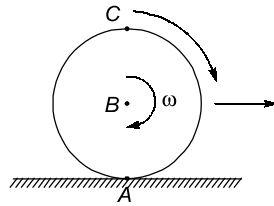
- (a)  $1.06W$  (Compressive)  
(b)  $0.53W$  (Tensile)  
(c)  $0.75W$  (Compressive)  
(d)  $0.75W$  (Tensile)

**Q.167** The acceleration  $a_1, a_2, a_3$  of the three blocks if a horizontal force of 10 N is applied on 2 kg block will be

- (a)  $a_1 = 3\text{m/s}^2, a_2 = 0, a_3 = 0.$   
(b)  $a_1 = 3\text{m/s}^2, a_2 = 0, a_3 = 0.57\text{ms}^2$   
(c)  $a_1 = 3\text{m/s}^2, a_2 = a_3 = 0.4\text{m/s}^2.$   
(d)  $a_1 = 1.5\text{m/s}^2, a_2 = 1.57, a_3 = 0\text{ms}^2.$



**Q.168** A sphere is rolling without slipping on a fixed horizontal plane surface. In the figure, A is the point of contact, B is the centre of the sphere and C is its topmost point. Then



- (a)  $\vec{V}_C - \vec{V}_A = 2(\vec{V}_B - \vec{V}_C)$                       (b)  $\vec{V}_C - \vec{V}_B = \vec{V}_B - \vec{V}_A$   
 (c)  $2|\vec{V}_C - \vec{V}_A| = 2|\vec{V}_B - \vec{V}_C|$                       (d)  $|\vec{V}_C - \vec{V}_A| = 4|\vec{V}_B|$

**Q.169** A man is standing on a straight bridge over a river and another man is on a boat in the river just below the man on the bridge. If the first man starts walking at the uniform speed of 4 m/min and the boat moves perpendicularly to the bridge at the speed of 5 m/min then the rate at which the boat and man are separating after 4 minutes is \_\_\_\_\_ m/min. [Assume the height of bridge over the boat is 3 m] [Correct upto 2 decimal places]

**Q.170** A news paper boy buys paper for 60 paise each and sells them for ₹ 1.40 each, he cannot return unsold newspaper. Daily demand has the following distribution

Number of customer	Probability
23	0.01
24	0.03
25	0.06
26	0.10
27	0.20
28	0.25
29	0.15
30	0.10
31	0.05
32	0.05

If each day's demand is independent of previous day's, the number of papers ordered each day is \_\_\_\_\_.

**Q.171** A job shop has received an order consisting of 4 different jobs :

Job name	A	B	C	D
Milling Machine	12	8	6	7
Drilling Machine	10	12	14	9

What are the percentage utilization of milling and drilling machines?

- (a) 64.71%, 88.24%                      (b) 88.24%, 64.71%  
 (c) 85.46%, 75.63%                      (d) 93.45%, 67.75%



### Multiple Select Questions (MSQ)

**Q.174** Which of the following statement(s) is/are correct?

- (a) A linear programming problem with three variables and two constraints can be solved by graphical method.
- (b) For solutions of a linear programming problem with mixed constraints, Big-M method can be employed.
- (c) In the solution process of a linear programming problem using Big-M-method, when an artificial variable leaves the basic, the column of the artificial variable can be removed from all subsequent tables.
- (d) All of the above

**Q.175** A company has four warehouses and six stores. The warehouses altogether have a surplus of 22 units of a given commodity, divided among them as follows:

<b>Warehouse</b>	<b>1</b>	<b>2</b>	<b>3</b>	<b>4</b>
<b>Surplus</b>	<b>5</b>	<b>6</b>	<b>2</b>	<b>9</b>

The six stores altogether need 22 units the commodity. Individual requirements at stores 1, 2, 3, 4, 5 and 6 are 4, 4, 6, 2, 4 and 2 units respectively.

If  $x_{ij}$  represents the number of units of commodity to be shipped from warehouse to store, then which of the following are correct?

- (a)  $\sum_{j=1}^5 x_{1j} = 5, \sum_{j=1}^6 x_{2j} = 6, \sum_{j=1}^6 x_{3j} = 2$  and  $\sum_{j=1}^6 x_{4j} = 9$
- (b)  $\sum_{j=1}^5 x_{1j} = 4, \sum_{j=1}^6 x_{2j} = 4, \sum_{j=1}^6 x_{3j} = 6, \sum_{j=1}^6 x_{4j} = 2, \sum_{j=1}^6 x_{5j} = 4, \sum_{j=1}^6 x_{6j} = 2$
- (c)  $\sum_{i=1}^4 x_{i1} = 4, \sum_{i=1}^4 x_{i2} = 4, \sum_{i=1}^4 x_{i3} = 6, \sum_{i=1}^4 x_{i4} = 2, \sum_{i=1}^5 x_{i5} = 4, \sum_{i=1}^6 x_{i6} = 2$
- (d)  $\sum_{i=1}^4 x_{i1} = 5, \sum_{i=1}^4 x_{i2} = 6, \sum_{i=1}^4 x_{i3} = 2, \sum_{i=1}^4 x_{i4} = 9$

■■■■



### Detailed Explanations

151. (d)

Given data:

$$u = 196 + 0.718T \text{ kJ/kg}$$

$$m = 2 \text{ kg}$$

$$P_1 = 1 \text{ MPa} = 1000 \text{ kPa}$$

$$T_1 = 100^\circ\text{C}$$

$$T_2 = 30^\circ\text{C}$$

$$Q = 0$$

Using first law of thermodynamics for the process,

$$Q = dU + W$$

$$0 = m(u_2 - u_1) + W$$

or  $-W = m(u_2 - u_1)$

$$= 2(196 + 0.718T_2 - 196 - 0.718T_1)$$

$$= 2 \times 0.718(T_2 - T_1)$$

$$= 2 \times 0.718 \times (30 - 100)$$

$$-W = -100.52 \text{ kJ}$$

or  $W = 100.52 \text{ kJ}$

152. (c)

Given data:

$$P_1 = 7 \text{ kPa}$$

$$T_1 = 420^\circ\text{C} = 693 \text{ K}$$

$$V_1 = 400 \text{ m/s}$$

$$V_2 = 700 \text{ m/s}$$

$$d_1 = 200 \text{ mm} = 0.2 \text{ m}$$

Applying steady flow energy equation,

$$\frac{V_1^2}{2} + c_p T_1 = \frac{V_2^2}{2} + c_p T_2$$

$$\frac{(400)^2}{2} + 1005 \times 693 = \frac{(700)^2}{2} + 1005 \times T_2$$

$$80000 + 696465 = 245000 + 1005 T_2$$

$$T_2 = 528.82 \text{ K}$$

or  $P_1 = \rho_1 R T_1$

$$7 = \rho_1 \times 0.287 \times 693$$

or  $\rho_1 = 0.03519 \text{ kg/m}^3$

$$\rho_2 = \rho_1 \left( \frac{T_2}{T_1} \right)^{\frac{1}{\gamma-1}} = 0.03519 \times \left( \frac{528.82}{693} \right)^{\frac{1}{1.4-1}} = 0.0179 \text{ kg/m}^3$$

Applying continuity equation,

$$\rho_1 A_1 V_1 = \rho_2 A_2 V_2$$

$$\rho_1 \times \frac{\pi}{4} d_1^2 V_1 = \rho_2 \times \frac{\pi}{4} d_2^2 \times V_2$$

or  $\rho_1 d_1^2 V_1 = \rho_2 d_2^2 V_2$

$$0.03519 \times (0.2)^2 \times 400 = 0.0179 \times d_2^2 \times 700$$

or  $d_2^2 = 0.04493$

or  $d_2 = 0.21196 \text{ m} = 211.96 \text{ mm}$   
 $\approx 212 \text{ mm}$

153. (c)

Given data:

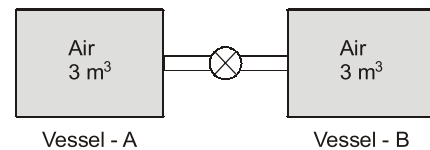
$$V_A = V_B = 3 \text{ m}^3$$

$$p_A = 7 \text{ bar} = 700 \text{ kPa}$$

$$T_A = 95^\circ\text{C} = 368 \text{ K}$$

$$p_B = 3.5 \text{ bar} = 350 \text{ kPa}$$

$$T_B = 205^\circ\text{C} = 478 \text{ K}$$



Mass of air in vessel A is given by

$$m_A = \frac{p_A V_A}{RT_A} = \frac{700 \times 3}{0.287 \times 368} = 19.88 \text{ kg}$$

Mass of air in vessel B is given by

$$m_B = \frac{p_B V_B}{RT_B} = \frac{350 \times 3}{0.287 \times 478} = 7.65 \text{ kg}$$

Since mixing is adiabatic,

Internal energy before mixing = Internal energy after mixing

$$m_A c_v T_A + m_B c_v T_B = (m_A + m_B) c_v T_f$$

where  $T_f$  = Final temperature

or 
$$T_f = \frac{m_A T_A + m_B T_B}{m_A + m_B} = \frac{19.88 \times 368 + 7.65 \times 478}{19.88 + 7.65} = 398.56 \text{ K}$$

154. (a)

155. (a)

Given data:

$$V = 1 \text{ m}^3$$

$$T_1 = 50^\circ\text{C} = 323 \text{ K}$$

$$p_1 = 2 \text{ MPa} = 2000 \text{ kPa}$$

$$m_2 = 0.5 m_1$$

$$p_1 V = m_1 R T_1$$

$$2000 \times 1 = m_1 \times 0.287 \times 323$$

or

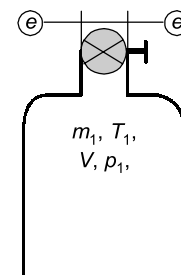
$$m_1 = 21.57 \text{ kg}$$

$$m_2 = 0.5 \times 21.57 = 10.78 \text{ kg}$$

$$m_e = m_1 - m_2 = 21.57 - 10.78 = 10.78 \text{ kg}$$

Applying unsteady flow energy equation,

$$\frac{dU}{dt} = m_i h_i + Q - m_e h_e - W_{cv}$$



where

$$Q = 0 \quad (\because \text{adiabatic process})$$

$$W_{cv} = 0 \quad (\because \text{constant volume})$$

$$m_i = 0 \quad (\because \text{no inlet})$$

$$\frac{dU}{dt} = \frac{dm}{dt} \times h_e$$

$$c_v \left\{ T \frac{dm}{dt} + m \frac{dT}{dt} \right\} = \frac{dm}{dt} \times c_p \times T$$

$$T \frac{dm}{dt} + m \frac{dT}{dt} = \frac{dm}{dt} \times \gamma T$$

$$m \frac{dT}{dt} = \frac{dm}{dt} \times (\gamma - 1) T$$

$$\int \frac{dT}{T} = \int \left( \frac{dm}{m} \right) \times (\gamma - 1)$$

$$\ln \frac{T_2}{T_1} = (\gamma - 1) \ln \frac{m_2}{m_1}$$

$$\ln \frac{T_2}{323} = 0.4 \ln \frac{1}{2}$$

$$T_2 = 244.788 \text{ K}$$

$$p_2 = \frac{m_2 R T_2}{V_2} = \frac{10.78 \times 0.287 \times 244.788}{1} = 757.339 \text{ kPa}$$

156. (b)

157. (44.03)(43.50 to 44.50)

Given data:

At inlet:

$$p_1 = 700 \text{ kPa}$$

$$T_1 = 65^\circ\text{C} = 338 \text{ K}$$

$$V_1 = 90 \text{ m/s}$$

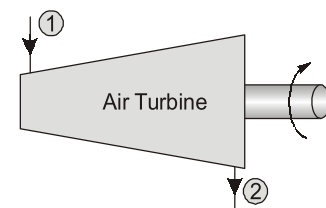
At exit:

$$p_2 = 140 \text{ kPa}$$

$$T_2 = 5^\circ\text{C} = 278 \text{ K}$$

$$V_2 = 60 \text{ m/s}$$

$$T_o = 25^\circ\text{C} = 298 \text{ K}$$



Maximum work:

$$w_{\max} = (h_1 - h_2) - T_o (s_1 - s_2) + \frac{V_1^2 - V_2^2}{2}$$

$$= c_p (T_1 - T_2) - T_o \left( c_p \log_e \frac{T_1}{T_2} - R \log_e \frac{p_1}{p_2} \right) + \frac{V_1^2 - V_2^2}{2000}$$

$$= 1.005(338 - 278) - 298 \left( 1.005 \log_e \frac{338}{278} - 0.287 \log_e \frac{700}{140} \right) + \frac{(90)^2 - (60)^2}{2000}$$

$$= 60 - 298(0.1964 - 0.4619) + 2.25 = 141.36 \text{ kJ/kg}$$

Actual work:  $w = (h_1 - h_2) + \frac{V_1^2 - V_2^2}{2}$

$$= 60 + 2.25 = 62.25 \text{ kJ/kg}$$

Second law efficiency,

$$\eta_{II} = \frac{w}{w_{\max}} = \frac{62.25}{141.36} = 0.4403 = 44.03 \%$$

158. (2443.248) (2443.10 to 2443.45)

At 25°C,  $\frac{dp_s}{dT_s} = 0.189 \text{ kPa/K}$

Specific volume of saturated vapour,

$$v_s = 43.38 \text{ m}^3/\text{kg}$$

From Clausius-Clapeyron equation neglecting specific volume of liquid

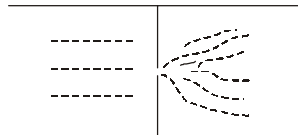
$$\frac{dp_s}{dT_s} = \frac{h_{fg}}{T_s \times v_s}$$

$h_{fg}$  = Enthalpy of vaporization

$$0.189 = \frac{h_{fg}}{(25 + 273) \times 43.38}$$

$$\therefore h_{fg} = 2443.248 \text{ kJ/kg}$$

159. (162.253) (161 to 163)



$$I = T_o (\Delta S)_{\text{uni}}$$

$$= 298 \{s_2 - s_1\} = 298 \left\{ 1.005 \ln \frac{T_2}{T_1} - 0.287 \ln \frac{1.2}{8} \right\}$$

Since it is a free expansion process therefore the temperature will remain constant, therefore  $T_2 = T_1$

$$\therefore I = -298 \times 0.287 \ln \frac{1.2}{8}$$

$$I = 162.253 \text{ kJ}$$

160. (613.70) (613 to 614)

$$\begin{aligned} \text{Maximum work} &= \Psi_1 - \Psi_o = (H - T_o S)_1 - (H - T_o S)_o \\ &= H_1 - H_o - T_o (S_1 - S_o) \end{aligned}$$

$$= 4 \times 2 \times (500 - 250) - 250 \left[ 4 \times 2 \times \ln \left( \frac{500}{250} \right) \right]$$

$$= 2000 - 1386.294$$

$$\therefore \Psi_1 - \Psi_o = 613.705 \text{ kJ}$$

161. (b)

$$W_{max} = (u_1 - u_2) - T_o(s_1 - s_2)$$

$$= c_v(T_1 - T_2) - T_o \left( c_p \ln \frac{T_1}{T_2} - R \ln \frac{P_1}{P_2} \right)$$

$$= 0.716(300 - 600) - 300 \left[ 1.004 \ln \frac{300}{600} - 0.287 \ln \frac{1}{8} \right]$$

$$= -185.06 \text{ kJ/kg}$$

$$\frac{T_2}{T_1} = \left( \frac{P_2}{P_1} \right)^{\frac{n-1}{n}}$$

$$\Rightarrow \frac{n-1}{n} = \frac{\ln \left( \frac{T_2}{T_1} \right)}{\ln \left( \frac{P_2}{P_1} \right)} = \frac{\ln 2}{\ln 8} = 0.333$$

$$\Rightarrow n = 1.5$$

$$W_{actual} = \frac{mR(T_1 - T_2)}{n-1} = \frac{1 \times 0.287(300 - 600)}{1.5 - 1} = -172.2 \text{ kJ/kg}$$

$$\begin{aligned} \text{Irreversibility, } I &= W_{max} - W_{actual} \\ &= 185.06 - 172.2 = 12.86 \text{ kJ/kg} \end{aligned}$$

162. (a)

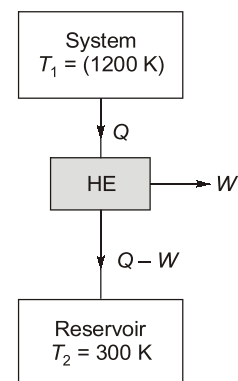
$$\text{Heat removed from the system, } Q_1 = \int_{T_1}^{T_2} C_v dT = \int_{1200}^{300} (0.05 T^2) dT$$

$$= 0.05 \left[ \frac{T^3}{3} \right]_{1200}^{300} = -28.35 \times 10^6 \text{ J}$$

$$(\Delta s)_{\text{system}} = \int_{1200}^{300} \frac{C_v \cdot dT}{T} = \int_{1200}^{300} (0.05 \times T^2) \frac{dT}{T}$$

$$= 0.05 \int_{1200}^{300} T dT = 0.05 \left[ \frac{T^2}{2} \right]_{1200}^{300} = -33750 \text{ J/K}$$

$$(\Delta s)_{\text{reservoir}} = \frac{Q_1 - W}{T_{\text{Reservoir}}} = \frac{28.35 \times 10^6 - W}{300} \text{ J/K}$$



$$(\Delta s)_{\text{working fluid in HE}} = 0$$

$$(\Delta s)_{\text{universe}} = (\Delta s)_{\text{system}} + (\Delta s)_{\text{reservoir}}$$

For maximum work,  $(\Delta s)_{\text{universe}} = 0$

$$\Rightarrow 0 = -33750 + \frac{28.35 \times 10^6 - W}{300}$$

$$\Rightarrow W = 18.225 \times 10^6 \text{ J} = 18.23 \text{ MJ}$$

163. (c)

$$P_1 = 1 \text{ bar}$$

$$T_1 = 300 \text{ K}$$

$$V_1 = 0.18 \text{ m}^3$$

$$V_2 = 0.09 \text{ m}^3$$

$$V_3 = 0.045 \text{ m}^3$$

$$m = \frac{P_1 V_1}{RT_1} = \frac{1 \times 10^5 \times 0.18}{287 \times 300} = 0.209 \text{ kg}$$

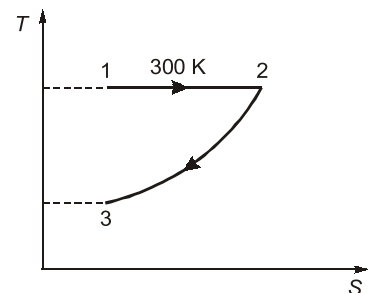
$$P_2 = \frac{P_1 V_1}{V_2} = 2P_1 = 2 \times 1 = 2 \text{ bar}$$

$$W_{1-3} = W_{1-2} + W_{2-3}$$

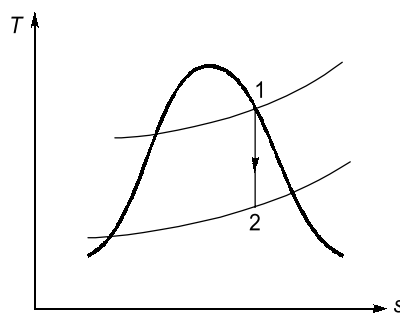
$$= \int_{V_1}^{V_2} p dv + \int_{V_2}^{V_3} p dv = mRT_1 \ln \frac{V_2}{V_1} + P_2 (V_3 - V_2)$$

$$= 0.209 \times 287 \times 300 \times \ln \frac{0.09}{0.18} + 2 \times 10^5 (0.045 - 0.09)$$

$$= -21476.6 \text{ J} = -21.476 \text{ kJ}$$



164. (a)



$$h_1 = 2751 \text{ kJ/kg}$$

$$s_1 = 5.7081 \text{ kJ/kg}$$

Let the dryness fraction at state '2' is  $x_2$ .

$$s_1 = s_2 = s_f + x_2 (s_{g2} - s_f)$$

$$\Rightarrow x_2 = \frac{S_1 - S_{f2}}{S_{g2} - S_{f2}} = \frac{5.7081 - 2.9206}{5.9735 - 2.9206} = 0.913$$

$$h_2 = h_{f_2} + x_2(h_{g_2} - h_{f_2})$$

$$h_2 = 1154.5 + 0.913(2794.2 - 1154.5) = 2651.65 \text{ kJ/kg.}$$

$$V = 44.72\sqrt{(h_1 - h_2)} = 44.72\sqrt{(2751 - 2651.65)} = 445.7 \text{ m/s}$$

165. (d)

For no tipping or prevent overturning

$$Ph < \frac{Wb}{2}$$

where

$W \rightarrow$  weight of block

and

$b \rightarrow$  width of block

$$h < \frac{Wb}{2P}$$

...(1)

and for slipping without tipping

$$P > f(\text{force of friction})$$

$$P > \mu W$$

...(2)

From (1) and (2)  $h < \frac{b}{2\mu}$

$$\therefore h < \frac{60}{0.6}$$

$$\therefore h < 100 \text{ mm}$$

Option (d) is correct.

166. (a)

Let Reaction at A be  $R_A$

Taking moments about point E,

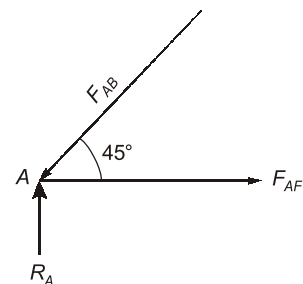
$$W \times \frac{a}{2} + Wa = 2a \cdot R_A$$

$$\therefore R_A = 0.75 W$$

For equilibrium of joint A,

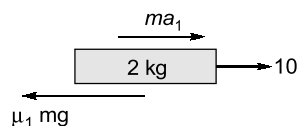
$$F_{AB} \sin 45^\circ = R_A$$

$$F_{AB} = 1.06 W \text{ (compressive)}$$



167. (c)

Drawing free body diagram of upper block,

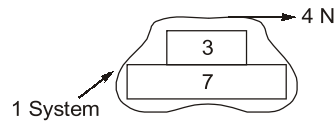


$$10 - \mu_1 mg = m a_1$$

$$10 - 0.2 \times 2 \times 10 = 2 \times a_1$$

$$a_1 = 3 \text{ ms}^{-2}$$

For the 3 kg block, as frictional reaction from 2 kg will act towards right, the 3 kg and 7 kg block will move simultaneously, since the 7 kg block is in contact with zero friction surface. There will be no tendency of relative motion between 3 kg and 7 kg and both will move as a same system due to the action of frictional force acting on the top of 3 kg by the 2 kg block



$$4 = 10a$$

$$a = 0.4$$

$$a_2 = 0.4 \text{ ms}^{-2}$$

$$a_3 = 0.4 \text{ ms}^{-2}$$

168. (b)

Let  $V$  be the linear velocity and  $\omega$  is the angular velocity.

$$\vec{V}_C = V + R\omega$$

For pure rolling,  $V = R\omega$

$$\vec{V}_C = 2V\hat{i}$$

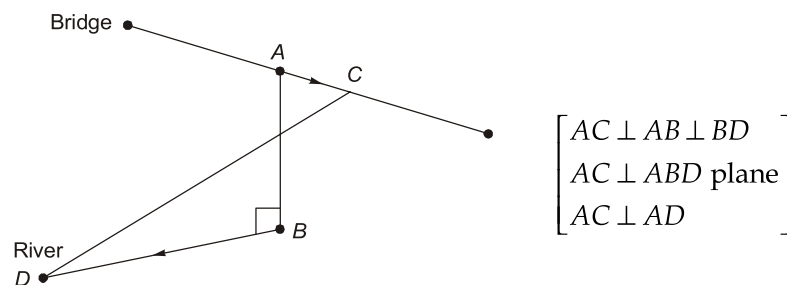
$$\therefore \vec{V}_B = V\hat{i}$$

$$\vec{V}_A = 0$$

$$\Rightarrow \vec{V}_C - \vec{V}_B = 2V\hat{i} - V\hat{i} = V\hat{i}$$

$$\vec{V}_B - \vec{V}_A = V\hat{i} - 0\hat{i} = V\hat{i}$$

169. (6.36) (6.30 to 6.40)



Initially man was at A and boat was at B. After  $t$  minutes, man is at C and boat is at D.

$$AC = 4t, \quad BD = 5t$$

$$AB = 3 \text{ m}$$

$$DA = \sqrt{AB^2 + BD^2} = \sqrt{3^2 + (5t)^2} = \sqrt{9 + 25t^2}$$



$$DC = \sqrt{AD^2 + AC^2} = \sqrt{9 + 25t^2 + (4t)^2} = \sqrt{9 + 41t^2}$$

Let the distance between boat and man is

$$x = DC = \sqrt{9 + 41t^2}$$

$$\frac{dx}{dt} = \frac{1}{2\sqrt{9 + 41t^2}} \times 41 \times 2t$$

At  $t = 4$  min

$$\frac{dx}{dt} = \frac{41 \times 2 \times 4}{2\sqrt{9 + 41 \times 4^2}} = 6.36 \text{ m/min}$$

170. (28) (28 to 28)

$$p(S-1) < \left( \frac{P}{P+L} \right) \leq p(S)$$

$p(S-1)$  = Cumulative probability of the demand for  $(S-1)$  units.

$p(S)$  = Cumulative probability of the demand for  $S$  units.

$P$  = profit /unit

$L$  = loss/unit.

$$\frac{P}{P+L} = \frac{0.8}{0.6+0.8} = 0.57$$

Number of customer	Probability	Cumulative Probability
23	0.01	0.01
24	0.03	0.04
25	0.06	0.10
26	0.10	0.20
27	0.20	0.40
28	0.25	0.65
29	0.15	0.80
30	0.10	0.90
31	0.05	0.95
32	0.05	1.00

Since  $\frac{P}{P+L} = 0.57$  lies between 0.40 and 0.65.

Hence, optimal number of newspaper to be ordered is 28.

171. (a)

According to Johnson rule, the correct order will be

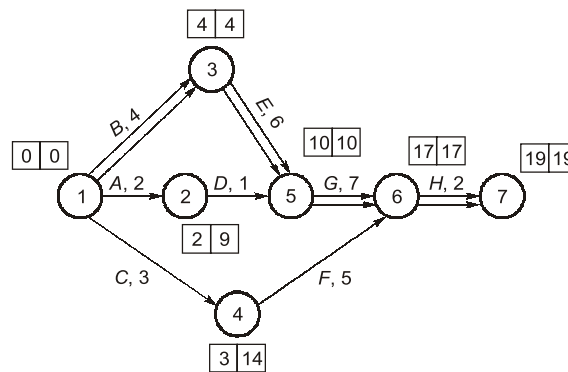
C - D - B - A

	0	6	13	21	33
Milling					
Drilling					
		6	20	29	41

$$\text{Utilisation of milling machine} = \frac{33}{51} \times 100 = 64.71\%$$

$$\text{Utilisation of drilling machine} = \frac{45}{51} \times 100 = 88.24\%$$

172. (c)



Critical path : B - E - G - H

Critical path duration = 19 days

$$\text{Variance} = \left( \frac{t_p - t_0}{6} \right)^2$$

Activity	$t_0$	$t_m$	$t_p$	Variance
B	1	4	7	1
E	2	5	14	4
G	3	6	15	4
H	1	2	3	0.11

The variance along critical path = 1 + 4 + 4 + 0.11 = 9.11

173. (15) (15 to 15)

Rate of breakdown of machines =  $\lambda = 3/\text{hour}$ , Idle time cost of machine = ₹ 16/hour

**Fast repairman**

$$\text{Rate of repair} = \mu = \frac{1}{10} \times 60/\text{hour} = 6/\text{hour}$$

$$\text{Average number of breakdown machines in the system} = \frac{\lambda}{\mu - \lambda} = 1$$

Machine hours lost in 8 hour day = 1 × 8 = 8 hours

$$\begin{aligned} \text{Total cost per day} &= \text{Cost of idle machines} + \text{repairman charges} \\ &= ₹(16 \times 8 + 10 \times 8) = ₹208 \end{aligned}$$

$$\Rightarrow \text{Slow repairman's cost} = ₹448$$

**Slow repairman**

$$\text{Slow repairman's daily working charges} = ₹ 8 \times 8 = ₹ 64$$

$$\text{Cost of idle machines} = ₹ 448 - ₹ 64 = ₹ 384$$

$$\text{Number of idle machines a day} \times \text{cost of idle machine} = ₹ 384$$

$$\text{Number of idle machines a day} \times ₹ 16 = ₹ 384$$

$$\text{Number of idle machines a day} = \frac{384}{16} = 24$$

$$\text{Number of idle machines an hour} = \frac{24}{8} = 3$$

Average number of breakdown machines in the system

$$= \frac{\lambda}{\mu - \lambda} = \frac{3}{\mu - 3} = 3$$

$$\Rightarrow \mu = 4/\text{hour}$$

Times taken to repair a machine = 15 minutes

174. (b, c)

A LPP with 3 variables and 2 constraints cannot be solved by graphical method.

175. (a, c)

Since  $x_{1j}$  represents quantity shipped from warehouse to store

The transportation problem is:

$C_1$	$C_2$	$C_3$	$C_4$	$C_5$	$C_6$	5
$C_7$	$C_8$	$C_9$	$C_{10}$	$C_{11}$	$C_{12}$	6
$C_{13}$	$C_{14}$	$C_{15}$	$C_{16}$	$C_{17}$	$C_{18}$	2
$C_{19}$	$C_{20}$	$C_{21}$	$C_{22}$	$C_{23}$	$C_{24}$	9
4	4	6	2	4	2	

where  $c_1, c_2, \dots, c_{24}$  = unit costs of transportation

$$\Rightarrow \sum_{j=1}^6 x_{1j} = 5 \quad \text{and so on}$$

$$\text{and} \quad \sum_{i=1}^4 x_{i1} = 4 \quad \text{and so on}$$

Option (a) and (c) are correct.

■■■■