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Leading Institute for ESE, GATE & PSUs

# ESE 2026 : Mains Test Series

UPSC ENGINEERING SERVICES EXAMINATION

## Mechanical Engineering

Test-1 : Thermodynamics [All Topics]

IC Engine + Refrigeration and Air-conditioning [All Topics]

Name : .....

Roll No :

Test Centres	Student's Signature
Delhi <input type="checkbox"/> Bhopal <input type="checkbox"/> Jaipur <input type="checkbox"/> Pune <input type="checkbox"/> Hyderabad <input checked="" type="checkbox"/>	

### Instructions for Candidates

1. Do furnish the appropriate details in the answer sheet (viz. Name & Roll No).
2. There are Eight questions divided in TWO sections.
3. Candidate has to attempt FIVE questions in all in English only.
4. Question no. 1 and 5 are compulsory and out of the remaining THREE are to be attempted choosing at least ONE question from each section.
5. Use only black/blue pen.
6. The space limit for every part of the question is specified in this Question Cum Answer Booklet. Candidate should write the answer in the space provided.
7. Any page or portion of the page left blank in the Question Cum Answer Booklet must be clearly struck off.
8. There are few rough work sheets at the end of this booklet. Strike off these pages after completion of the examination.

### FOR OFFICE USE

Question No.	Marks Obtained
Section-A	
Q.1	37
Q.2	—
Q.3	—
Q.4	25
Section-B	
Q.5	19
Q.6	40
Q.7	—
Q.8	37
<b>Total Marks Obtained</b>	<b>158</b>

Signature of Evaluator

Cross Checked by

## IMPORTANT INSTRUCTIONS

CANDIDATES SHOULD READ THE UNDERMENTIONED INSTRUCTIONS CAREFULLY. VIOLATION OF ANY OF THE INSTRUCTIONS MAY LEAD TO PENALTY.

### DONT'S

1. Do not write your name or registration number anywhere inside this Question-cum-Answer Booklet (QCAB).
2. Do not write anything other than the actual answers to the questions anywhere inside your QCAB.
3. Do not tear off any leaves from your QCAB, if you find any page missing do not fail to notify the supervisor/invigilator.
4. Do not leave behind your QCAB on your table unattended, it should be handed over to the invigilator after conclusion of the exam.

### DO'S

1. Read the Instructions on the cover page and strictly follow them.
2. Write your registration number and other particulars, in the space provided on the cover of QCAB.
3. Write legibly and neatly.
4. For rough notes or calculation, the last two blank pages of this booklet should be used. The rough notes should be crossed through afterwards.
5. If you wish to cancel any work, draw your pen through it or write "Cancelled" across it, otherwise it may be evaluated.
6. Handover your QCAB personally to the invigilator before leaving the examination hall.

## Section A : Thermodynamics

- Q.1 (a) (i) A turbo compressor delivers  $3.5 \text{ m}^3/\text{s}$  of air at  $0.5 \text{ MPa}$ ,  $50^\circ\text{C}$ . The air is then heated at a constant pressure of  $0.5 \text{ MPa}$  to  $450^\circ\text{C}$  in a heater and finally expanded in a turbine which delivers  $2 \text{ MW}$ . During expansion, there is a heat transfer of  $0.05 \text{ MJ/s}$  to the surroundings. Calculate the turbine exhaust temperature if changes in kinetic and potential energy in the turbine are negligible.
- (ii) The Clausius inequality forms the basis of the second law of thermodynamics and provide a criterion for the direction of heat transfer and the feasibility of thermodynamic processes.
1. State the Clausius inequality and explain its physical significance.
  2. Using Clausius inequality, drive the concept of entropy for a closed system.
  3. Discuss how the entropy change differs for reversible and irreversible processes, with suitable thermodynamic reasoning.

$$V_1 = 3.5 \text{ m}^3/\text{s}$$

[6 + 6 marks]

$$P_1 = 0.5 \text{ MPa} = P_2$$

$$T_1 = 323^\circ\text{K}, \quad T_2 = (450 + 273)^\circ\text{K}$$

$$h_2 + \dot{Q} = h_3 + W_T$$

$$C_p \times 723 - 50 = C_p \times T_3 + 2000$$

$$T_3 =$$

$$m_1 = \frac{P_1 V_1}{RT_1} = \frac{500 \times 3.5}{0.287 \times 323} = 18.877 \text{ kg/s}$$

$$H_2 + \dot{Q} = H_3 + W_T$$

$$18.877 \times 1.005 \times 723 - 50 = 18.877 \times 1.005 \times T_3$$

$$T_3 = 614.94^\circ\text{K}$$

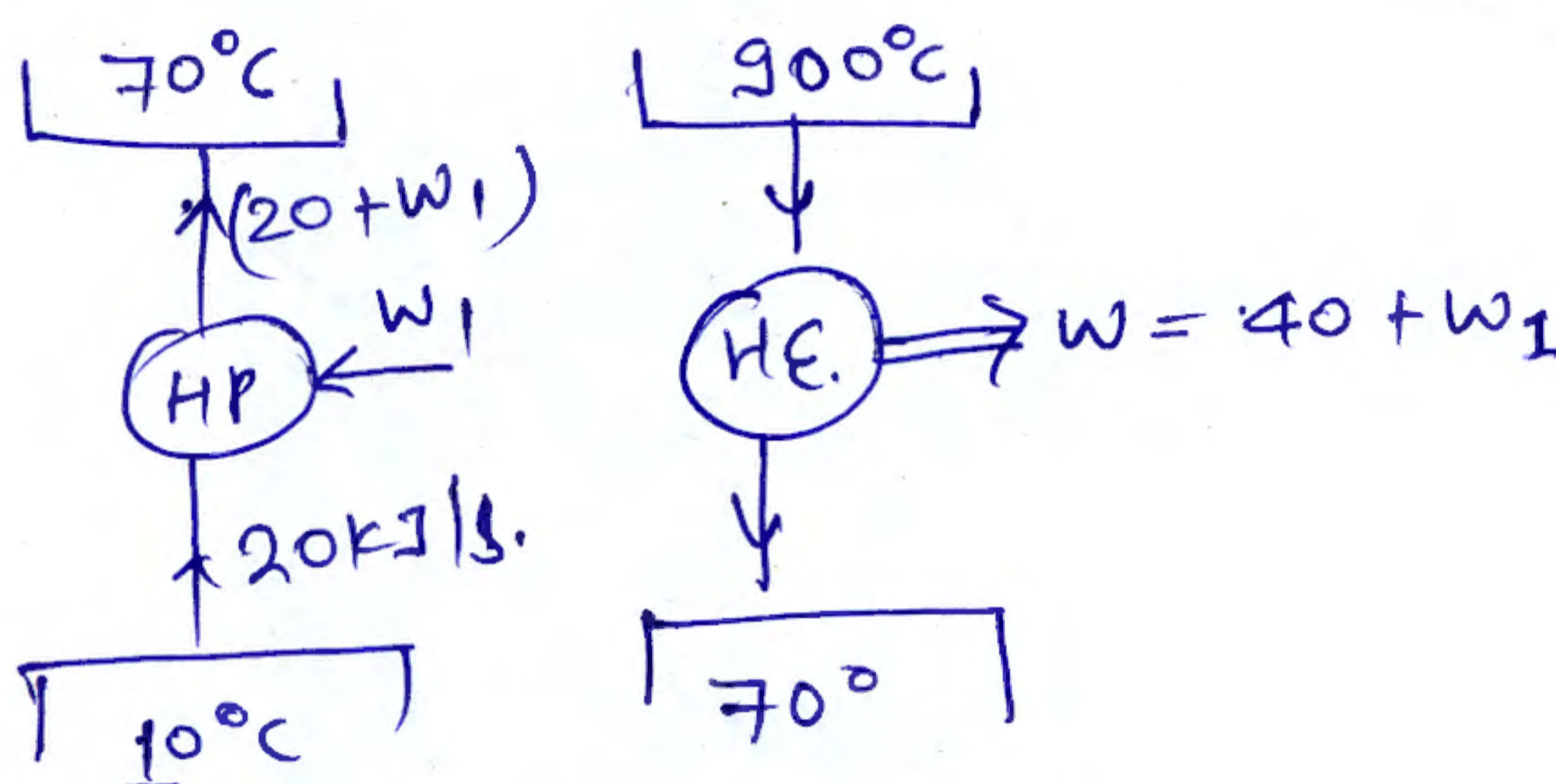
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*[Faint, illegible handwritten text and diagrams are visible in the main body of the page, possibly representing a technical drawing or a complex calculation. A prominent red curved line is drawn across the page.]*

Q.1 (b) A heat pump working on the Carnot cycle extract heat from a reservoir at  $10^{\circ}\text{C}$  and delivers heat to a reservoir at  $70^{\circ}\text{C}$ . The heat pump is driven by a reversible heat engine operating between  $900^{\circ}\text{C}$  and  $70^{\circ}\text{C}$ . The reversible heat engine also drives a machine that absorbs  $40\text{ kW}$  of work. If the heat pump extracts  $20\text{ kJ/s}$  from the  $10^{\circ}\text{C}$  reservoir, determine:

- (i) The rate of heat supply from  $900^{\circ}\text{C}$  source.  
 (ii) The rate of heat rejection to  $70^{\circ}\text{C}$  sink.

[12 marks]



$$(\text{COP})_{\text{HP}} = \frac{20}{W_1} = \frac{283}{343 - 283}$$

$$\text{Hence } W_1 = \frac{20}{\frac{283}{60}} = \frac{283}{60}$$

$$W_1 = 4.24 \text{ kW}$$

$$\text{Hence } W = 40 + 4.24$$

$$W = 44.24 \text{ kW}$$

$$\eta_{\text{HE}} = 1 - \frac{343}{273 + 900}$$

$$\frac{40 + 4.24}{Q_{\text{sup}}} = \frac{1 - \frac{343}{1173}}{1173}$$

$$Q_{\text{suppl}} = 62.52 \text{ kW}$$

$$\text{Heat Rejected}^n \text{ By engine} = 62.52 - 44.24$$

$$\text{HR engine} = 18.28 \text{ kW} \quad \underline{\text{Ans}}$$

$$H_{\text{Reject}} \text{ By Heat pump} = 20 + 4.29 \\ = 24.29 \text{ kW}$$

$$\text{Total H/R to } 70^\circ\text{C} = 24.29 + 18.28$$

$$\text{Total H.R.} = 42.52 \text{ kW}$$

12

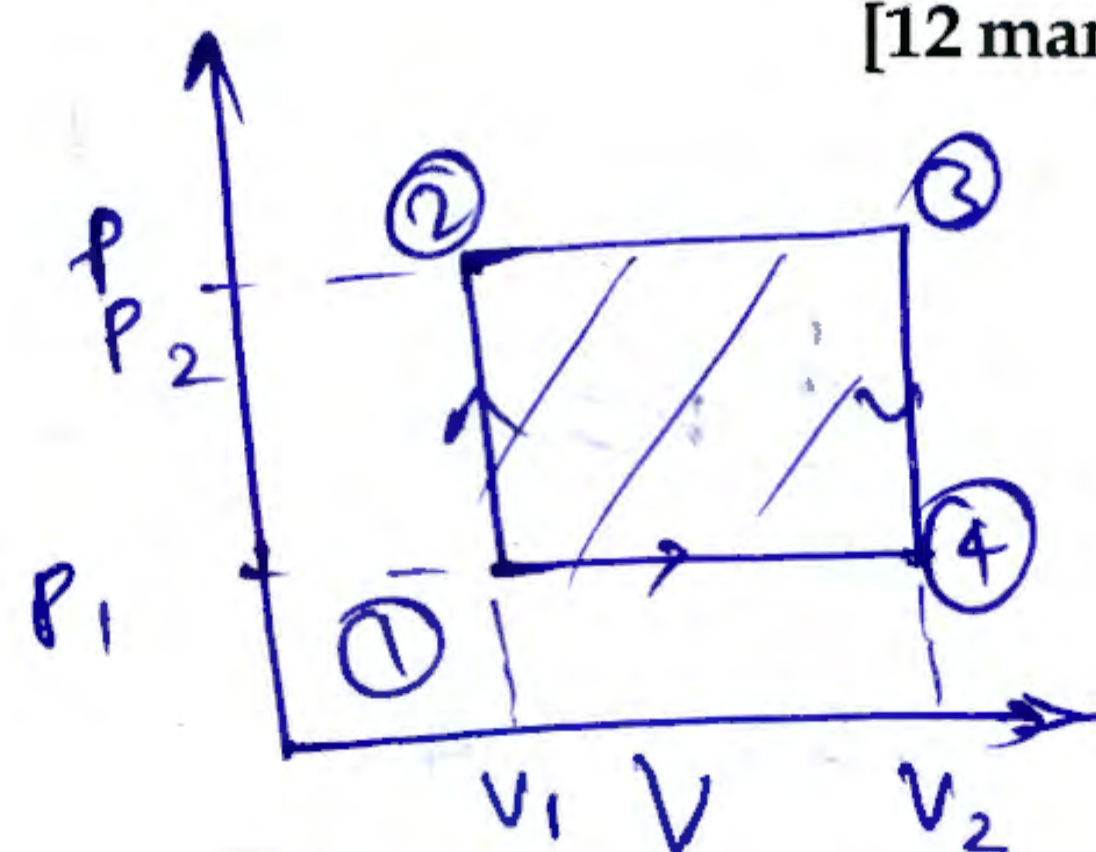
Q.1 (c) An ideal gas cycle is represented by a rectangle on a P-V diagram. If  $P_1$  and  $P_2$  are the lower and higher pressures; and  $V_1$  and  $V_2$ , be the smaller and larger volumes, respectively. Then,

- (i) Calculate the net work done per cycle.  
 (ii) Show that the thermal efficiency of the cycle is given by

$$\eta = \frac{\gamma - 1}{\frac{\gamma P_2}{P_2 - P_1} + \frac{V_1}{V_2 - V_1}} \text{ if the specific heat capacities are constant}$$

①  $w_{\text{net}} = \text{area under the curve}$   
 $= (P_2 - P_1) \times (V_2 - V_1)$

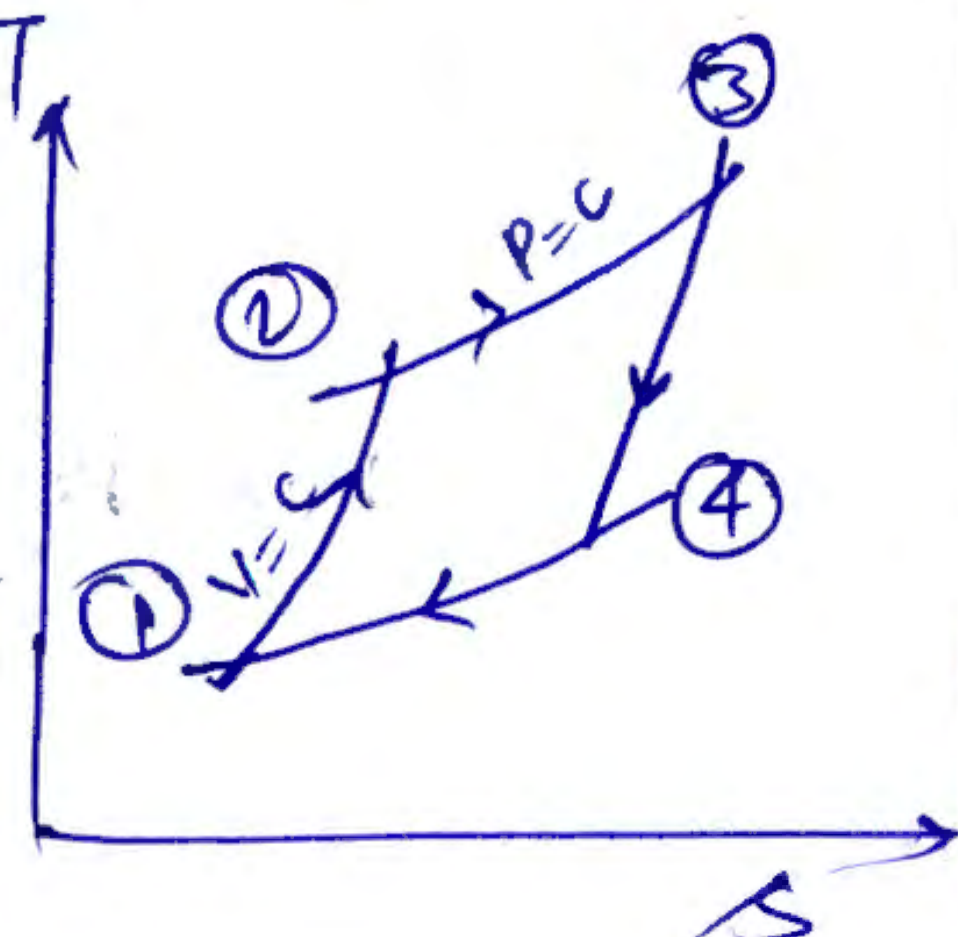
$$w_{\text{net}} = (P_2 - P_1) \times (V_2 - V_1)$$



② Thermal  $\eta = \frac{w_{\text{net}}}{Q_{\text{supplied}}}$

$$Q_{\text{sup}} = C_v(T_2 - T_1) + C_p(T_3 - T_2)$$

$$\therefore \frac{P_2}{P_1} = \frac{T_2}{T_1} \quad , \quad \frac{V_2}{V_1} = \frac{T_3}{T_2}$$



Ques ①

$$Q = \frac{(P_2 - P_1)(V_2 - V_1)}{T_1 C_V \left(\frac{T_2}{T_1} - 1\right) + T_2 C_P \left(\frac{T_3}{T_2} - 1\right)}$$

$$= \frac{(P_2 - P_1)(V_2 - V_1)}{T_1 \left(\frac{P_2}{P_1} - 1\right) + T_2 \gamma \left(\frac{V_2}{V_1} - 1\right)} \times \frac{1}{C_V}$$

$$= \frac{1}{\frac{T_1}{P_1} \times \frac{1}{(V_2 - V_1)} + \frac{T_2 \gamma}{V_1} \times \frac{1}{(P_2 - P_1)}} \times \frac{1}{C_V}$$

$$= \frac{1}{\frac{V_1}{(V_2 - V_1)} + \frac{\gamma P_2}{P_2 - P_1}} \times \frac{1}{C_V}$$

Take 1

$$\Rightarrow \frac{R}{C_V \left[ \frac{V_1}{V_2 - V_1} + \frac{\gamma P_2}{P_2 - P_1} \right]}$$

then  $C_V = R/\gamma - 1$

$$P_1 V_1 = nRT_1$$

$$R = \frac{\gamma}{\gamma - 1}$$

$$C_P - C_V = R$$

$$C_V = \frac{R}{\gamma - 1}$$

$$Q = \left( \frac{\gamma - 1}{\frac{V_1}{V_2 - V_1} + \frac{\gamma P_2}{P_2 - P_1}} \right)$$

12

- Q.1 (d) In the temperature range between  $0^{\circ}\text{C}$  and  $100^{\circ}\text{C}$  a particular thermodynamic system maintained at constant volume has a temperature dependent heat capacity given by,
- $$C_v = A + 2BT \quad [\text{where 'T' is in Kelvin (K)}]$$
- and, the constant  $A$  and  $B$  are  $0.019 \text{ J/K}$  and  $B = 5.8 \times 10^{-4} \text{ J/K}^2$
- A heat reservoir at  $5^{\circ}\text{C}$  and a reversible work source are available. What is the maximum amount of work that can be transferred to the reversible work source as the system is cooled from  $100^{\circ}\text{C}$  to the temperature of the reservoir?

[12 marks]

$$\begin{array}{ccc} 100^{\circ}\text{C} & \longrightarrow & 5^{\circ}\text{C} \\ & & \downarrow \\ \text{Max work} & = & \int m c_v dT \end{array}$$

$$w_{\text{rev}} = \int (A + 2BT) dT$$

As system of  $100^{\circ}\text{C}$  is getting cooled to  $5^{\circ}\text{C}$   
Then Heat will transfer from source to  
 $5^{\circ}\text{C}$  Heat reservoir.

Max<sup>m</sup> work can be transferred =  
- Heat transferred from source

$$= - \int_{373}^{278} (A + 2BT) dT$$

3

$$= - \int_{373}^{278} [0.019 + 2 \times 5.8 \times 10^{-4} T] dT$$

$$w_{\text{max}} = \underline{37.67 \text{ J}}$$

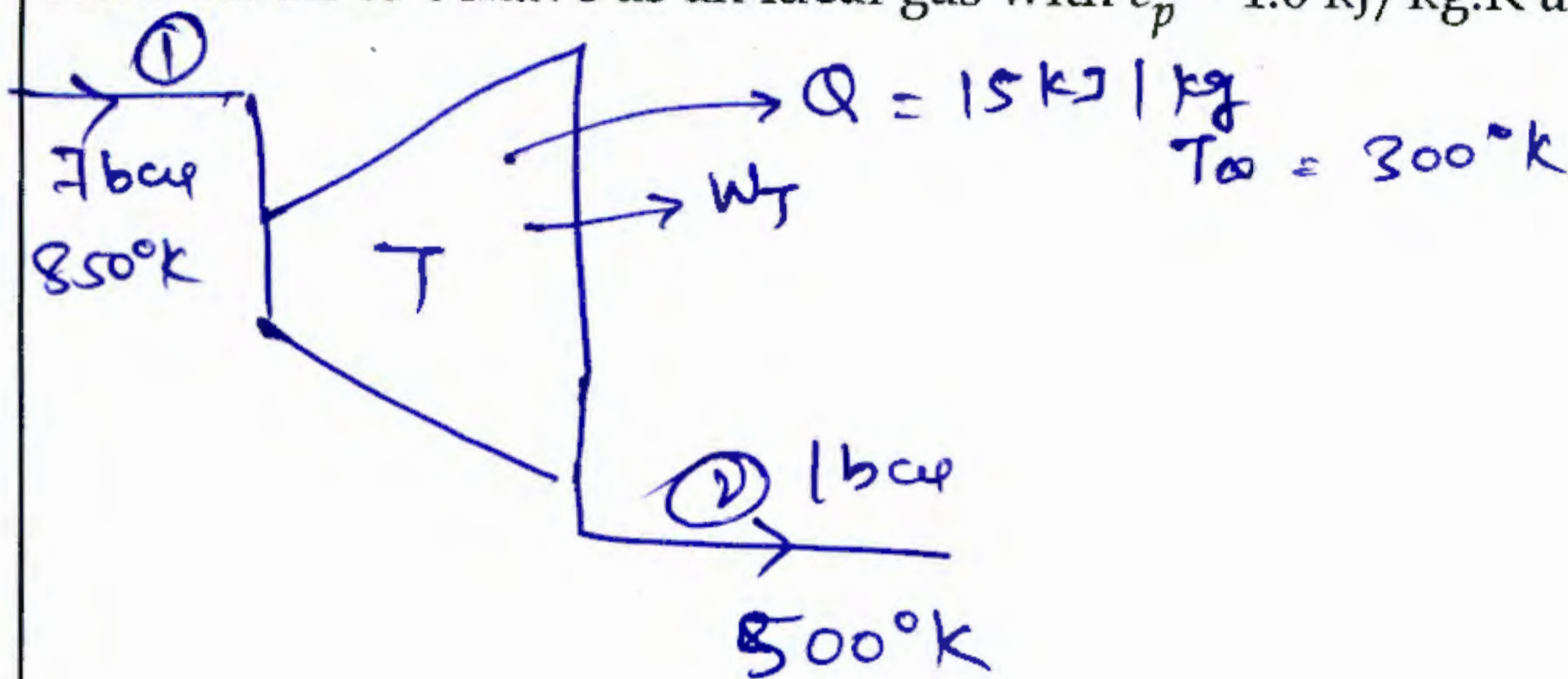
Ans

Q.1 (e) Air expands steadily through a turbine from 7 bar, 850 K to 1 bar, 500 K. During the expansion, heat transfer from air to the surroundings at 300 K is 15 kJ/kg. Neglect the change in kinetic and potential energies. Evaluate:

- (i) The irreversibility per kg air
- (ii) Actual Work
- (iii) Maximum Work

Assume air to behave as an ideal gas with  $c_p = 1.0 \text{ kJ/kg.K}$  and  $R = 0.287 \text{ kJ/kg.K}$ .

[12 marks]



$$(\Delta S)_{1-2} = c_p \ln \left( \frac{500}{850} \right) - R \ln \left( \frac{1}{7} \right)$$

$$\frac{(S_2 - S_1)}{(\Delta S)_{1-2}} = 1 \ln \left( \frac{50}{85} \right) - 0.287 \ln \left( \frac{1}{7} \right)$$

$$(\Delta S)_{1-2} = 0.02784 \text{ kJ/kg.K}$$

as entropy principle.

$$S_1 + (\Delta S)_{\text{gen}} = S_2 + \frac{15}{300}$$

$$(\Delta S)_{\text{gen}} = 0.02784 + 15/300$$

$$(\Delta S)_{\text{gen}} = 0.07784$$

$$\textcircled{1} \quad \text{Irreversibility} = \dot{I} = T_0 (\Delta S)_{\text{gen}}$$

$$= 300 \times 0.07784$$

$$\dot{I} = 23.352 \text{ kJ/kg} \quad \underline{\underline{\text{Ans}}}$$

$$\textcircled{2} \quad \text{Max}^m \text{ Actual work} = (h_1 - T_0 s_1) - (h_2 - T_0 s_2)$$

$$= (h_1 - h_2) - T_0 (s_1 - s_2)$$

$$= 1 \times (850 - 500) + T_0 (s_2 - s_1)$$

$$= 350 + 23.352$$

$$\text{Max work} = 373.352 \text{ kJ/kg} \quad \underline{\underline{\text{Ans}}}$$

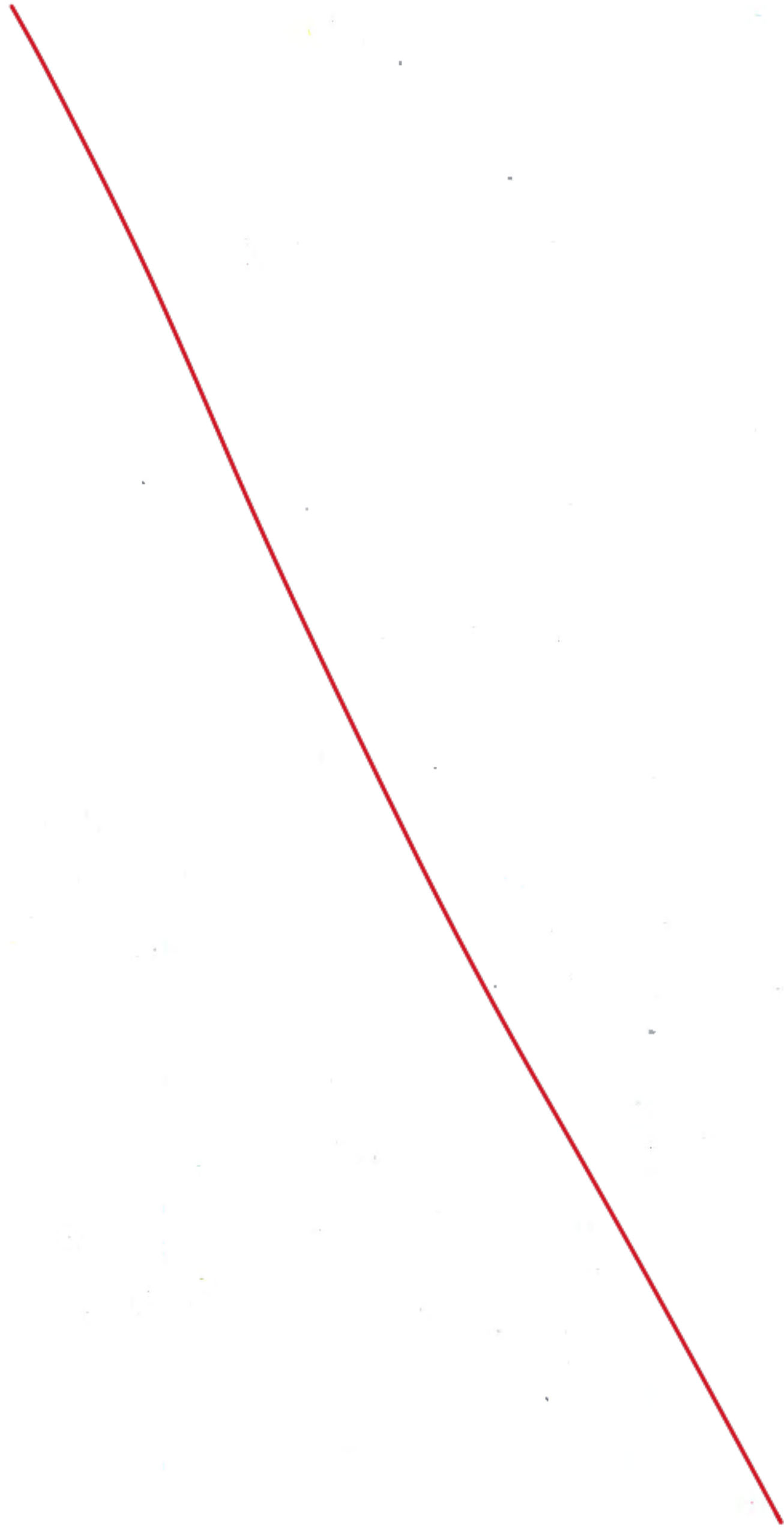
$$\begin{aligned} \text{actual work} &= h_i - h_e \\ &= 350 \text{ kJ/kg} \quad \underline{\text{Ans}} \end{aligned}$$

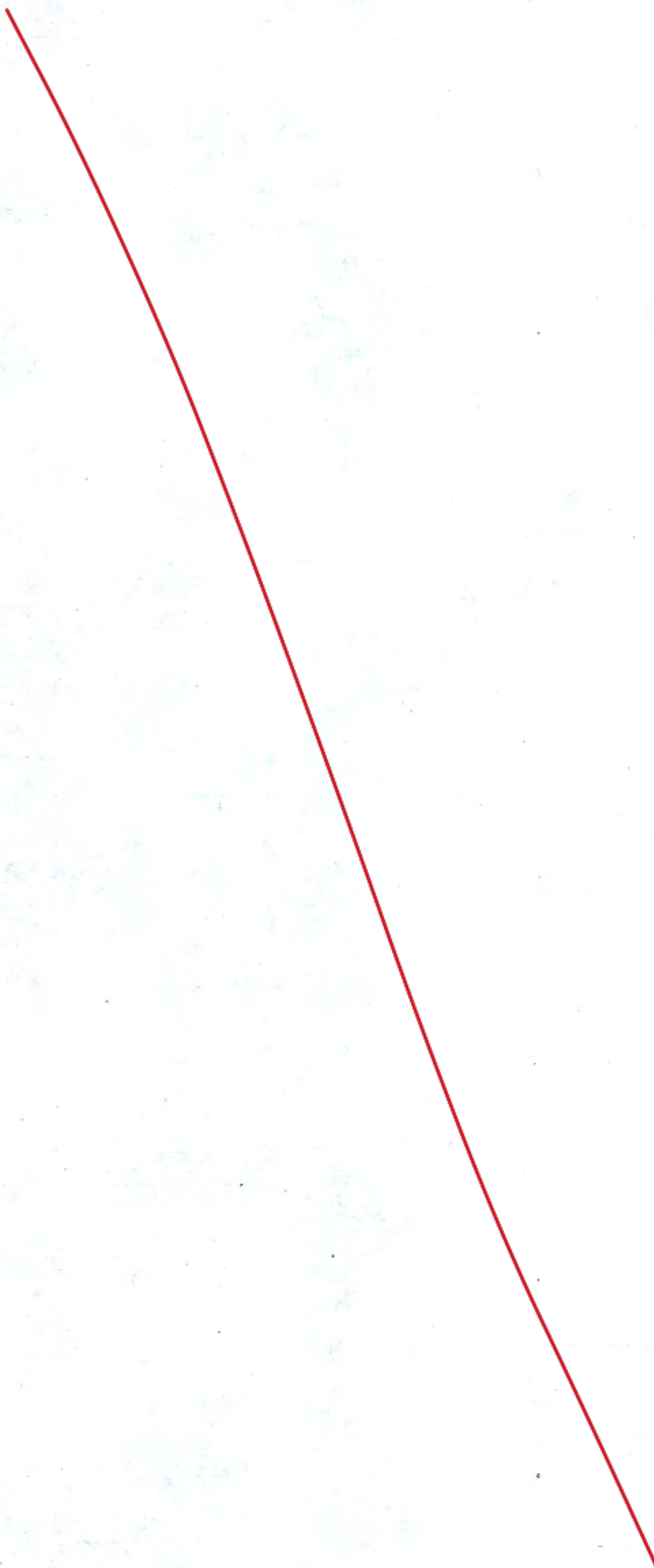
Q.2 (a) An air preheater is used to heat up the air used for combustion by cooling the outgoing products of combustion from a furnace. The rate of flow of the products is 20 kg/s and products are cooled from 400°C to 200°C and for the products at this temperature  $c_p = 1.03 \text{ kJ/kgK}$ . The rate of air flow is 18 kg/s, the inlet air temperature is 30°C and for the air  $c_p = 1005 \text{ kJ/kgK}$ .

- (i) What is initial and final availability of the products?
- (ii) What is the irreversibility for this process?
- (iii) If heat transfer from the products were to take place reversibly through heat engines, what would be the final temperature of the air? What power would be developed by heat engine?

[Take surrounding temperature,  $T_0 = 300 \text{ K}$ ]

[20 marks]



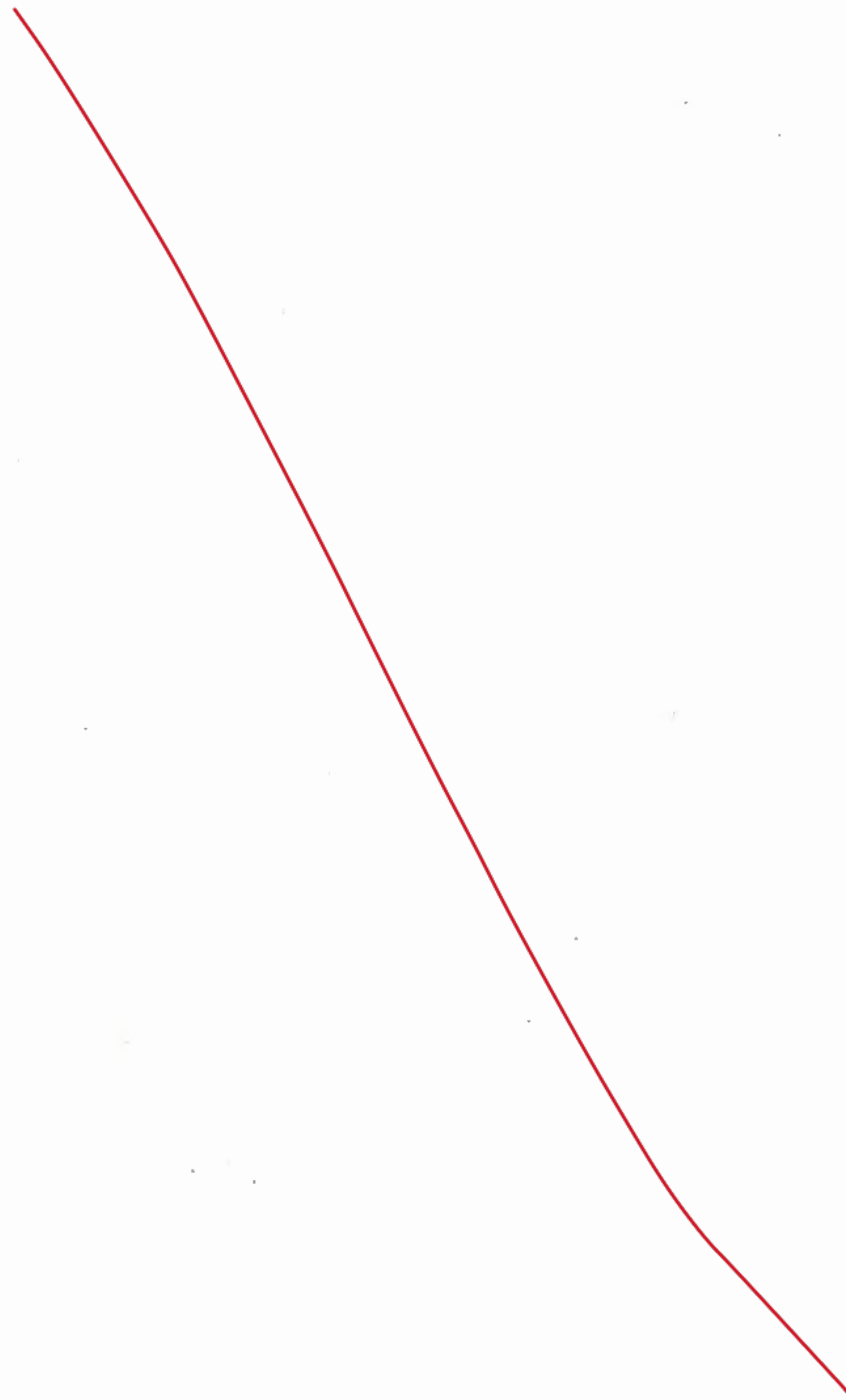


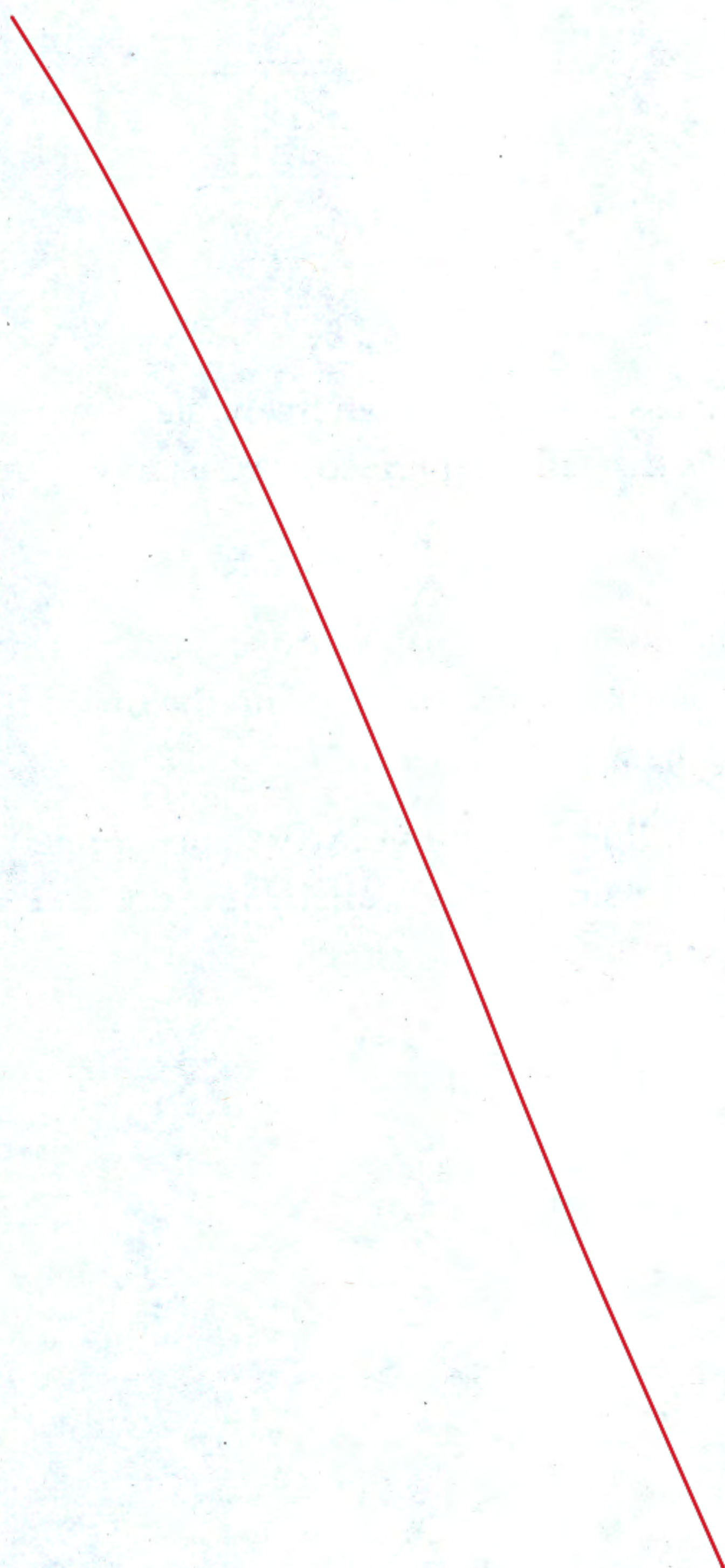
Q.2 (b) Air enters a compressor at 1 bar  $27^{\circ}\text{C}$ , which is also the state of the environment. It leaves at 4 bar,  $164^{\circ}\text{C}$  and 110 m/s. Neglecting inlet velocity and potential energy effect, determine:

- (i) Whether the compression is adiabatic or polytropic.
- (ii) If not adiabatic, the polytropic index.
- (iii) Isothermal efficiency.
- (iv) Minimum work input and irreversibility.
- (v) The second law efficiency.

[Take  $c_p$  of air =  $1.003 \text{ kJ/kgK}$ ,  $\gamma = 1.4$ ]

[20 marks]





- Q.2 (c) (i) An object of mass 20 kg falls down freely, starting from rest through a distance of 20 m. During this free fall it experiences a resistance  $F$ , due to air which is given by

$$F = \frac{V^2}{200} \text{ Newton}$$

where  $V$  is the instantaneous velocity of the object in m/s. Assuming the process to be adiabatic, find the work transfer and the final velocity of the object.

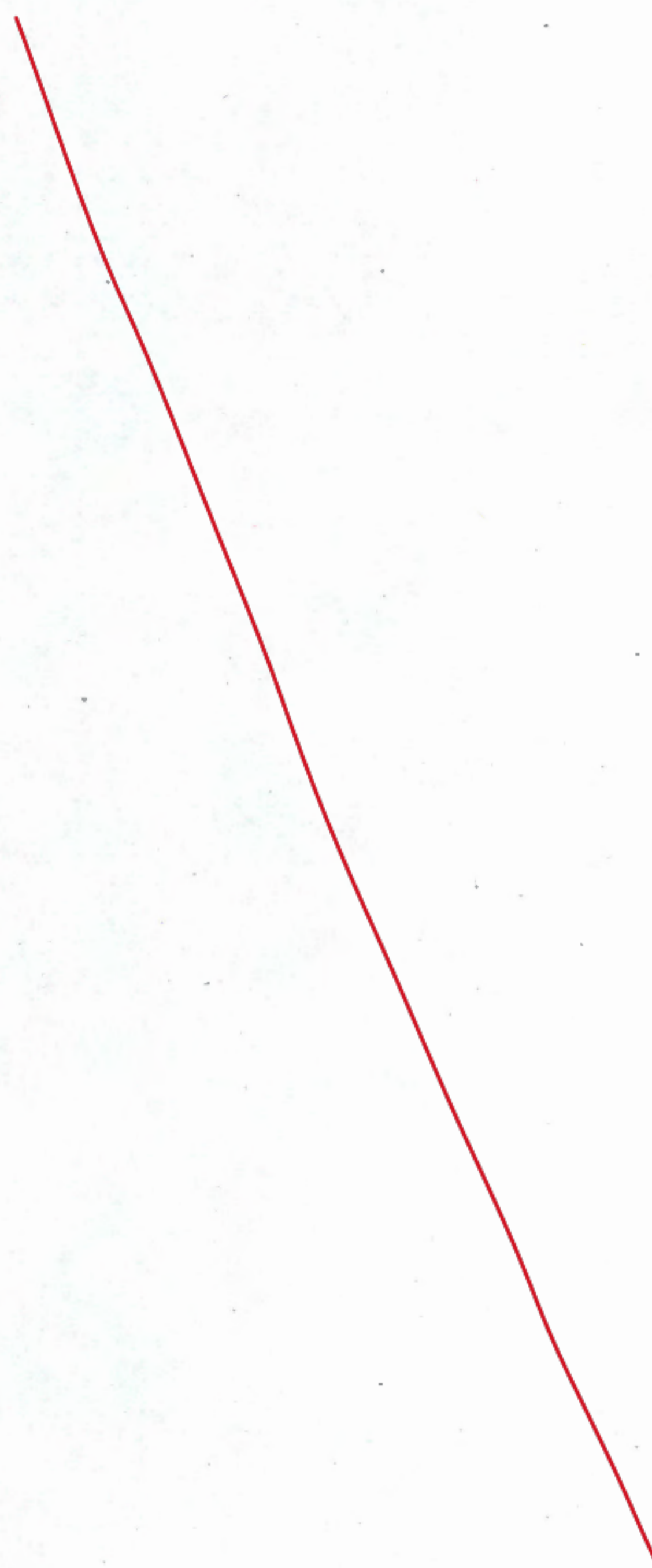
[Take  $g = 9.8 \text{ m/s}^2$ ]

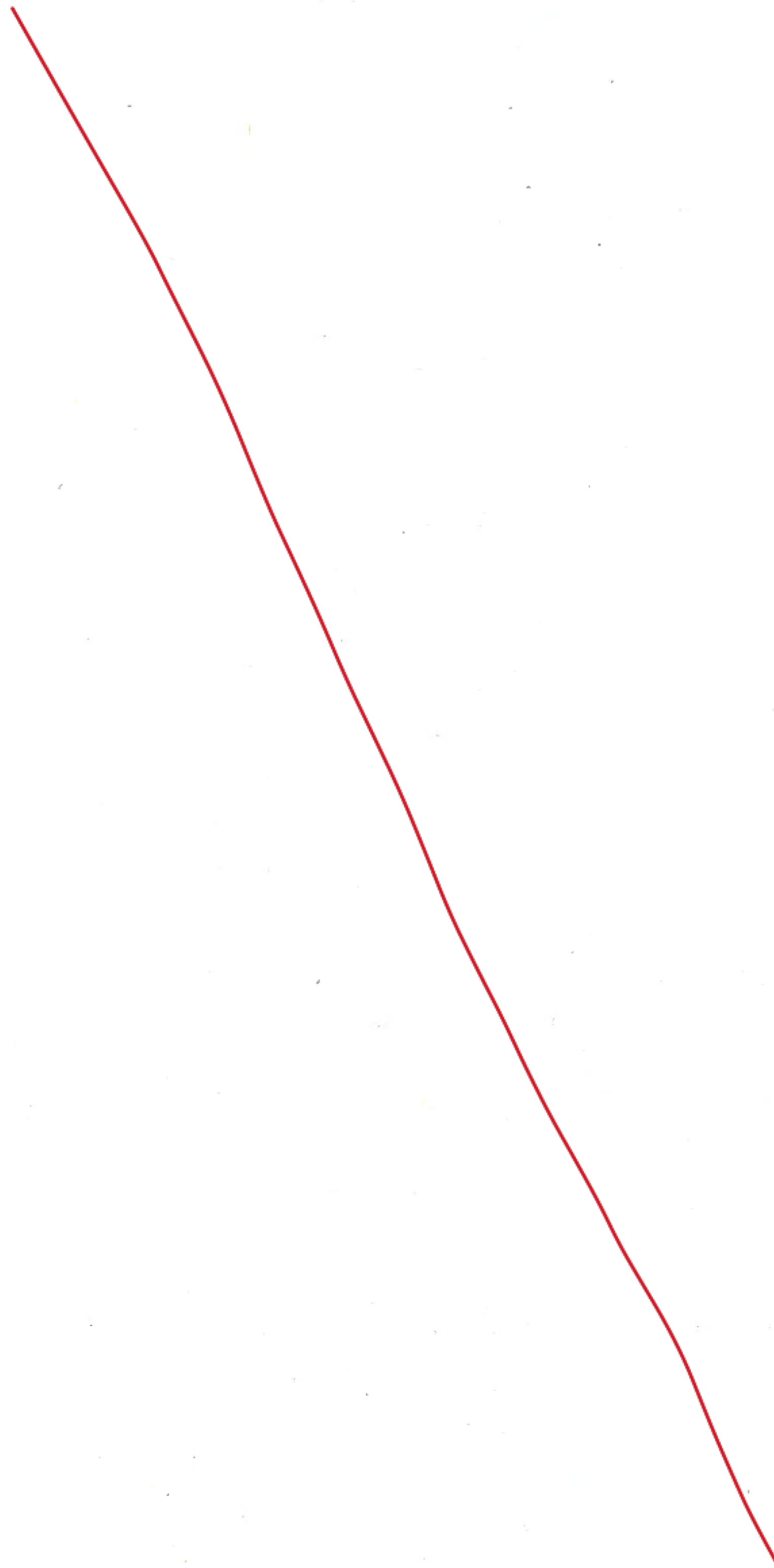
- (ii) Enumerate the different types of work encountered in thermodynamics. For each type, briefly explain its physical significance and state whether work is a point function or path function.

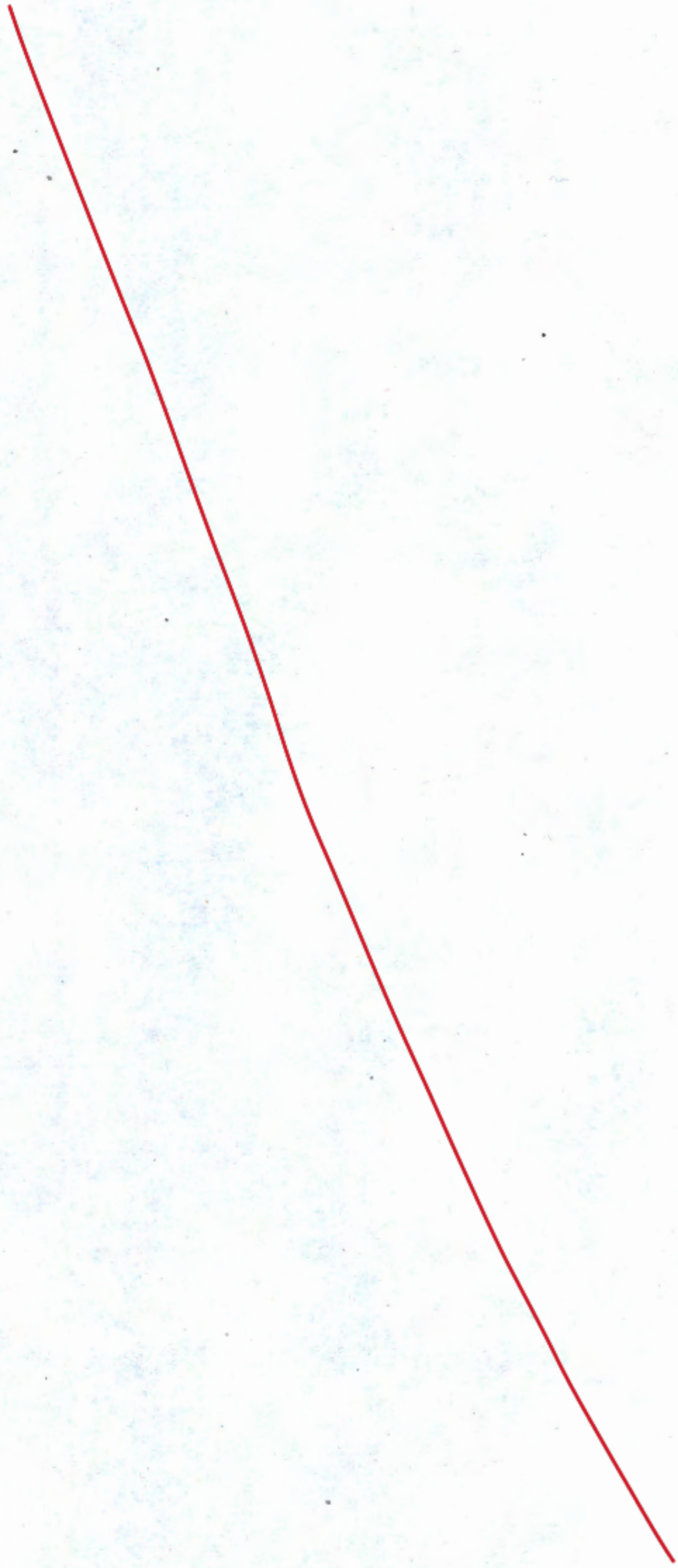
[15 + 5 marks]

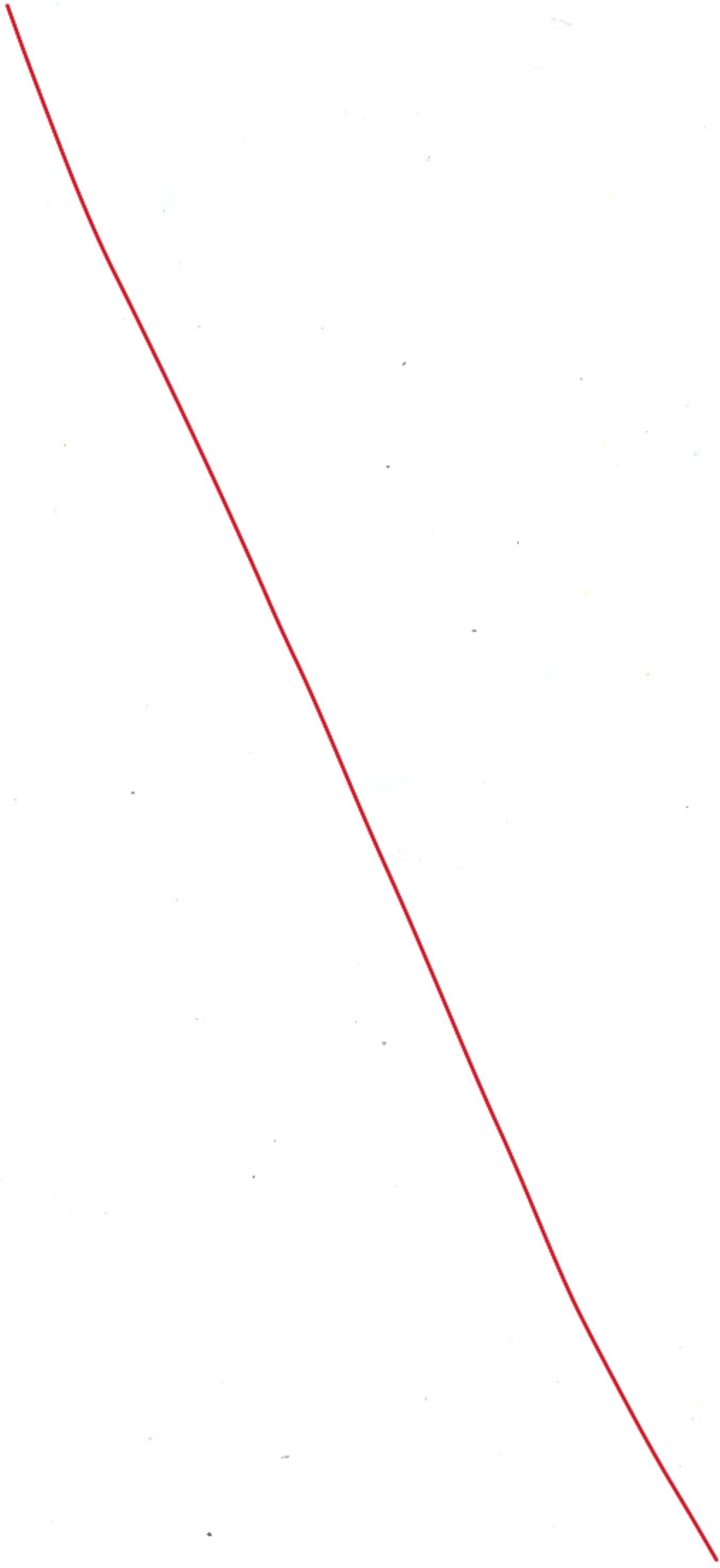
- Q.3 (a) Three identical finite bodies of constant heat capacity are at temperatures 500 K, 500 K and 200 K. If no work or heat is supplied from outside what is the highest temperature to which any one of the bodies can be raised by the operation of heat engines or refrigerators?

[20 marks]









Q.3 (b) The internal energy of air is given, at ordinary temperature by

$$u = u_0 + 0.718t$$

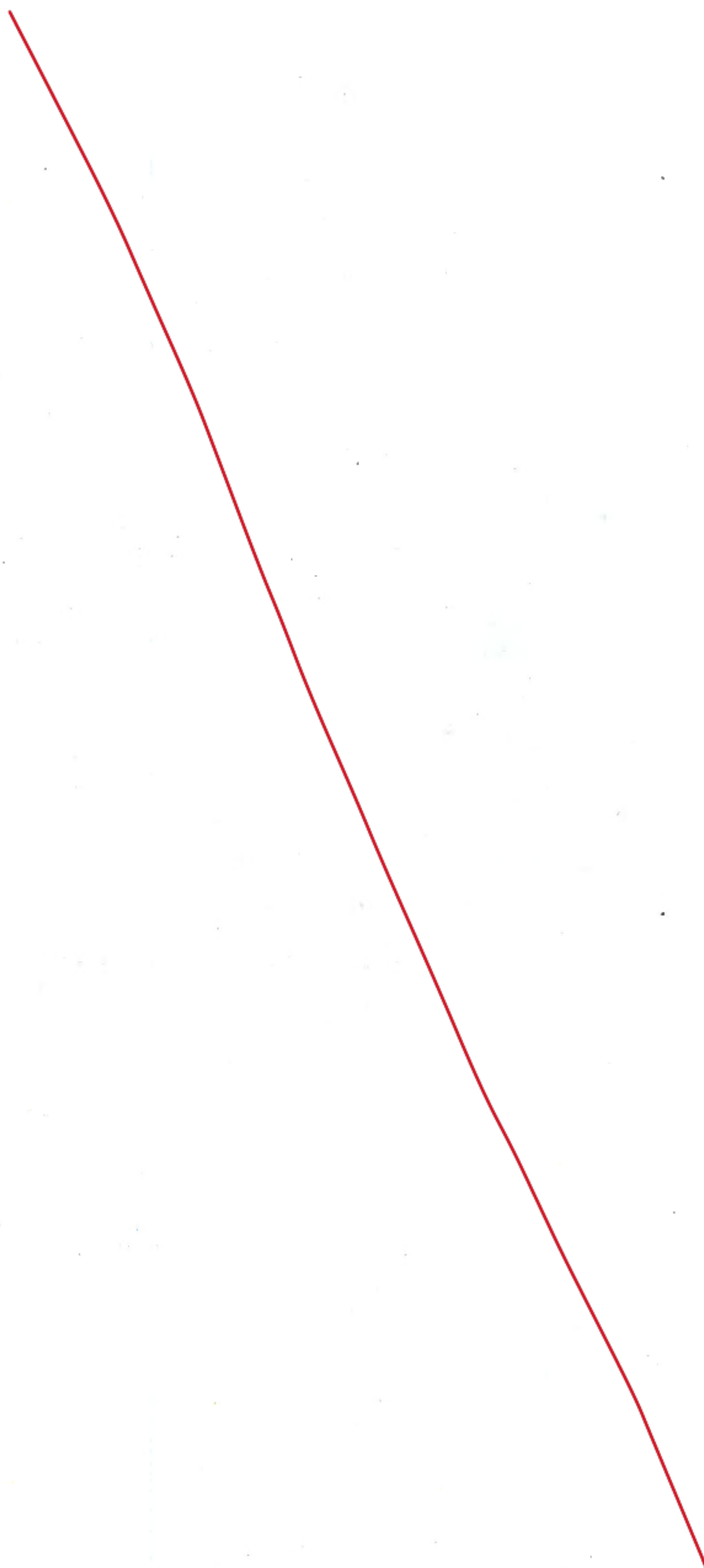
where  $u$  is in kJ/kg,  $u_0$  is any arbitrary value of  $u$  at  $0^\circ\text{C}$ , kJ/kg and  $t$  is temperature in  $^\circ\text{C}$ .

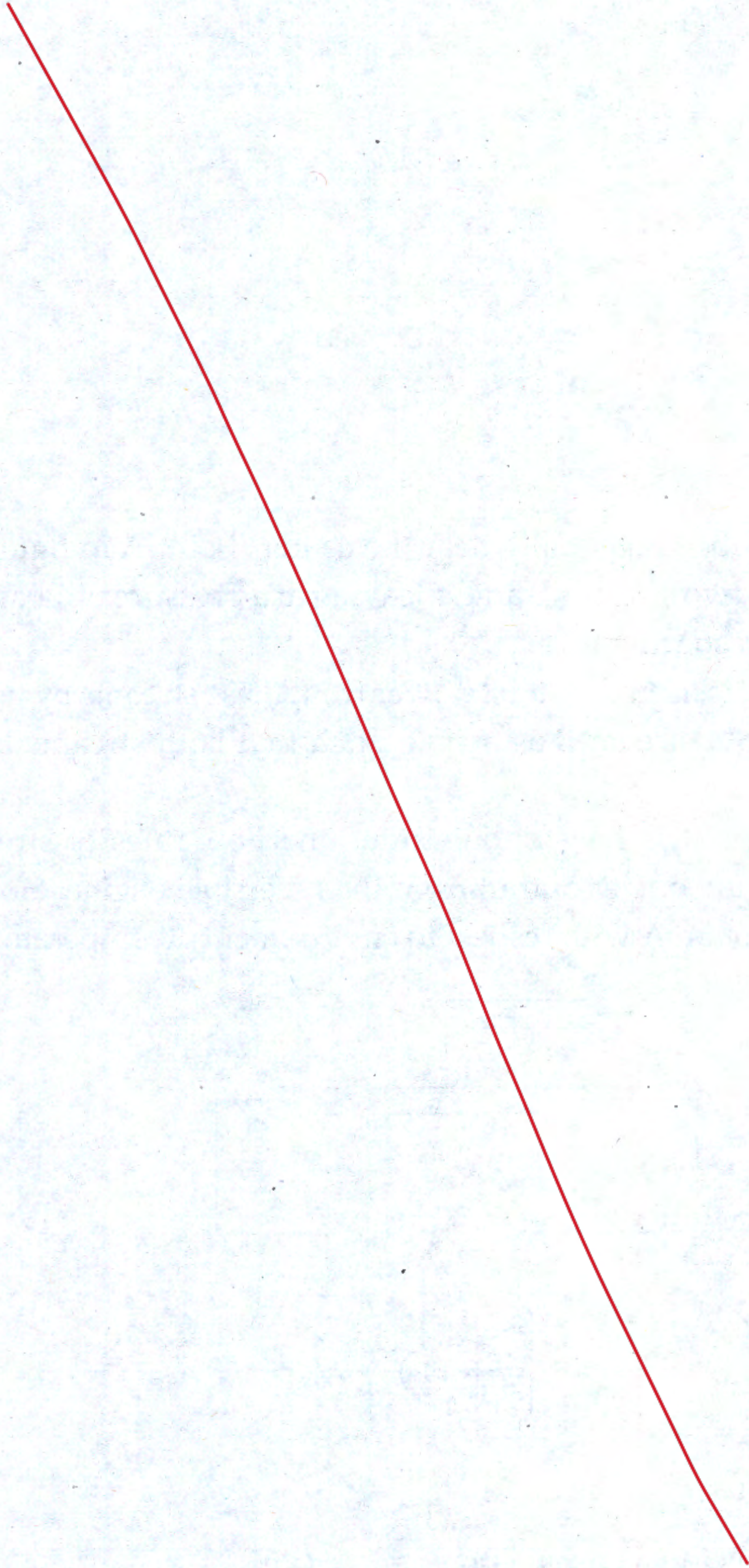
Also for air,  $pv = 0.287(t + 273)$

where,  $p$  is in kPa and  $v$  is in  $\text{m}^3/\text{kg}$ .

- (i) An evacuated bottle is fitted with a valve through which air from the atmosphere, at 760 mm Hg and  $27^\circ\text{C}$ , is allowed to flow slowly to fill the bottle. If no heat is transferred to or from the air in the bottle, what will its temperature be when pressure in the bottle reaches 760 mm Hg?
- (ii) If the bottle initially contains  $0.04 \text{ m}^3$  of air at 500 mm Hg and  $27^\circ\text{C}$ , what will the temperature be when pressure in the bottle reaches 760 mm Hg?

[20 marks]

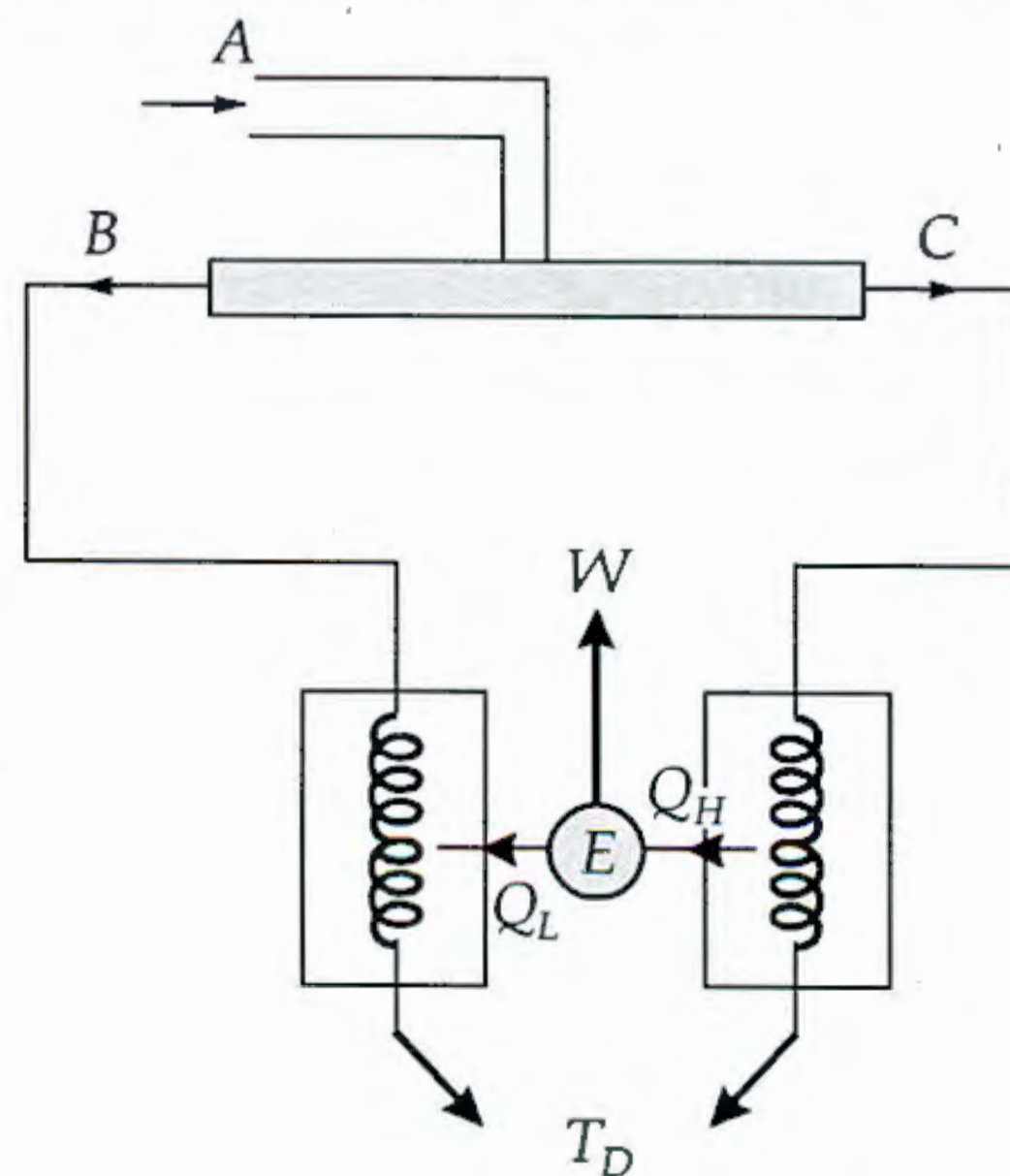




- Q.3 (c) Air enters a vortex tube tangentially near the center (Point A in figure) at 300 K and 15 bar. It bifurcates into two streams B and C leaving at a pressure of 1 bar and temperatures of 250 K and 315 K respectively.

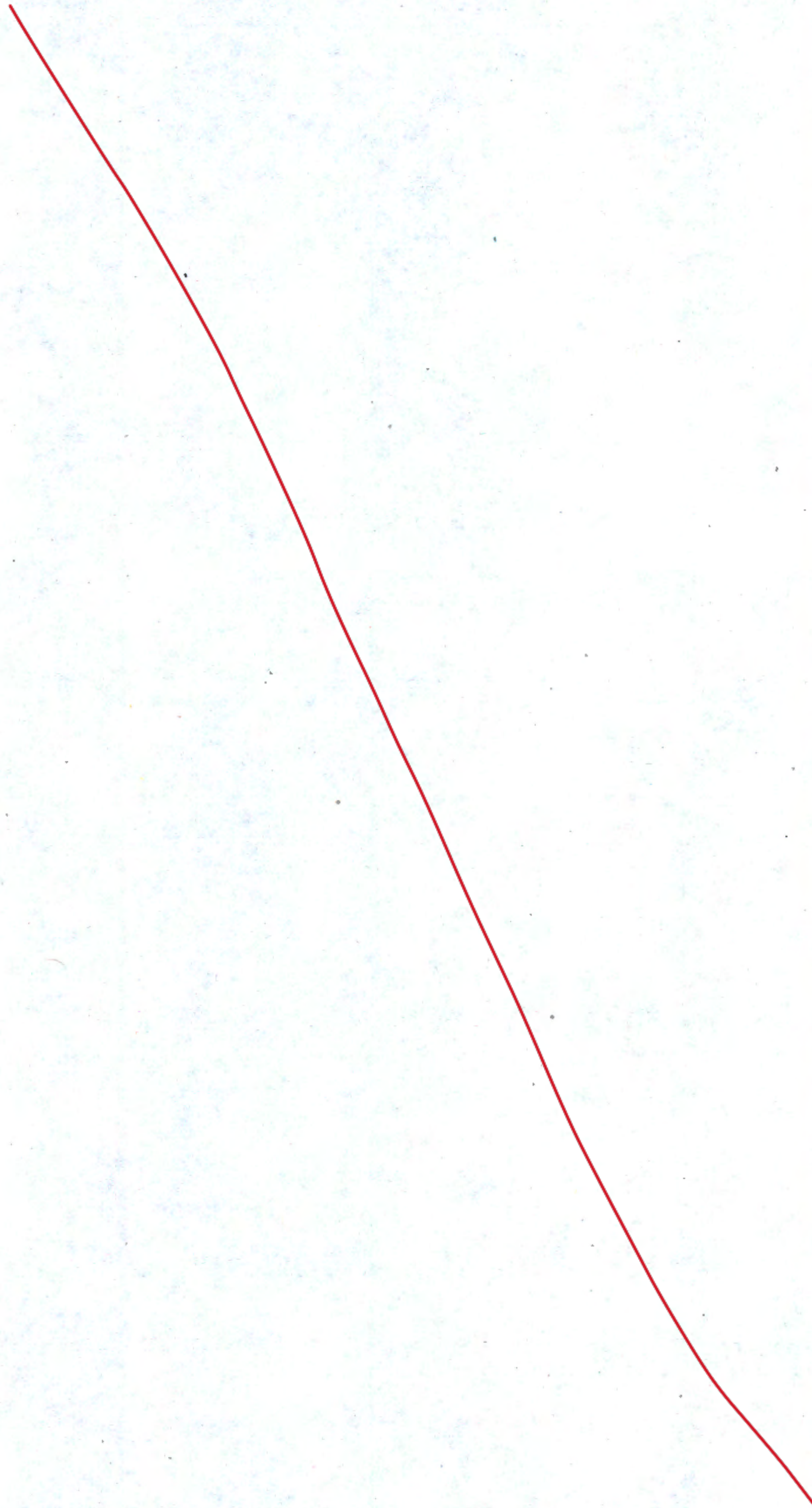
A reversible engine E is used to extract power from these streams by using the hot stream C as a source and cold stream B as a sink. Such that both streams leave the engine at temperature  $T_D$ .

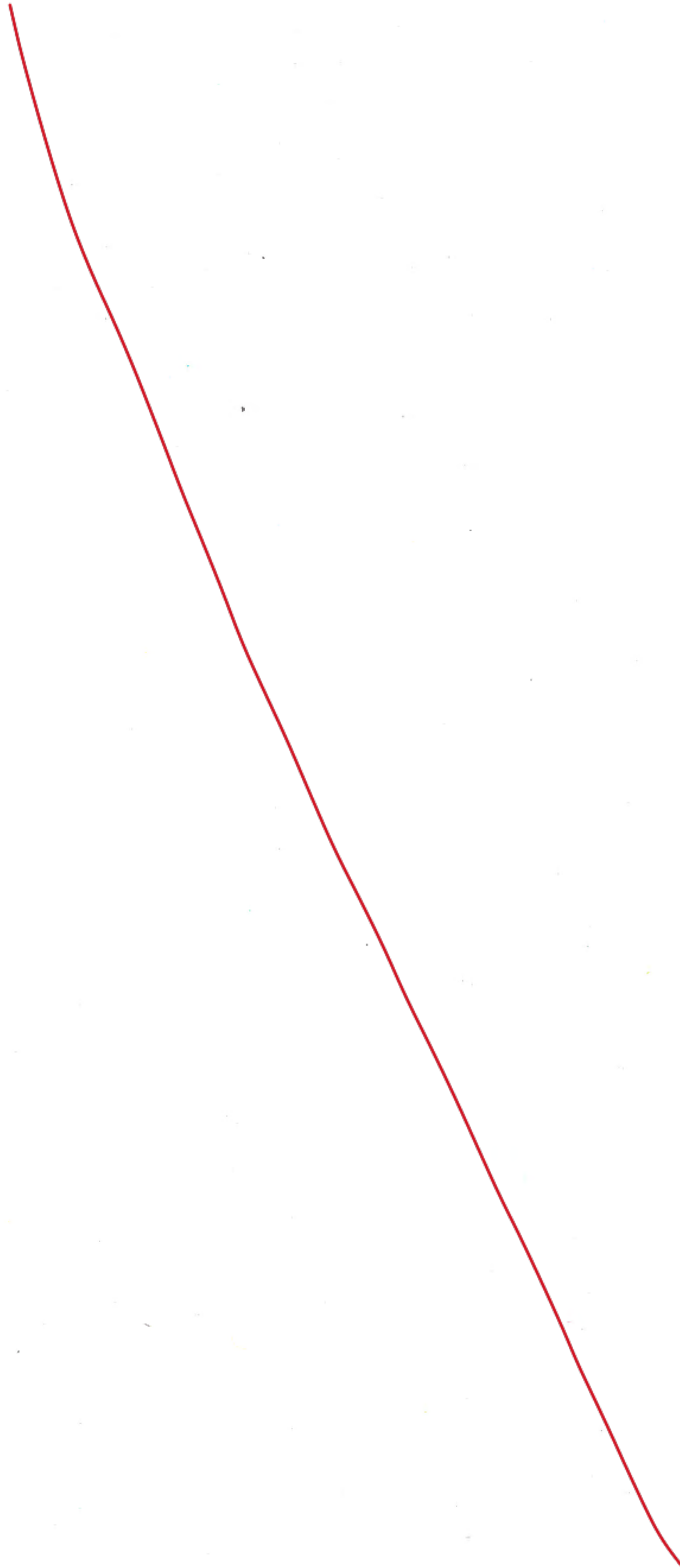
If flow rate of stream A is 1 kg/s, determine the flow rates of streams B and C, the temperature  $T_D$  and the power output from the reversible engine. How does it compare with the energy of stream A with respect to environment at temperature  $T_D$ ?



Assume all streams as ideal gases with  $c_p = 1 \text{ kJ/kgK}$ .

[20 marks]



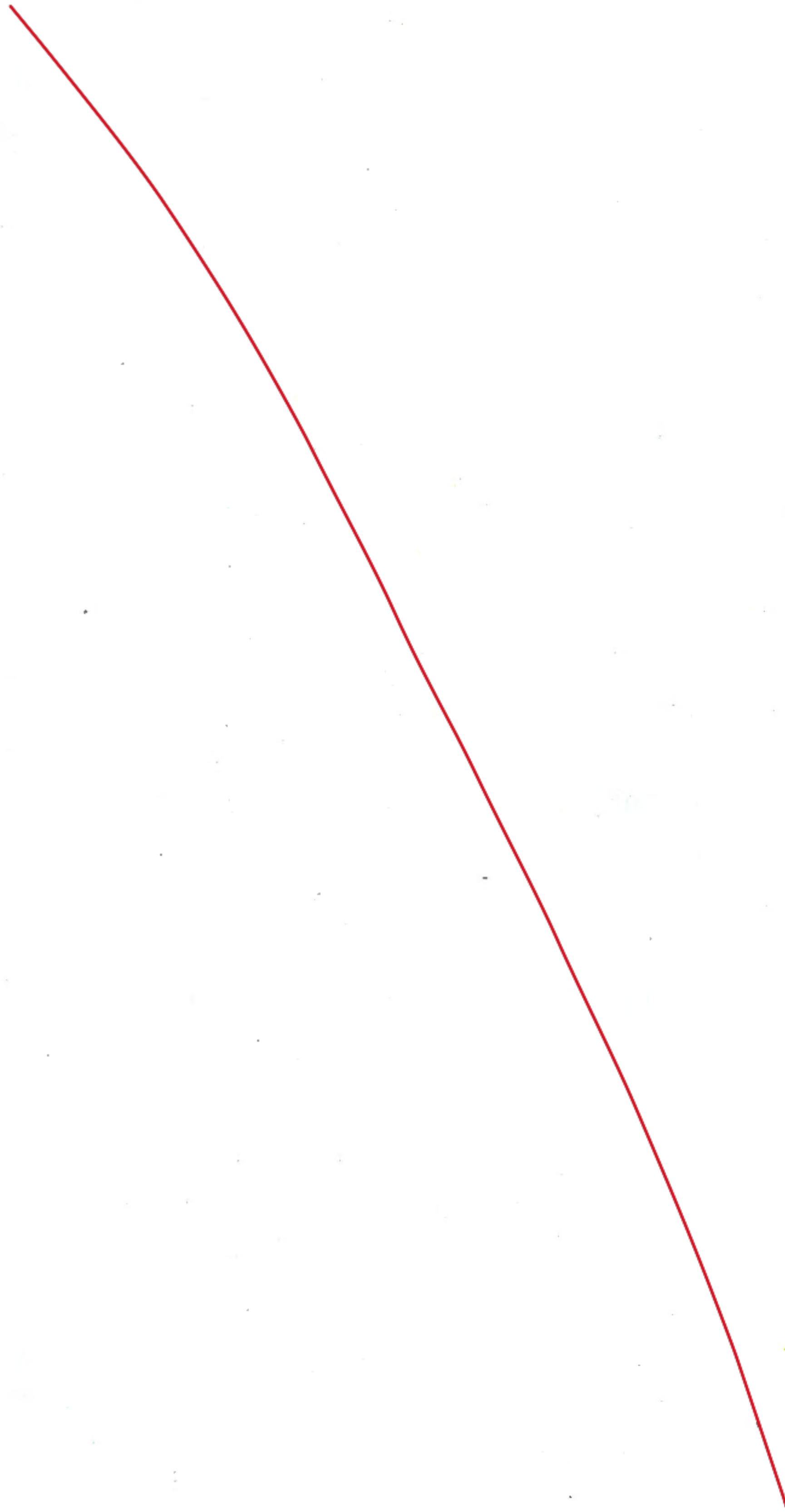


- Q.4(a) The equation of state of a certain gas is  $v = \frac{RT}{P} + \frac{K}{RT}$  (where  $K$  is a constant). Show that the change in temperature during throttling (enthalpy before and after remains the same) of such a gas from an initial pressure  $P_1$  to a final pressure  $P_2$  is given by

$$\frac{T_2^2 - T_1^2}{4K} = \frac{P_1 - P_2}{C_p R}$$

where,  $C_p$  is assumed constant during the process 1-2.

[20 marks]



- Q.4 (b) An ideal gas is compressed reversibly and adiabatically from state  $a$  to  $b$ . It then heated reversibly at constant volume to state  $c$ . After expanding reversibly and adiabatically to state  $d$  such that,  $T_b = T_d$ , the gas is again reversibly heated at constant pressure to state  $e$  such that  $T_e = T_c$ . Heat is then rejected reversibly from the gas at constant volume till it returns to state  $a$ . Express  $T_a$  in terms of  $T_b$  and  $T_c$ . If  $T_b = 500$  K and  $T_c = 850$  K. Estimate  $T_a$ . Take  $\gamma = 1.4$

[20 marks]

$$T_c = T_e = 850^\circ\text{K}$$

$$T_b = T_d$$

$$T_b = T_d = 500^\circ\text{K}$$

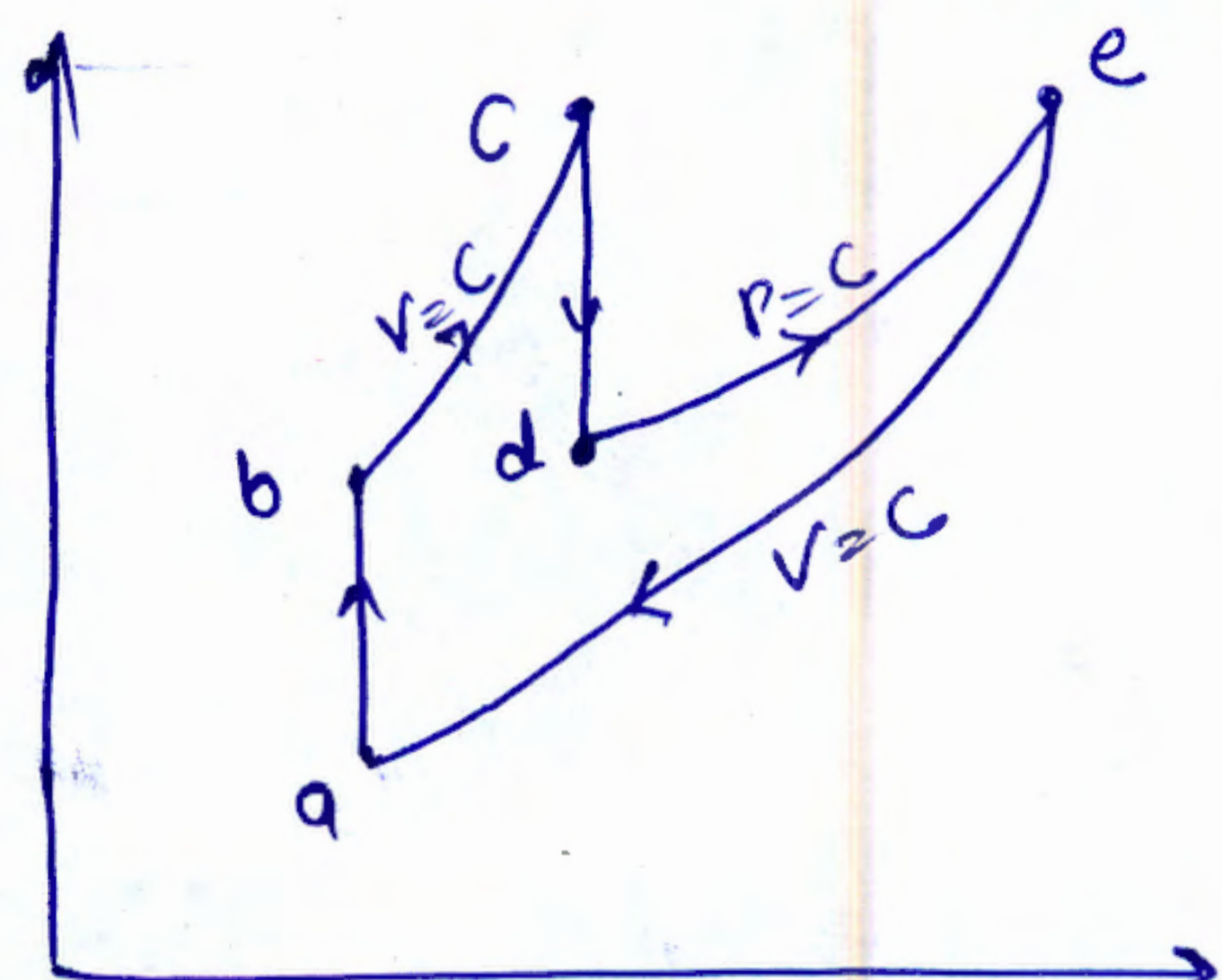
$$T_a = f(T_b \text{ \& } T_c)$$

$$\frac{T_b}{T_a} = \left(\frac{P_b}{P_a}\right)^{\frac{\gamma-1}{\gamma}}$$

$$T_b V_b^{\gamma-1} = T_a V_a^{\gamma-1}$$

from  $b$  to  $c$ 

$$\frac{P_b}{P_c} = \frac{T_b}{T_c}$$

from  $d$  to  $e$ 

$$\frac{T_d}{T_e} = \frac{V_d}{V_e}$$

$$\frac{T_b}{T_c} = V_d/V_e$$

from c to d

$$\frac{T_c}{T_d} = \left(\frac{P_c}{P_d}\right)^{\frac{\gamma-1}{\gamma}}$$

from a to e

$$\frac{P_e}{P_a} = \frac{T_e}{T_a}$$

$$(\Delta S)_{\text{cycle}} = 0$$

$$(\Delta S)_{b-c} + (\Delta S)_{d-e} + (\Delta S)_{e-a} = 0$$

$$A \quad C_v \ln\left(\frac{T_c}{T_b}\right) + C_p \ln\left(\frac{T_e}{T_d}\right) + C_v \ln\left(\frac{T_a}{T_e}\right)$$

$$\ln\left(\frac{T_c}{T_b}\right) + \ln\left(\frac{T_c}{T_b}\right)^{\gamma} + \ln\left(\frac{T_a}{T_c}\right) = 0$$

$$\frac{T_c}{T_b} \times \frac{T_c^{\gamma}}{T_b^{\gamma}} \times \frac{T_a}{T_c} = 1$$

$$T_a = \frac{T_b^{\gamma+1}}{T_c^{\gamma}} \quad \text{Ans}$$

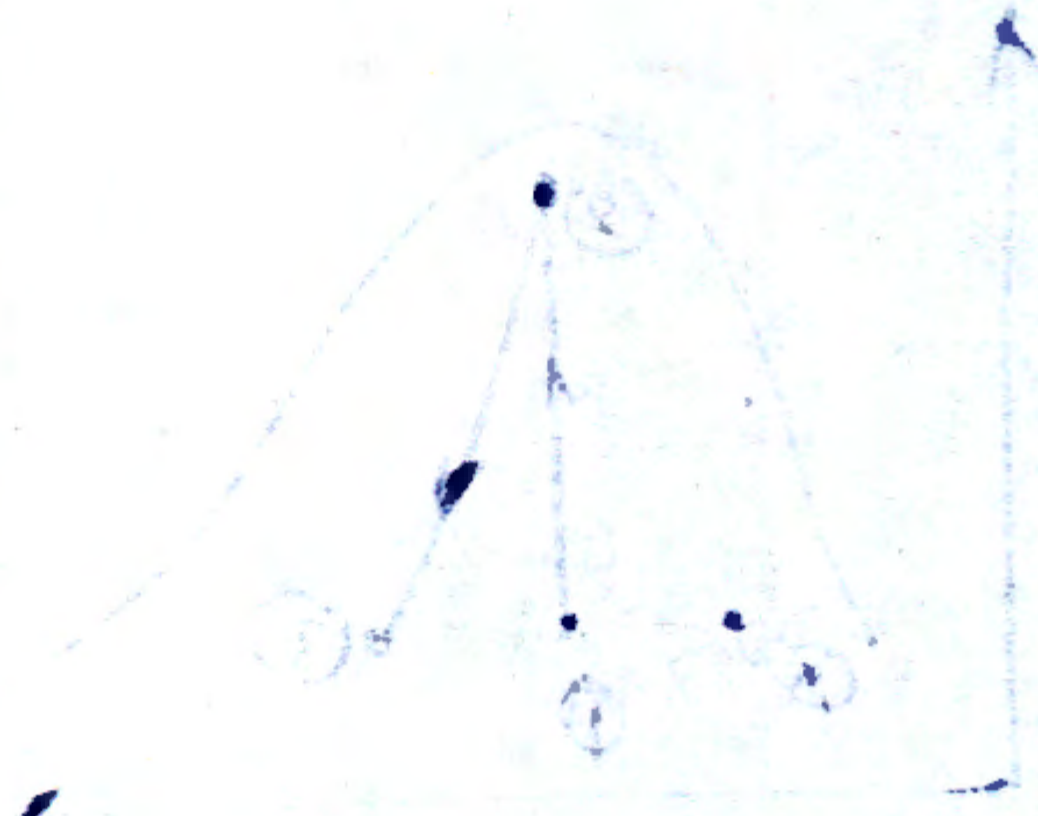
16

?

0



$C_2H_4$   
 The water vapor



$(0.0000100 - 2.42880) + 0.000000000$   
 $\times 0.12$

$(1.000000000 - 1.000000000) + 0.000000000$

$(1.000000000 - 1.000000000) + 0.000000000$

$(1.000000000 - 1.000000000) + 0.000000000$

$(1.000000000 - 1.000000000) + 0.000000000$

$(1.000000000 - 1.000000000) + 0.000000000$

Q.4 (c) A leakproof piston- cylinder arrangement contains 1 kg of water and steam at 2 bar and 0.35 dry. Heat is supplied at constant volume until pressure reaches 4 bar. The steam is then expanded according to law  $Pv = \text{constant}$  until the pressure reaches 2 bar. Calculate.

- Heat transferred during constant volume heating.
- Heat transferred and work transferred during  $Pv = \text{constant}$  expansion.
- Temperature and quality of steam after expansion process.

Also show the processes on P- V diagram.

[Use the steam table attached at the end]

[20 marks]

$$P_1 = 2 \text{ bar.}$$

$$x = 0.35$$

Heat supplied.

$$P_2 = 4 \text{ bar.}$$

Then expand accordingly

$$Pv = C$$

$$P_3 = 2 \text{ bar.}$$

from steam table

$$T_1 = 120.210^\circ\text{C.}$$

~~24~~

$$v_1 = v_f + (v_g - v_f) \times 0.35$$

$$= 0.00106052 + (0.88568 - 0.00106052) \times 0.35$$

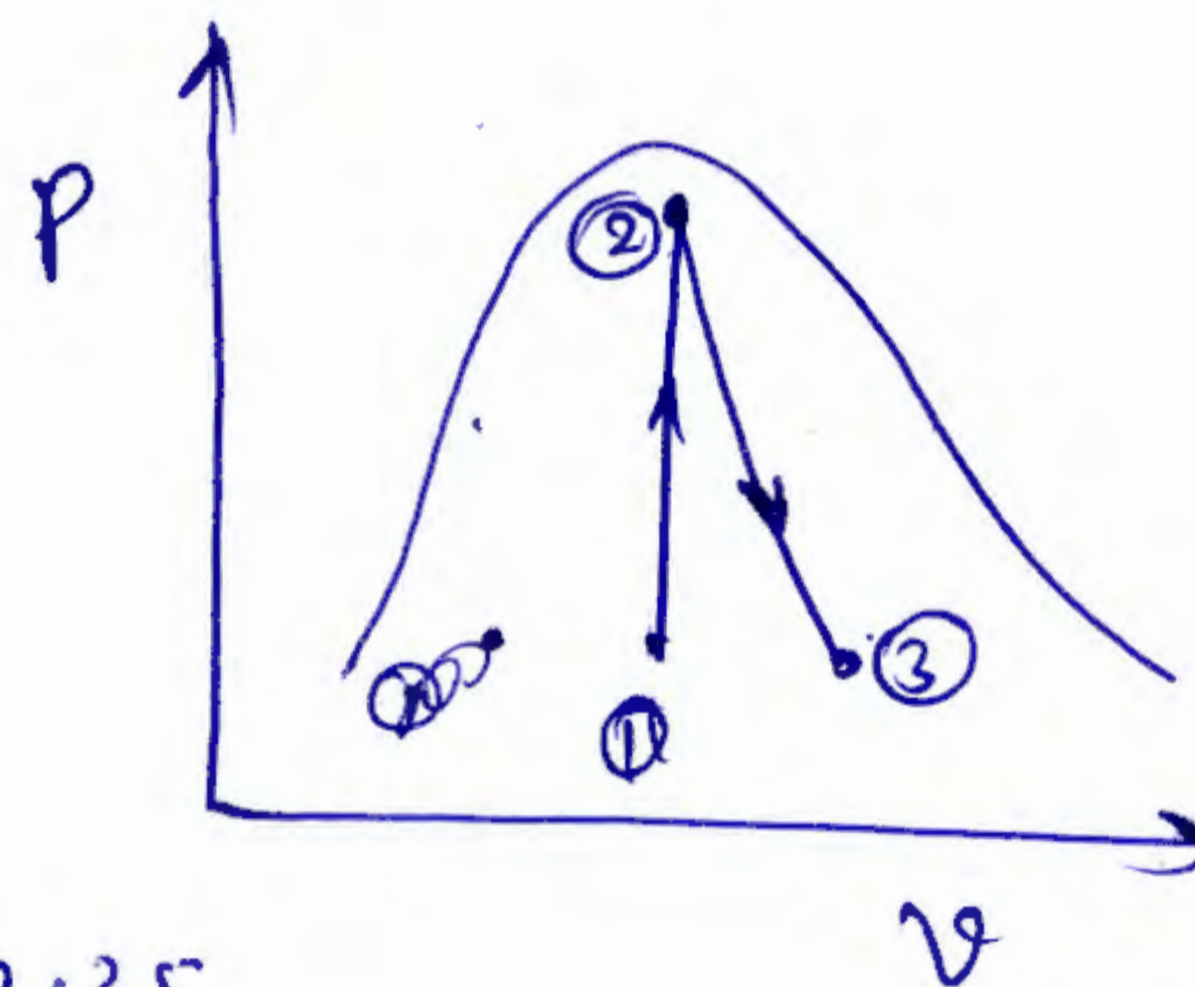
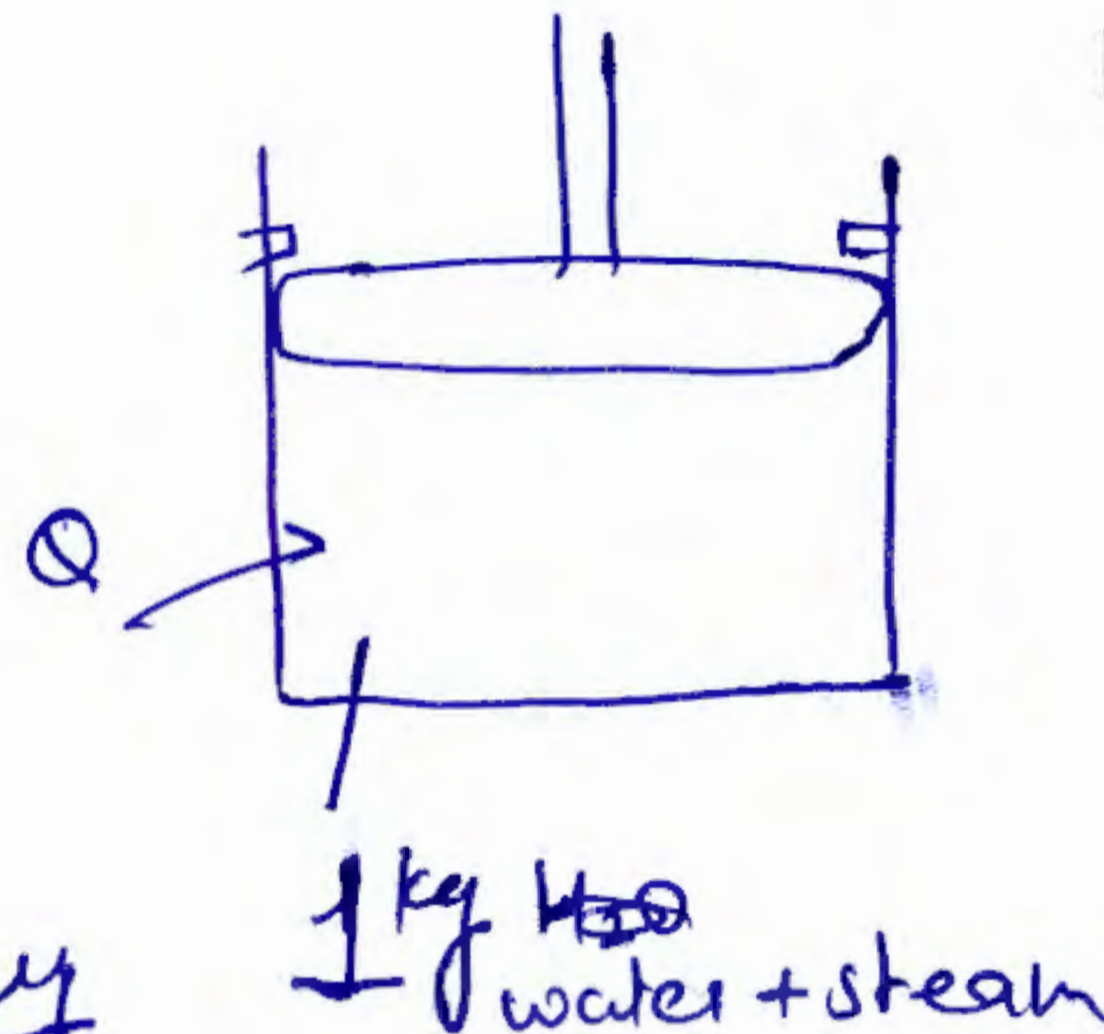
$$v_1 = 0.3106 \text{ m}^3/\text{kg}$$

$$u_1 = u_f + (u_g - u_f) \times 0.35$$

$$u_1 = 1213.1035 \text{ kJ/kg}$$

$$\Sigma V_1 = 0.3106 \times 1 \text{ m}^3$$

$$V_1 = 0.3106 \text{ m}^3$$



9

at stage (2)

$$v_2 = 0.3106 = 0.00108355 +$$

$$\kappa (0.46238 - 0.00108355)$$

$$\boxed{\kappa = 0.6709}$$

$$u_2 = 604.22 + (2553.1 - 604.22) \times 0.6709$$

$$\boxed{u_2 = 1911.723 \text{ kJ/kg}}$$

(1) Heat transfer during const  $v_0$  heating  
 $= 1911.723 - 1213.1$

$$\boxed{HT = 698.62 \text{ kJ}}$$

(2)

$$pv = \text{const.}$$

$$4 \times 0.3106 = 2 \times v_3$$

$$\boxed{v_3 = 0.6212 \text{ m}^3/\text{kg}}$$

(a) 2 bar, 2  $0.6212 \text{ m}^3/\text{kg}$

$$u_3 = ?$$

$$0.6212 \times v_3 = 0.00106052 + \kappa_3 (0.88568 - 0.00106052)$$

$$\boxed{\kappa_3 = 0.7}$$

$$u_3 = u_f + \kappa_3 (u_g - u_f)$$

$$\boxed{u_3 = 1921.717 \text{ kJ/kg}}$$

$$h_3 = 2045.75 \text{ kJ/kg}$$

$$h_2 = h_f + x_2(h_g - h_f) \quad \text{at point 2}$$

$$= 604.65 + 0.6709(2738.1 - 604.65)$$

$$h_2 = 2035.981 \text{ kJ/kg}$$

Heat transfer in  $PV = C$  process

$$= u_2 - u_3$$

$$= -1921.717 + 1911.723$$

$$= -10 \text{ kJ/kg}$$

10 kJ Heat will be rejected from the system

$$\delta Q = \Delta U + \delta W$$

There is no work transfer.

Temp<sup>r</sup> after expansion = 143.608°C

quality of steam after expansion = 0.7

Answer

3

Ans

## Section B : IC Engine + Refrigeration and Air-conditioning

Q.5 (a) A air refrigeration system working on the Bell-Coleman cycle takes air into the compressor at 1 bar and  $-6^{\circ}\text{C}$ . Air is compressed isentropically to 5.6 bar and then cooled at constant pressure to  $19^{\circ}\text{C}$ . Find the COP of the system if

- (i) The expansion is isentropic  
 (ii) The expansion follows the law  $pv^{1.26} = \text{constant}$   
 Take for air  $c_v = 0.7 \text{ kJ/kg-K}$ ,  $c_p = 1.0 \text{ kJ/kg-K}$ ,  $\gamma = 1.4$

[12 marks]

$$\frac{P_1 = 1 \text{ bar}}{T_1 = 267^{\circ}\text{K}}$$

$$\frac{P_2 = 5.6 \text{ bar.}}$$

$$T_2 = 267 \gamma (5.6)^{\frac{0.4}{1.4}}$$

$$\frac{T_2 = 436.79^{\circ}\text{K}}$$

$$\frac{T_3 = 292^{\circ}\text{K}}$$

$$\frac{T_3}{T_4} = (5.6)^{\frac{0.4}{1.4}}$$

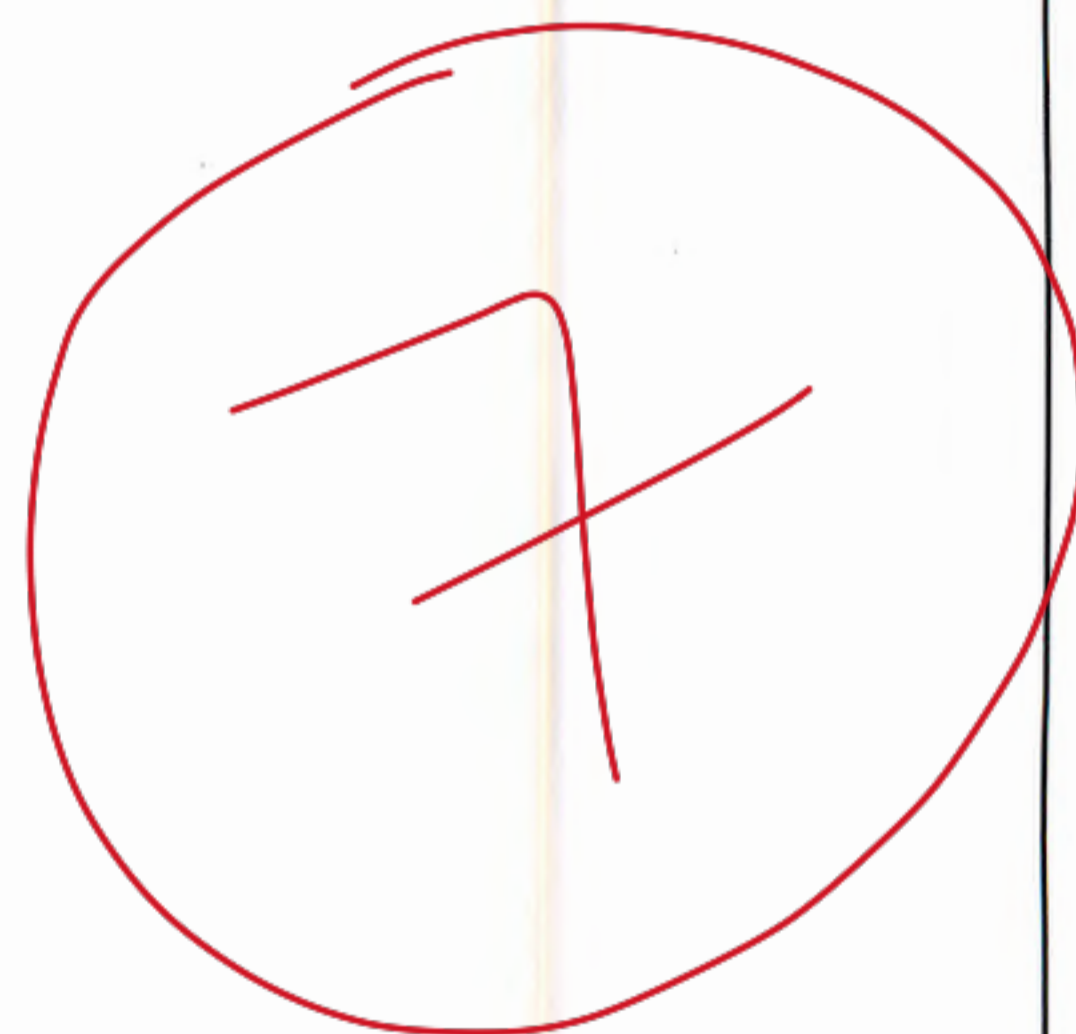
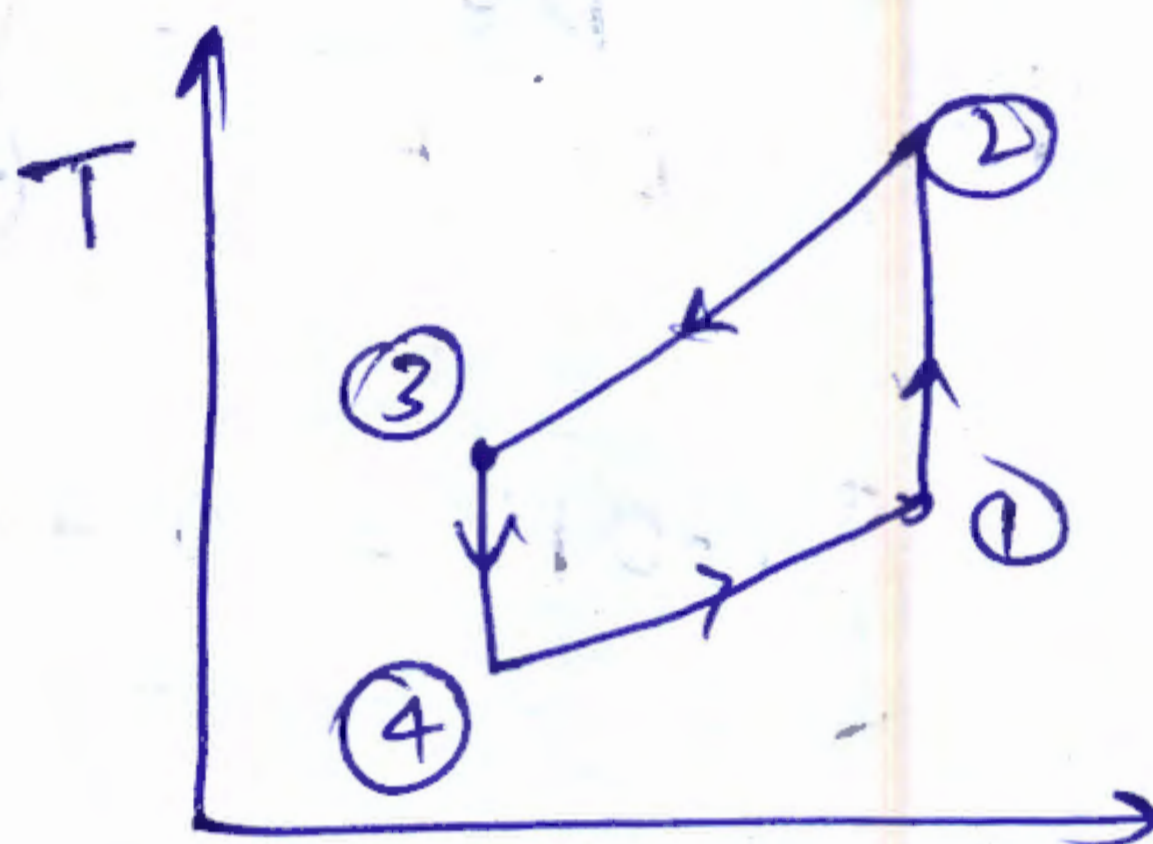
$$\frac{292}{T_4} = 5.6^{\frac{0.4}{1.4}}$$

$$\boxed{T_4 = 178.49^{\circ}\text{K}}$$

$$\text{COP} = \frac{DE}{W_c - W_r} = \frac{(T_1 - T_4)}{(T_2 - T_1) - (T_3 - T_4)} = \frac{267 - 178.49}{(436.79 - 267) - (292 - 178.49)}$$

$$= \frac{0.52192}{1.5726}$$

$$\boxed{\text{COP} = 1.5726}$$



Case II when expansion follows  $pV^{1.26} = c$

then

$$T_4 = \frac{T_3}{(5.6)^{\frac{0.26}{1.26}}}$$

$$T_4 = \frac{292}{5.6^{\frac{0.26}{1.26}}} = 204.64^\circ\text{K}$$

$$\text{COP}_2 = \frac{DE}{W_{\text{net}}} = \frac{(267 - 204.64)}{(\cancel{436.79} - 267) - (292 - 204.64)}$$

$$\boxed{\text{COP} = 0.7565}$$

Q.5 (b) A refrigeration plant of 110 tons capacity uses R-22 as refrigerant. The condensing and evaporating pressure are 11.82 bar and 1.64 bar respectively. The refrigerant enters the condenser as dry-saturated and it leaves the condenser, sub cooled by  $8^{\circ}\text{C}$ . The actual COP is 70% of theoretical COP. Determine

- The theoretical and actual COP
- The mass flow rate of refrigerant in kg/sec
- The compressor power required.

$p$ (bar)	$T_s$ ( $^{\circ}\text{C}$ )	$h_f$ (kJ/kg)	$h_g$ (kJ/kg)	$s_f$ (kJ/kg-K)	$s_g$ (kJ/kg-K)
1.64	-30	116.1	393.1	0.8698	1.803
11.82	+30	236.7	414.5	1.125	1.712

$C_p$  (vapour) =  $0.55$  kJ/kg $^{\circ}\text{C}$ ;  $C_p$  (liquid) =  $1.19$  kJ/kg $^{\circ}\text{C}$

[12 marks]

$$\begin{aligned}
 h_2 &= 414.5 \text{ kJ/kg} \\
 h_3 &= 236.7 \text{ kJ/kg} \\
 h_4 &= 236.7 \\
 &\quad - 1.19 \times 8 \\
 &= 227.18 \text{ kJ/kg}
 \end{aligned}$$

$$h_4 = h_5$$

$$h_1 = ?$$

$$\therefore s_2 = 1.712 \text{ kJ/kg-K}$$

$$s_2 = s_1$$

$$1.712 = 0.8698 + x_1 (1.803 - 0.8698)$$

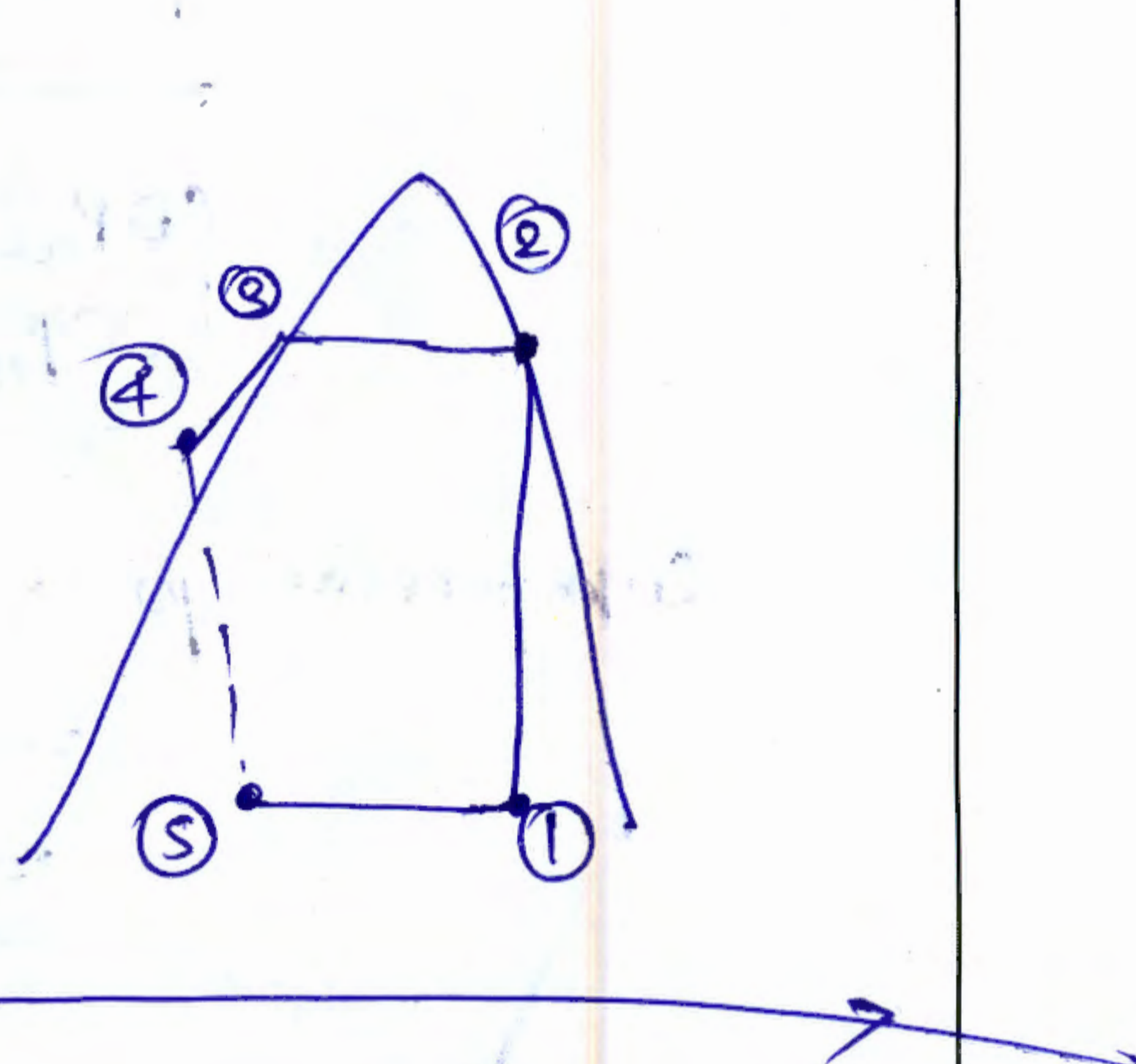
$$x_1 = 0.9024$$

$$RE = h_1 - h_5$$

$$h_1 = 116.1 + (393.1 - 116.1) \times 0.9024$$

$$h_1 = 366.0648 \text{ kJ/kg}$$

$$DE = RE = h_1 - h_5 = 138.88 \text{ kJ/kg}$$



$$RC = 110 \times 3.5$$

$$\dot{m} \times (RE) = 110 \times 3.5$$

$$\dot{m} \times 138.88 = 110 \times 3.5$$

$$\dot{m}_{\text{Req.}} = 2.7721 \text{ kg/s.} \quad \underline{\text{Ans}}$$

$$\text{COP}_{\text{the}} = \frac{DE}{W_{in}} = \frac{138.88}{414.5 - 366.0648}$$

$$\text{COP}_{\text{th}} = 2.867 \quad \underline{\text{Ans}}$$

$$\text{COP}_{\text{act}} = 0.7 \times \text{COP}_{\text{th}}$$

$$\text{COP}_{\text{act}} = 2 \quad \underline{\text{Ans}}$$

Compressor power Required

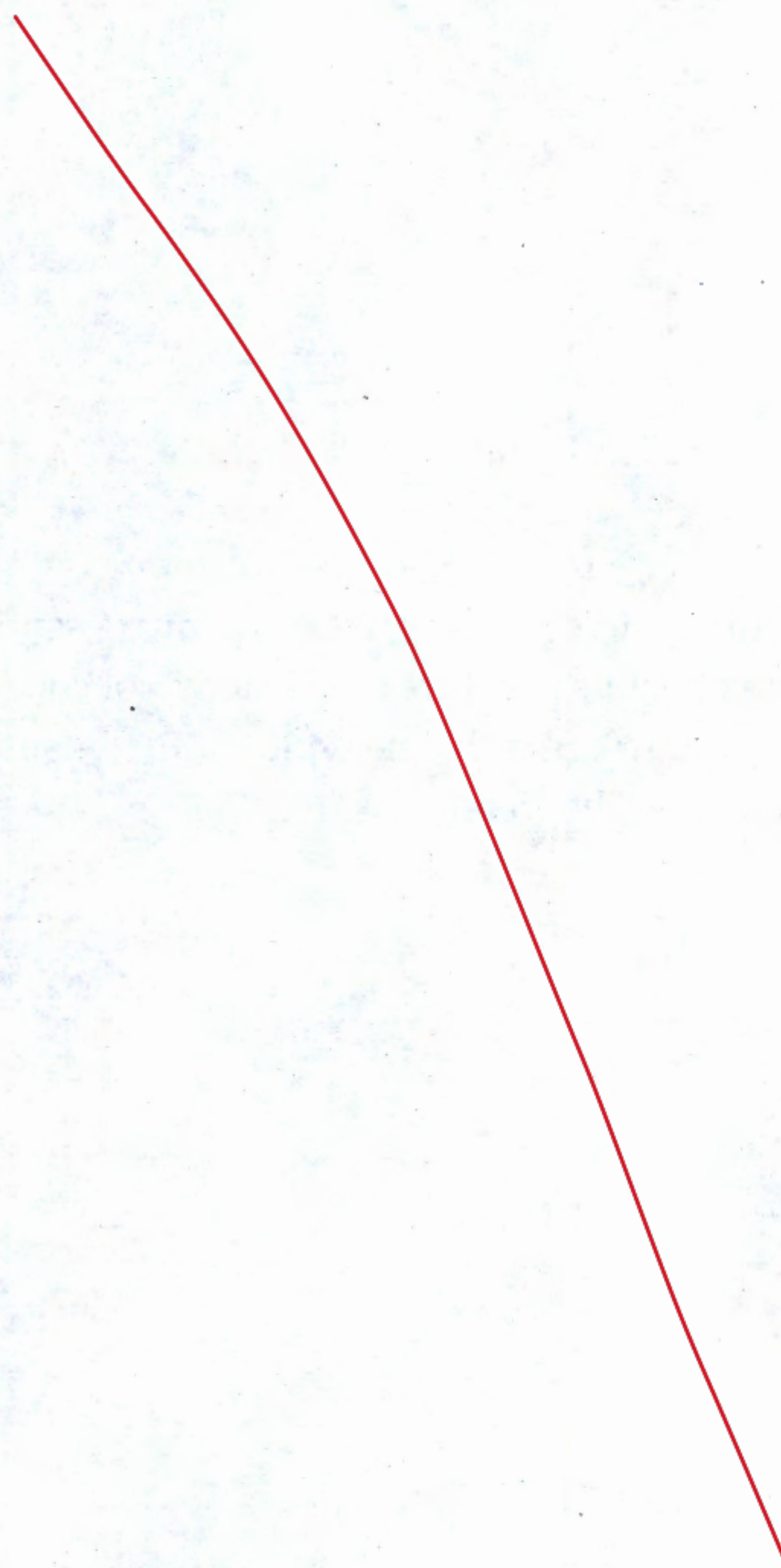
$$= \dot{m}_{\text{Re}} \times (h_2 - h_1)$$

$$= 134.26 \text{ kW.} \quad \underline{\text{Ans}}$$

12

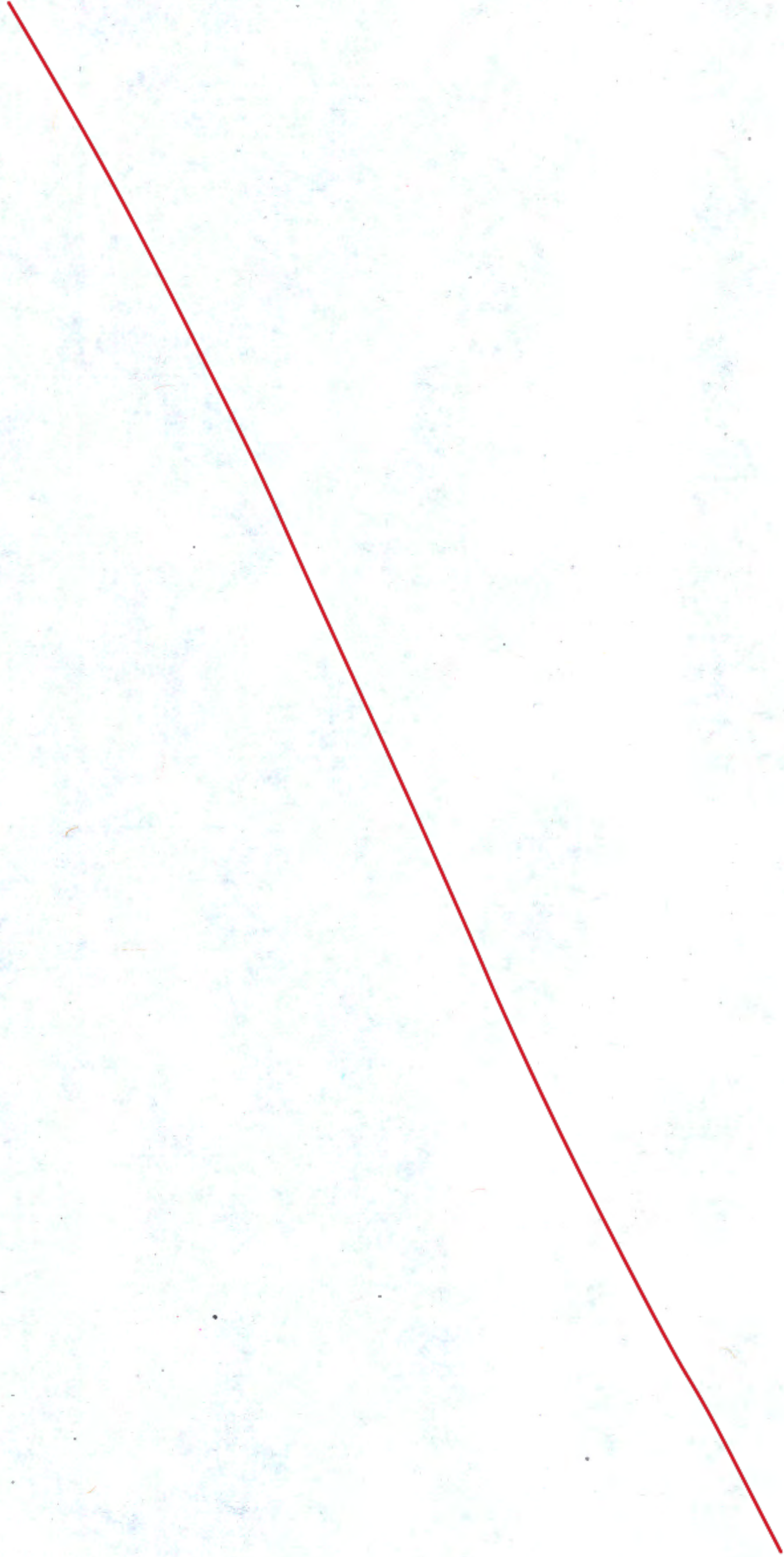
Q.5 (c) Discuss the advantages of an SI engine with the multi-point fuel injection system over the carburetted engine. Also draw the performance curve for the fuel-injection and carburettor system.

[12 marks]



- Q.5 (d) For an air standard otto cycle operating with initial pressure  $P_1$  and  $T_1$ , derive an expression for the mean effective pressure ( $P_m$ ) in terms of compression ratio ( $r$ ), specific heat ratio ( $\gamma$ ), pressure ratio ( $\alpha$ ). Sketch a neat plot of  $P_m$  versus  $\alpha$  for different values of compression ratio, indicating the trend.

[12 marks]



Q.5 (e) A Carnot engine receives heat at temperature,  $T_a$  and rejects heat to sink at temperature,  $T_b$ . This engine drives a Carnot refrigerator which removes the heat at  $T_c$  and rejects heat at  $T_b$ . Determine:

- (i) The ratio  $\frac{Q_c}{Q_a}$ , where  $Q_c$  = Heat removed at  $T_c$ ,  $Q_a$  = Heat received at  $T_a$  in terms of temperatures of reservoirs.
- (ii)  $T_b$ , such that  $Q_a$  (Heat supplied to engine) =  $Q_c$  (Heat removed by refrigerator)  
Given that  $T_a = 300^\circ\text{C}$  and  $T_c = -20^\circ\text{C}$
- (iii)  $\eta_{\text{engine}}$  and  $(\text{COP})_{\text{refrigerator}}$  for the conditions given in part (ii).

[12 marks]

- Q.6 (a) A steam ejector water vapor system is supplied with motive steam at 8 bar and in saturated condition when the water in the flash chamber is at 6°C. Make up water is supplied to the cooling system at 18°C and condenser is operated at 5 cm of Hg absolute. The nozzle efficiency is 90%, entrainment efficiency is 66%, and thermocompressor efficiency is 83%. The quality of the motive steam and flashed vapour mixed together at the beginning of compression is 93% dry.

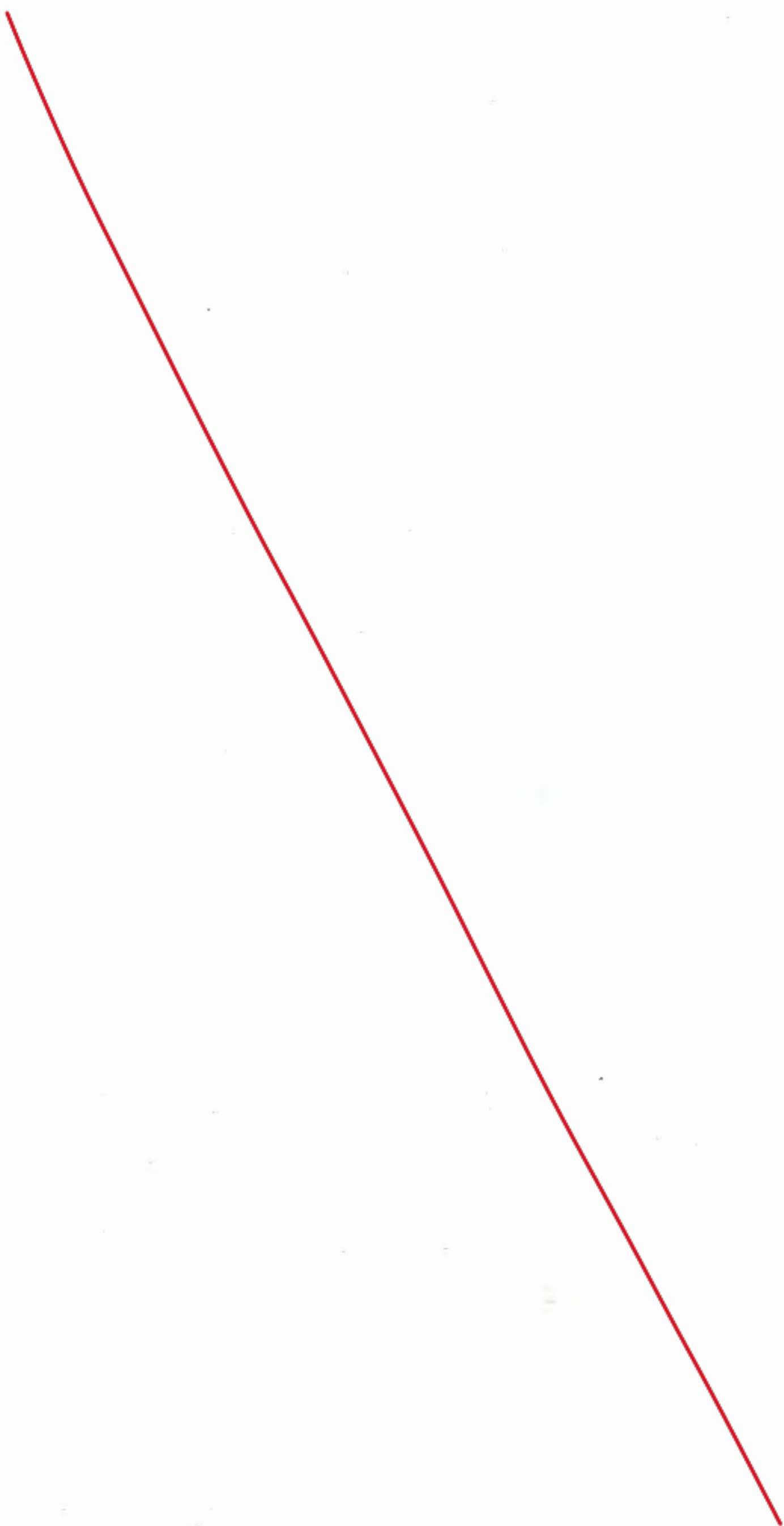
Take  $(c_p)_{\text{vapour}} = 2.1 \text{ kJ/kgK}$

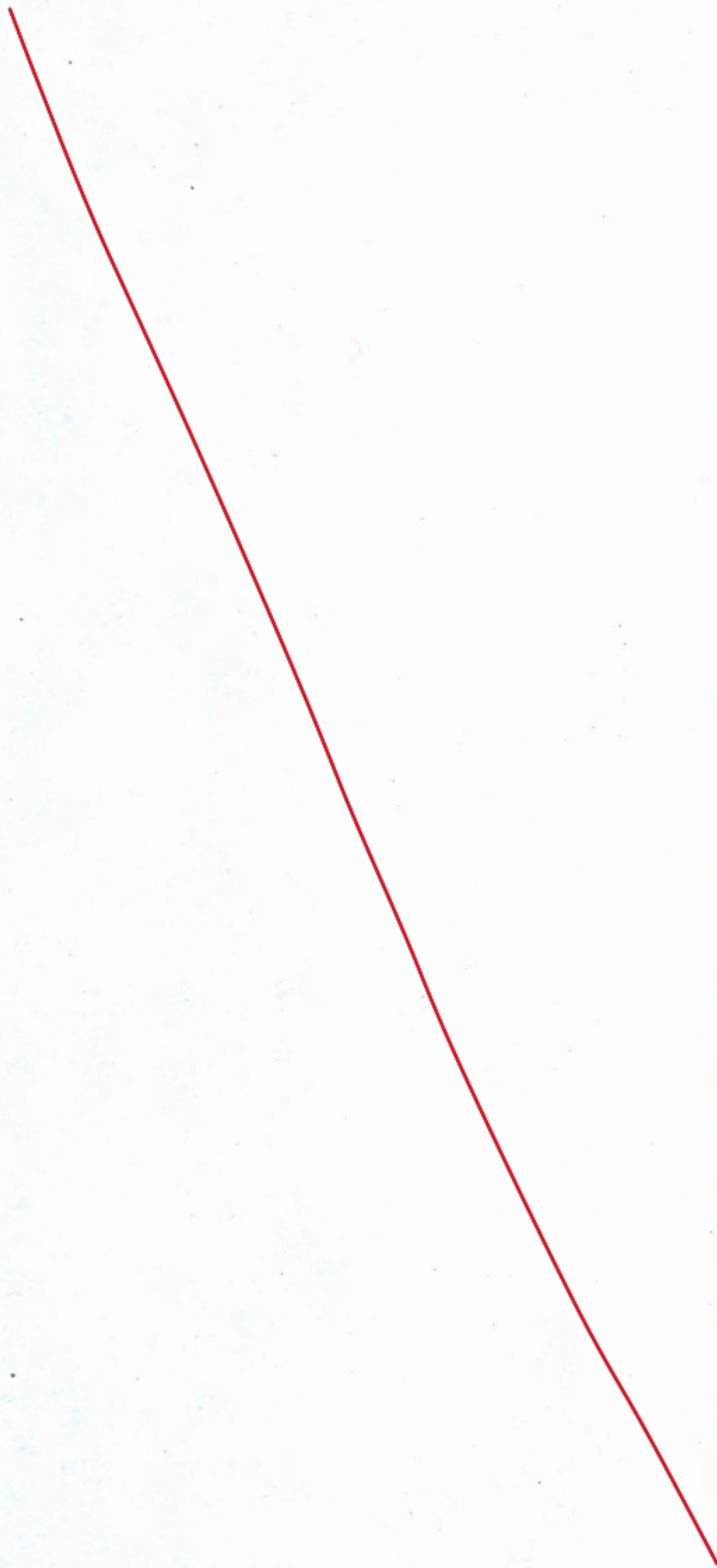
Determine:

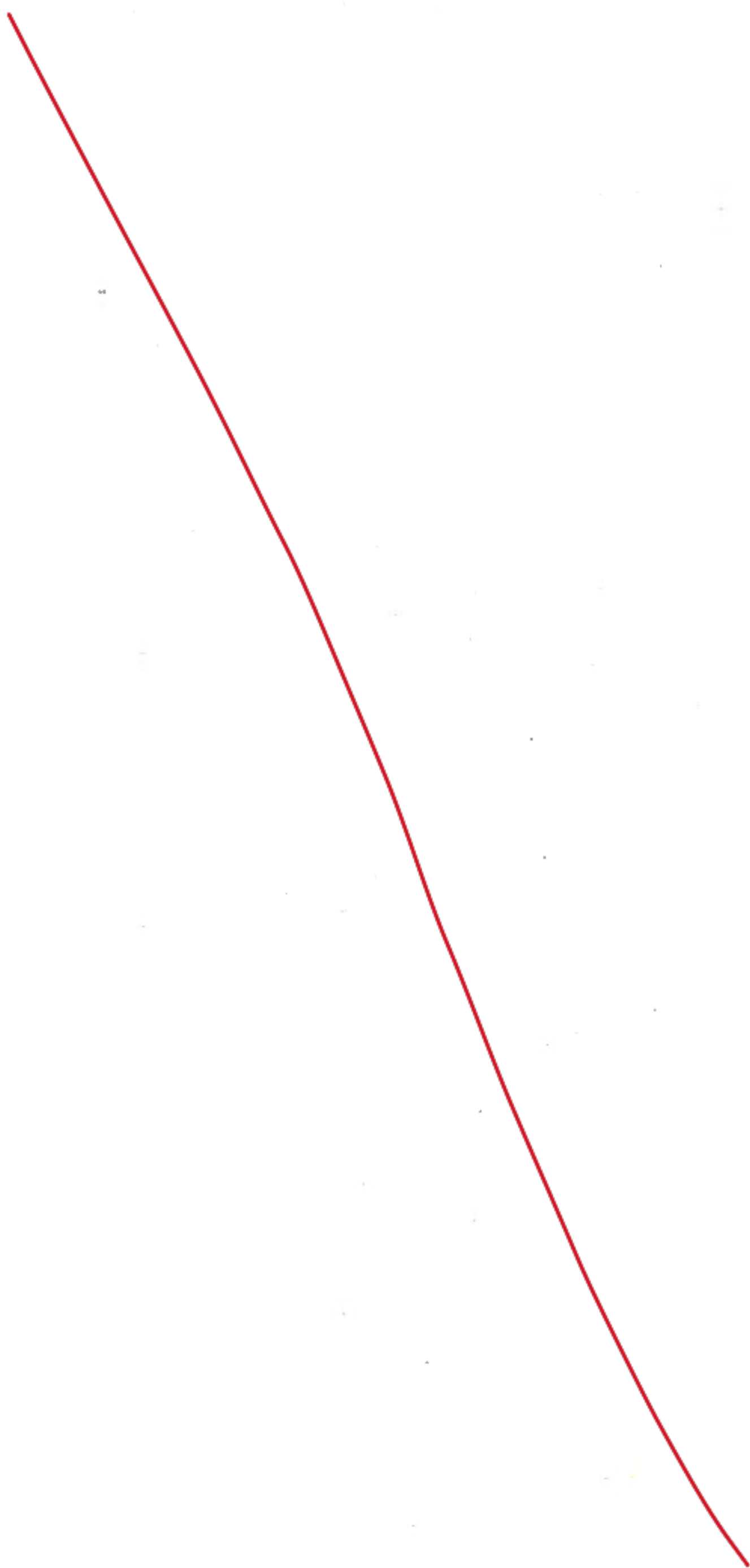
- (i) The mass of motive steam required per kg of flashed vapour.
- (ii) The refrigeration effect per kg of flash vapour.

[Use Steam Table attached at the end]

[20 marks]







- Q.6 (b) An air-Standard Diesel cycle operates with a Compression ratio of 16, and the cut-off occurs at 5% of the stroke. Determine the percentage change in thermal efficiency if the specific heat at constant pressure increases by 3%. Take  $c_p = 1.004$  kJ/kgK and  $R = 0.287$  kJ/kgK.

[20 marks]

$r = 16$   
cut off occurs at 5% of strokes

$$(\beta - 1) = \% \beta (r - 1)$$

$$(\beta - 1) = 0.05(15)$$

$$\beta = 0.75 + 1$$

$$\beta = 1.75$$

$$\therefore C_p - C_v = R$$

$$1.004 - C_v = 0.287$$

$$C_v = 0.717$$

$$\gamma = C_p / C_v = 1.4$$

$$\eta_1 = 1 - \frac{1}{r^{\gamma-1}} \times \frac{(\beta^{\gamma} - 1)}{\gamma(\beta - 1)}$$

$$= 0.6264$$

$$\eta_1 = 62.64\%$$

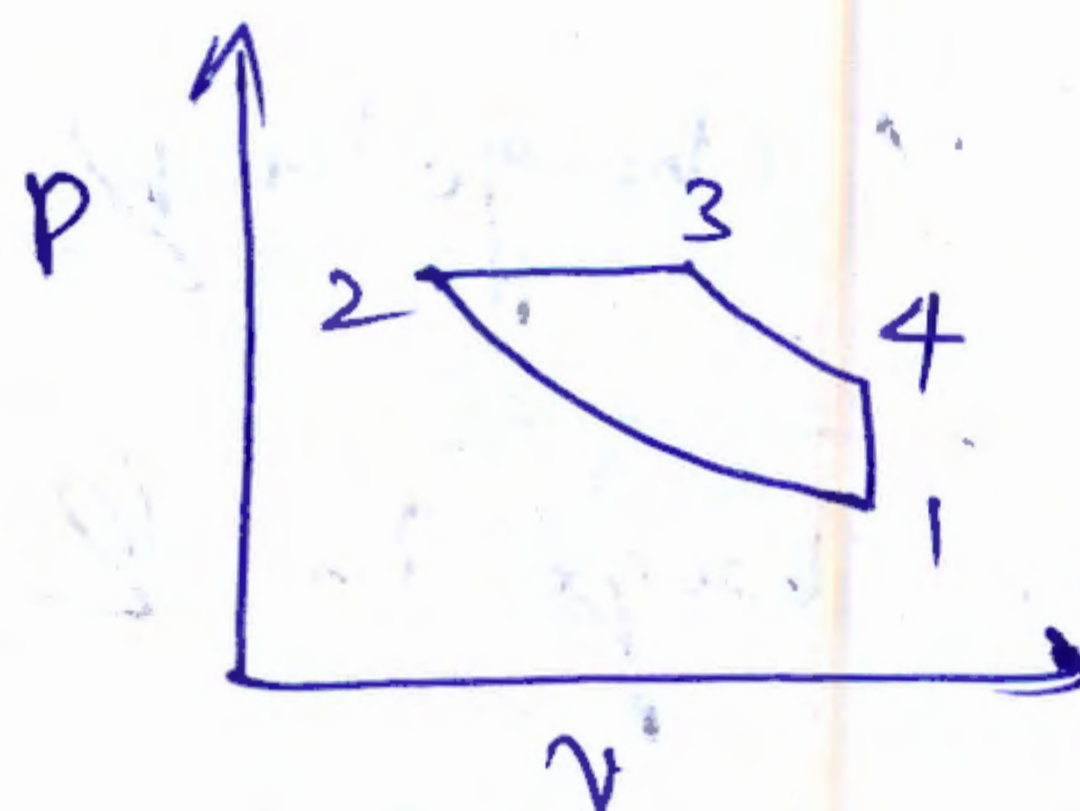
Case II: when  $C_p \rightarrow 1.03 C_p$

$$\therefore C_p' - C_v' = R$$

$$C_v' = -0.287 + 1.03 C_p$$

$$\therefore \gamma' = \frac{C_p'}{C_v'} = \frac{1.03 C_p}{1.03 C_p - 0.287}$$

$$\gamma' = 1.3841$$



$$V_{II} = 1 - \frac{1}{r^{y'-1}} \times \frac{(p^{y'} - 1)}{y'(p-1)}$$

$$V_{II} = 0.61156$$

$$V_{II} = 61.156\%$$

$$\% \text{ change in } V = \frac{61.156 - 62.64}{62.64} \times 100\%$$

$$\% \text{ change in } V = -2.36\%$$

Ans

20

Q.6 (c) A four cylinder four stroke SI engine has a bore of 50 mm and a stroke of 75 mm. It runs at 2500 rpm and is tested at this speed against a brake which has a torque arm of 0.30 m. The net brake load is 150 N and fuel consumption is 5.5 litre/hour. The specific gravity of the fuel used is 0.75 and it has a lower calorific value of 42000 kJ/kg. A Morse test is carried out and the cylinders are cut out in the order 1, 2, 3, 4 with corresponding brake loads of 108N, 101N, 103N and 110N respectively. Calculate for this speed

- |   |                                      |
|---|--------------------------------------|
| (i) Brake power                         | (ii) Brake mean effective pressure   |
| (iii) Brake thermal efficiency          | (iv) Brake specific fuel consumption |
| (v) Indicated power                     | (vi) Mechanical efficiency           |
| (vii) Indicated mean effective pressure |                                      |

[20 marks]

$$D = 0.05 \text{ m.}$$

$$L = 0.075 \text{ m.}$$

$$N = 2500 \text{ rpm.}$$

$$r_d = 0.3 \text{ m.}$$

$$F_b = 150 \text{ N.}$$

$$\dot{m}_f = 5.5 \text{ litre/hour}$$

$$S = 0.75$$

$$C_{vf} = 42000 \text{ kJ/kg.}$$

Morse key test

$$3I_1 - 4F = 108 \text{ N.}$$

$$3I_2$$

$$4I_1 - 4F = (3I_1 - 4F)$$

$$I_1 = 105 \quad 150 - 108$$

$$\text{(Indicated load)} = 42 \text{ N}$$

$$I_2 = 49 \text{ N}$$

$$I_3 = 47 \text{ N}$$

$$I_4 = 40 \text{ N}$$

$$\text{Total indicated load} = 178 \text{ N.}$$

$$\textcircled{1} \quad BP = B_{\text{load}} \times \omega \times R_d$$

$$= 150 \times 0.3 \times \left( \frac{2\pi \times 2500}{60} \right)$$

$$BP = 11.78 \text{ kW.} \quad \underline{\text{Ans}}$$

$$\textcircled{2} \quad \eta_{bm} = \frac{BP}{\text{HA/s.}} = \frac{11.78}{\frac{5.5 \times 0.75 \times 42000}{3600}}$$

$$= 0.244779.$$

$$\eta_{bm} = 24.4779\% \quad \underline{\text{Ans}}$$

$$BP = P_{bmep} \times V_s$$

$$10^3 \times 11.78 = P_{bmep} \times \frac{\pi}{4} \times 0.05^2 \times 0.075 \times$$

$$\frac{2500}{60 \times 2} \times 4$$

↓  
4 stroke     4 cy.

$$\textcircled{3} \quad P_{bmep} = 959.92 \text{ kPa} \quad \underline{\text{Ans}}$$

$$\textcircled{4} \quad \text{bsfc} = ?$$

$$\text{bsfc} = \frac{\dot{m}_f}{BP} = \frac{5.5 \times 0.75}{11.78}$$

$$\underline{\text{Ans}} \quad \text{bsfc} = 0.35016 \text{ kg/kwh}$$

$$\begin{aligned} \text{Indicated power} &= I_{\text{load}} \times \omega \times r_d \\ &= 178 \times \frac{2\pi \times 2500}{60} \times 0.3 \end{aligned}$$

$$\text{Ans } \boxed{IP = 13.980 \text{ kW}}$$

$$\begin{aligned} \textcircled{6} \quad \eta_{\text{mech}} &= BP/IP \\ &= \frac{11.78}{13.980} \\ &= 0.8426. \end{aligned}$$

$$\boxed{\eta_{\text{mech}} = 84.26 \%} \quad \text{Ans}$$

$$\begin{aligned} \textcircled{7} \quad P_{\text{meq}} &= ? \\ IP &= P_{\text{meq}} \times V_s. \end{aligned}$$

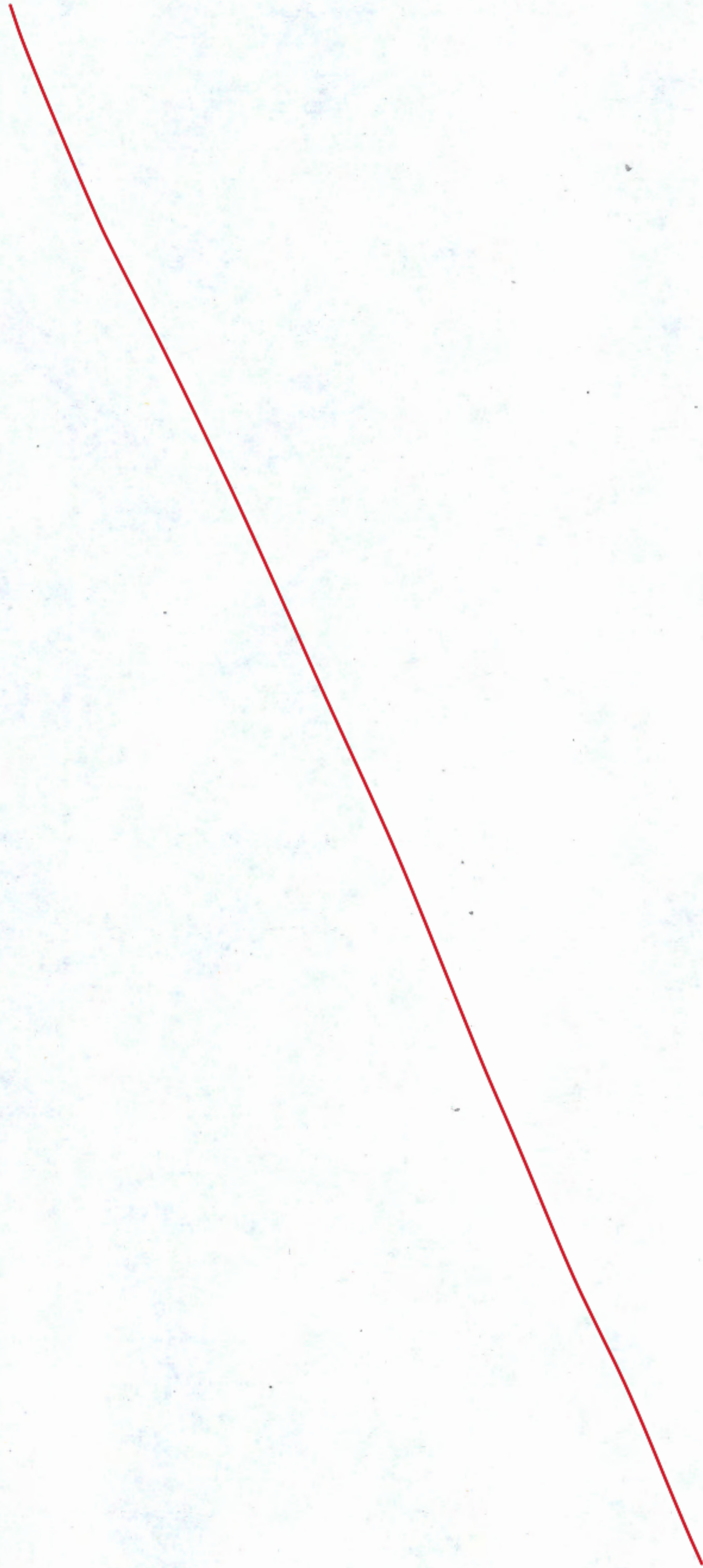
$$13.980 = P_{\text{meq}} \times \frac{\pi}{4} \times 0.05^2 \times 0.075 \times \frac{2500}{120} \times 4$$

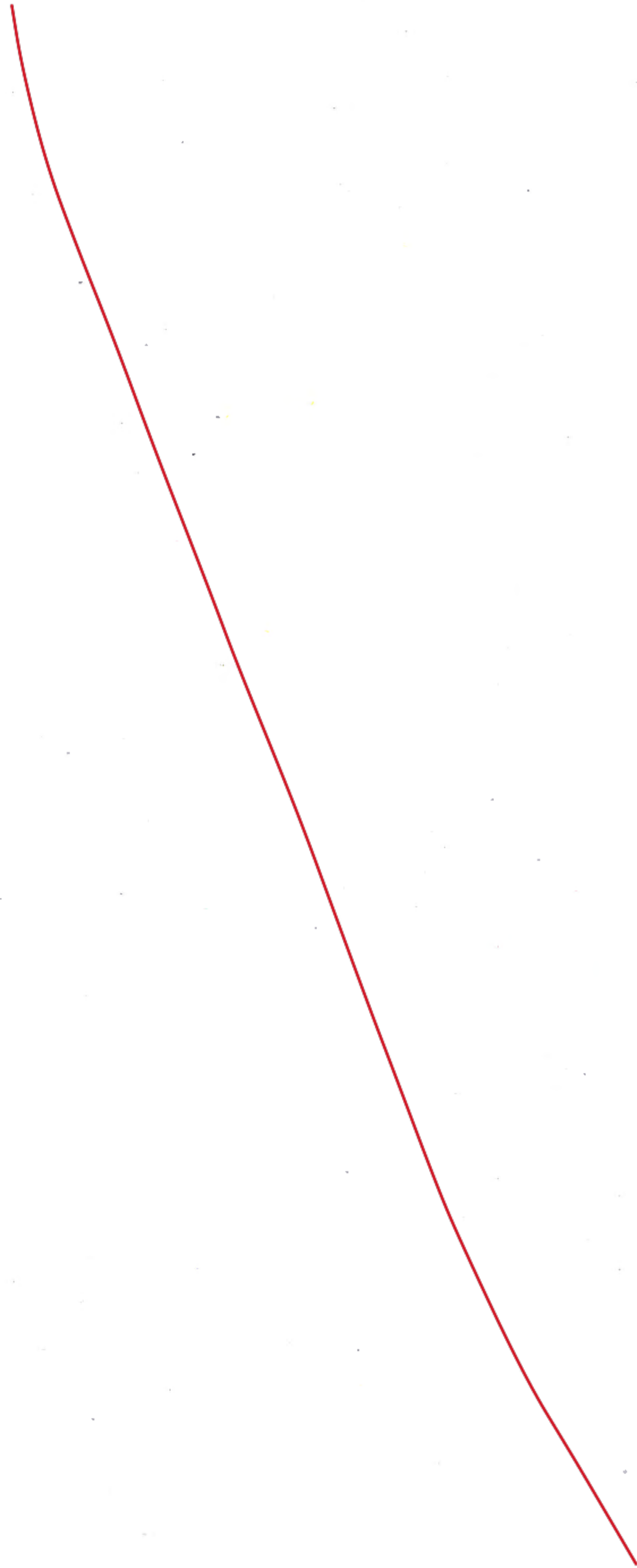
$$\boxed{P_{\text{meq}} = 1139.19 \text{ kPa}} \quad \text{Ans}$$

20

- Q.7 (a) The analysis of a fuel used in a SI engine found to be carbon 85%, hydrogen 6%, oxygen 1.8%, sulphur 0.6% by weight and the remaining is nitrogen. Determine the stoichiometric air-fuel ratio for complete combustion. If the actual supply of air is 20% in excess of stoichiometric, estimate the percentage composition of dry products of combustion by weight and volume.

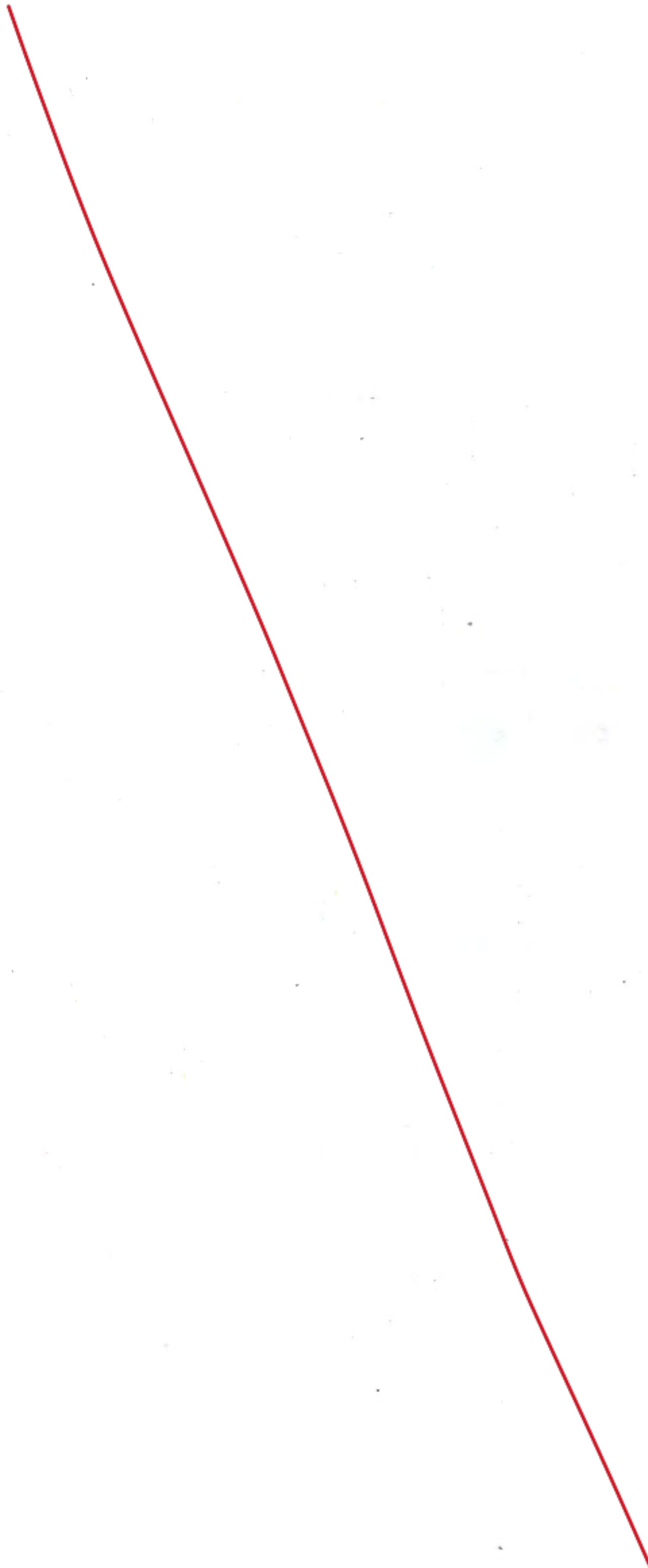
[20 marks]

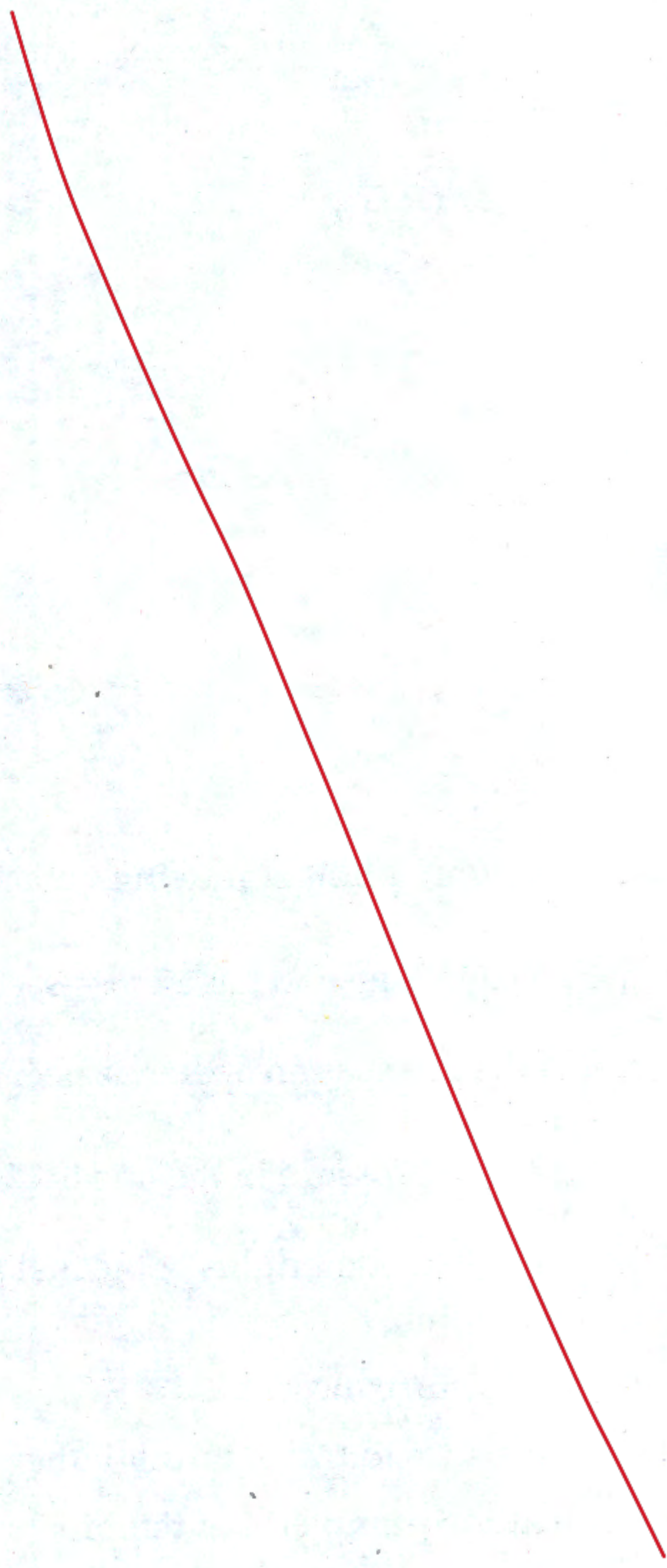




- Q.7 (b) (i) Describe the construction and working of a thermostatic expansion valve (TEV) with a neat sketch. Explain how superheat is maintained in the evaporator using a TEV.
- (ii) Explain working of counterflow Ranque-Hilsch vortex tube refrigeration system with the help of a neat sketch. Also state its advantages.

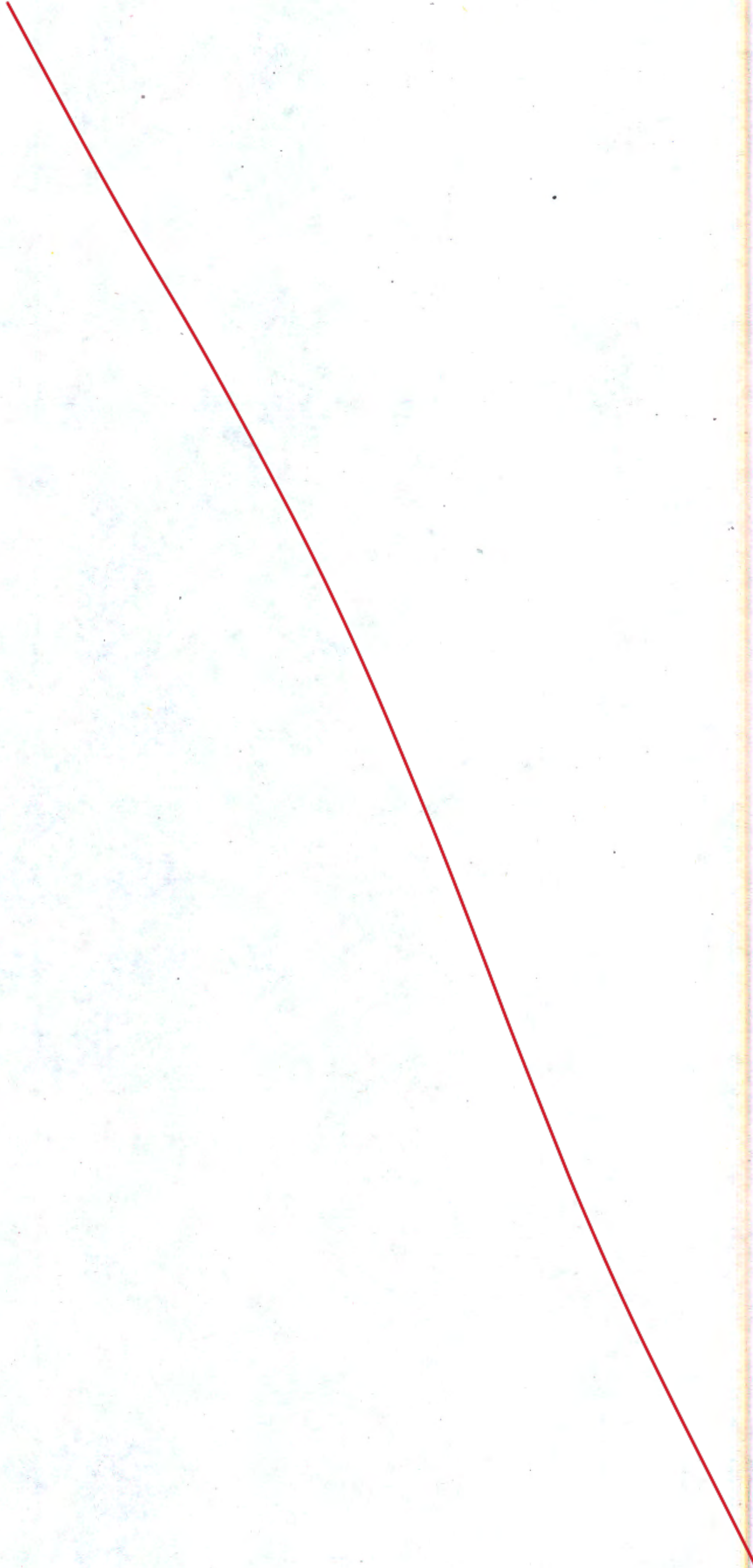
[10 + 10 marks]

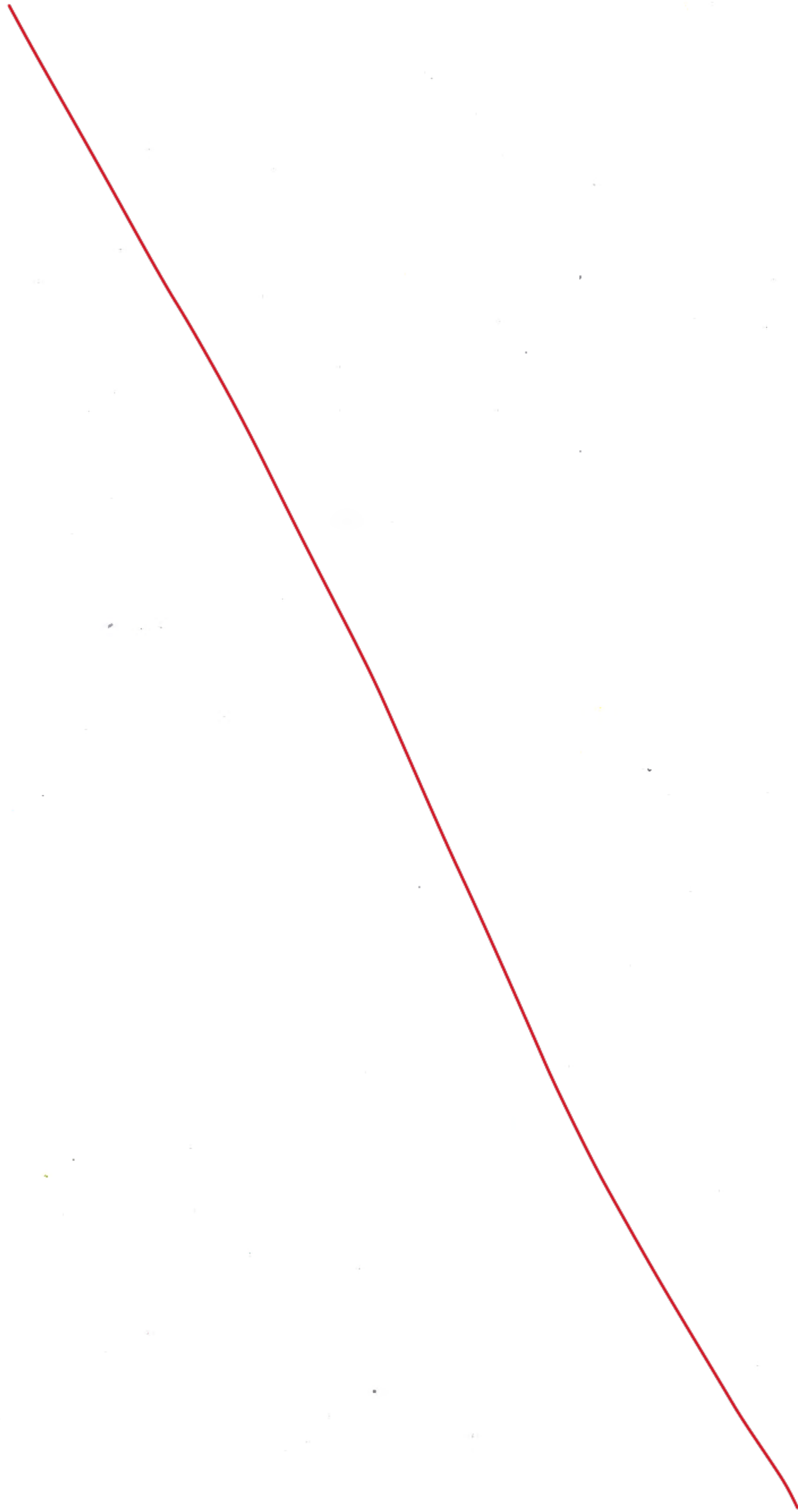




- Q.7 (c) An injection system consists of a pump plunger moving with a velocity of 0.35 m/s and connected to a fuel pipe which is 0.6m long and has a cross-sectional area  $\frac{1}{20}$  th of that of the plunger cylinder. The end of the pipe has an open nozzle having a hole of area which is  $\frac{1}{50}$  th of that of the pipe. The initial pressure in the line is 27 bar and the compression pressure of the engine is 30 bar. If the bulk modulus of the fuel is 1.8 GPa and the specific gravity of the oil is 0.85, then determine:
- The velocity of the pressure disturbances.
  - The time taken by the disturbance to travel through the pipe line.
  - The pressure and velocity at the pump end of the pipeline as the plunger moves.
  - The magnitude of the first reflected pressure and velocity wave.
  - The pressure and velocity at the orifice end of the pipe line after first reflection.

[20 marks]





The image shows handwritten work for a circuit problem. At the top left, there is a circuit diagram with a voltage source  $V_s$ , a resistor  $R_1$ , a dependent current source  $\beta i_1$ , and a resistor  $R_2$ . The dependent current source is controlled by the current  $i_1$  through  $R_1$ . A red diagonal line is drawn across the page.

Below the diagram, there are handwritten calculations:

For the left side of the circuit, the current  $i_1$  is calculated as:

$$i_1 = \frac{V_s}{R_1 + R_2} = \frac{100}{100 + 100} = 0.5 \text{ A}$$

For the right side of the circuit, the current  $i_2$  is calculated as:

$$i_2 = \frac{V_s}{R_2} = \frac{100}{100} = 1 \text{ A}$$

The dependent current source is  $\beta i_1$ . The total current  $i$  is the sum of  $i_1$  and  $\beta i_1$ :

$$i = i_1 + \beta i_1 = i_1(1 + \beta)$$

Substituting  $i_1 = 0.5$  A:

$$i = 0.5(1 + \beta)$$

The voltage  $V$  across  $R_2$  is:

$$V = i R_2 = 0.5(1 + \beta) \cdot 100 = 50(1 + \beta)$$

The power  $P$  is:

$$P = V i = 50(1 + \beta) \cdot 0.5(1 + \beta) = 25(1 + \beta)^2$$

For the right side of the circuit, the current  $i_2$  is:

$$i_2 = \frac{V}{R_2} = \frac{50(1 + \beta)}{100} = 0.5(1 + \beta)$$

The total current  $i$  is also  $i_2$ :

$$i = 0.5(1 + \beta)$$

The voltage  $V$  is:

$$V = i R_2 = 0.5(1 + \beta) \cdot 100 = 50(1 + \beta)$$

The power  $P$  is:

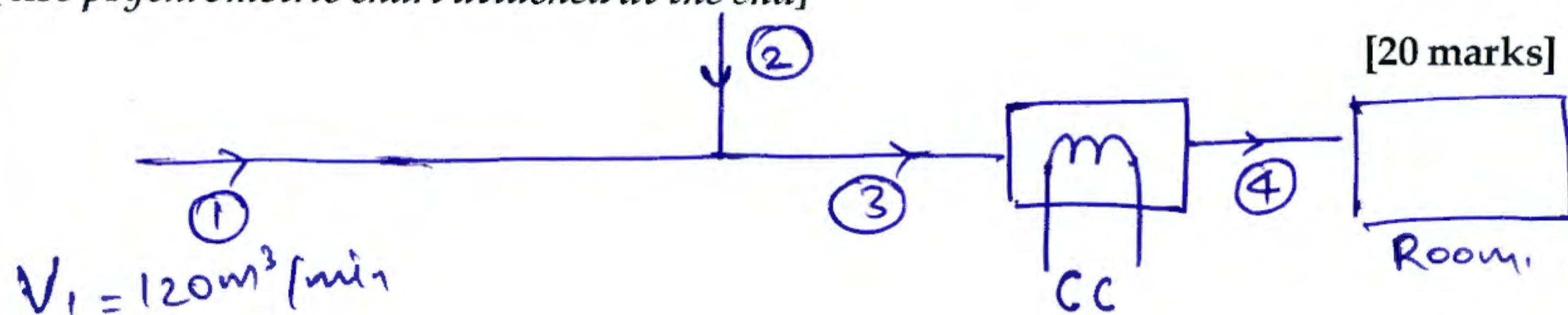
$$P = V i = 50(1 + \beta) \cdot 0.5(1 + \beta) = 25(1 + \beta)^2$$

The final answer is  $P = 25(1 + \beta)^2$ .

- Q.8 (a) Air flowing at the rate of  $120 \text{ m}^3/\text{min}$  at  $42^\circ\text{C}$  dry bulb temperature and 50% relative humidity is mixed with another stream flowing at the rate of  $30 \text{ m}^3/\text{min}$  at  $25^\circ\text{C}$  dry bulb temperature and 50% relative humidity. The mixture flows over a cooling coil whose apparatus dew point temperature is  $11^\circ\text{C}$  and bypass factor is 0.08. Find dry bulb temperature of air leaving the coil. If this air is supplied to an air conditioned room where dry bulb temperature of  $25^\circ\text{C}$  and relative humidity of 50% are maintained, estimate:

- (i) Room sensible heat factor  
(ii) Cooling load capacity of the coil in tonnes of refrigeration.

[Use psychrometric chart attached at the end]



$$\begin{aligned}
 V_1 &= 120 \text{ m}^3/\text{min} \\
 t_1 &= 42^\circ\text{C} \\
 h_1 &= 110 \text{ kJ/kg of da.} \\
 v_1 &= 0.93 \text{ m}^3/\text{kg da.} \\
 \dot{m}_{a1} &= \frac{V_1}{v_1} \\
 &= \frac{120}{0.93} = 129.03 \text{ kg/min}
 \end{aligned}$$

$$\begin{aligned}
 V_2 &= 30 \text{ m}^3/\text{min} \\
 t_2 &= 25^\circ\text{C} \\
 h_2 &= 50 \text{ kJ/kg of da.} \\
 v_2 &= 0.86 \text{ m}^3/\text{kg of da.} \\
 \dot{m}_{a2} &= \frac{30}{0.86} = 34.883 \text{ kg/min}
 \end{aligned}$$

$$\begin{aligned}
 \dot{m}_{a3} &= 163.91 \text{ kg/min} \\
 h_3 &= \frac{\dot{m}_{a1} h_1 + \dot{m}_{a2} h_2}{\dot{m}_{a1} + \dot{m}_{a2}}
 \end{aligned}$$

$$h_2 = 97.23 \text{ kJ/kg}$$

$$\begin{aligned}
 t_3 &= \frac{129.03 \times 42}{129.03 + 34.883} \\
 &\quad + \frac{34.883 \times 25}{129.03 + 34.883}
 \end{aligned}$$

$$t_3 = 36.807^\circ\text{C}$$

$$t_3 = 38.382^\circ\text{C}$$

$$t_{cc} = 11^\circ\text{C}$$

$$t_4 = 13.1905^\circ\text{C}$$

$$\begin{aligned}
 \text{BPF} &= 0.08 \\
 \frac{t_4 - t_{cc}}{t_3 - t_{cc}} &= 0.08
 \end{aligned}$$

$$\begin{aligned}
 \frac{t_4 - 11}{38.382 - 11} &= 0.08
 \end{aligned}$$

∴ from pt 4 air will directly go to Room

$$RSH = 65 - 50 = 15 \text{ kJ/kg of da.}$$

$$RLH = 97.23 - 65 \\ = 32.23 \text{ kJ/kg of da}$$

$$RSHF = \frac{RSH}{RTH} = \frac{15}{97.23 - 50}$$

$$RSHF = 0.3175$$

Ans

Cooling load Capacity of cooling coil

$$= \dot{m} [h_4 + h_3]$$

$$h_4 \text{ from chart} = 37 \text{ kJ/kg of da.}$$

$$CL \text{ of cooling coil} = \frac{163.91 \times (97.23 - 37)}{60 \times 3.5} \text{ tons}$$

$$\text{Cooling load Capacity of cooling coil} = \underline{\underline{47 \text{ tons}}}$$

Ans

16

*[Faint handwritten text, possibly bleed-through from the reverse side of the page. A prominent red diagonal line is drawn across the page.]*

Q.8 (b) A single-cylinder two-stroke SI engine has 90 mm diameter bore and 120 mm stroke, and the compression ratio is 10. The exhaust port opens  $55^\circ$  before BDC and closes  $55^\circ$  after BDC. The air-fuel ratio is 14.8:1. The temperature of the fresh mixture entering the engine is 310K, and the pressure in the cylinder at the time of closing exhaust port is 1.02 bar. Air supplied to the engine is 190 kg/h. The engine runs at 4200 rpm. Take  $R$  for mixture = 287 J/kg·K. Considering the effective stroke, calculate:

- Scavenging ratio
- Scavenging efficiency
- Trapping efficiency

[20 marks]

single cylinder, 2 stroke

$$D = 0.09$$

$$L = 0.12$$

$$r = 10$$

$$\theta_{\text{ex}} = 110^\circ \times \pi / 180$$

$$A/F = 14.8:1$$

$$T_1 = 310 \text{ K}$$

$$P_1 = 1.02 \text{ bar}$$

$$\dot{m}_a = 190 \text{ kg/h}$$

$$A/F = 14.8$$

$$\frac{\dot{m}_a}{\dot{m}_f} = 14.8$$

$$\dot{m}_f = \frac{190}{14.8} = 12.837 \text{ kg/h}$$

$$\dot{m}_{\text{total}} = 190 + 12.8378$$

$$= 202.8378 \text{ kg/h}$$

Scavenging Ratio

$$R = \frac{\dot{m}_{\text{total}}}{\dot{m}_{\text{ideal}}}$$

=

$$\dot{m}_{\text{ideal}} = \frac{PV}{RT}$$

$$= \frac{102 \times \frac{\pi}{4} \times 0.09^2 \times 0.12 \times 4200}{60 \times 0.287 \times 310}$$

$$= \frac{102 \times 0.053438}{0.287 \times 310}$$

$$= 0.06126 \text{ kg/s}$$

$$= 220.55 \text{ kg/h}$$

4

$$= \frac{202.83}{220.55}$$

$$R = 0.9196 \quad \text{Ans}$$

$$\text{Scavenging Efficiency} = 1 - e^{-R}$$

$$R_{sc} = 0.60133 \quad \text{Ans}$$

$$\text{Trapping Efficiency} = \frac{R_{sc}}{R}$$

$$= \frac{0.60133}{0.9196}$$

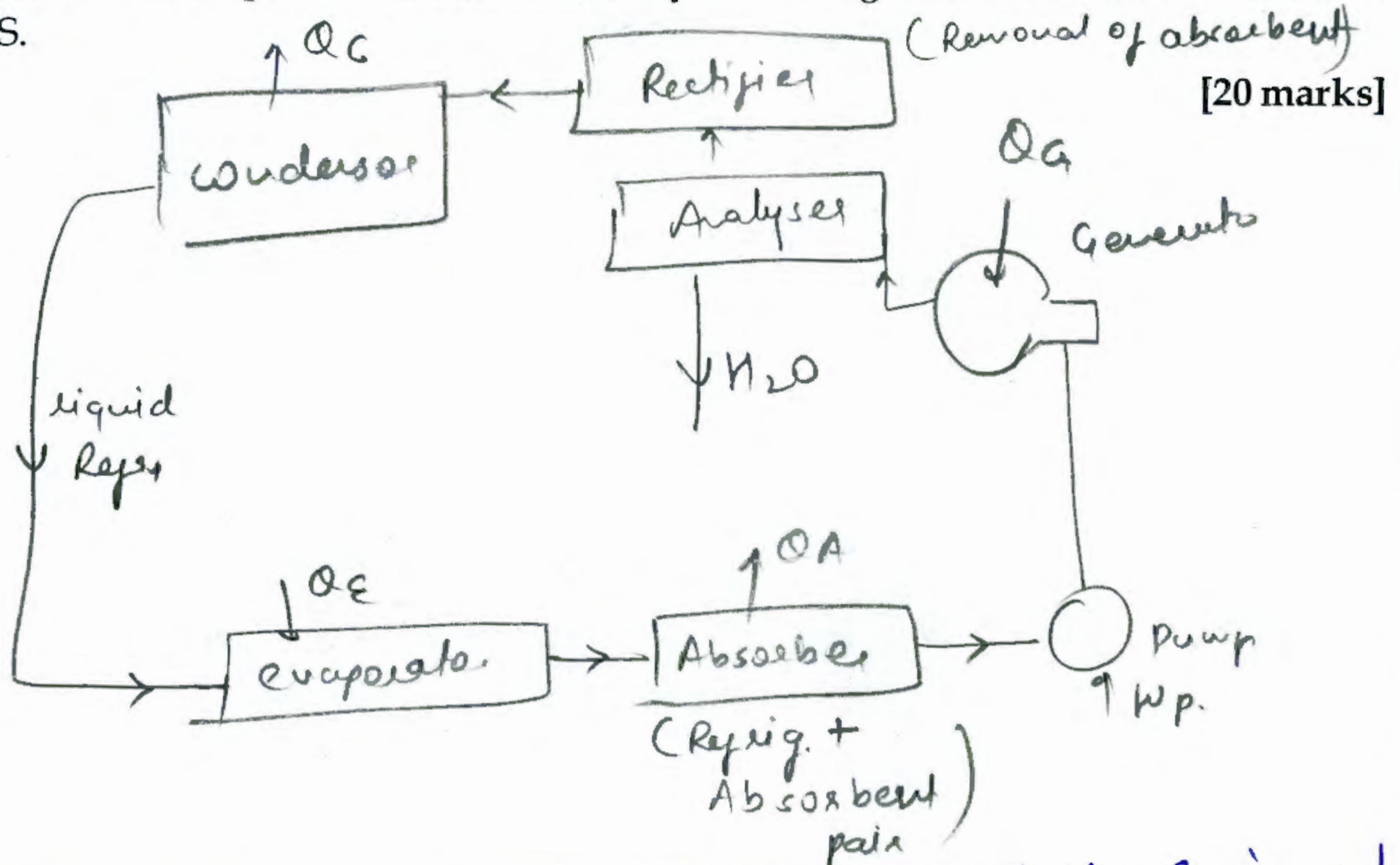
$$\text{Trap. eff} = 0.65391 \quad \text{Ans}$$

*[Faint, illegible handwritten text, possibly bleed-through from the reverse side of the page.]*

$$\textcircled{1} \rightarrow 10 + 20 = 30$$

$$\textcircled{1} \rightarrow \frac{10 + 20}{27} = \frac{30}{27} = \frac{10}{9}$$

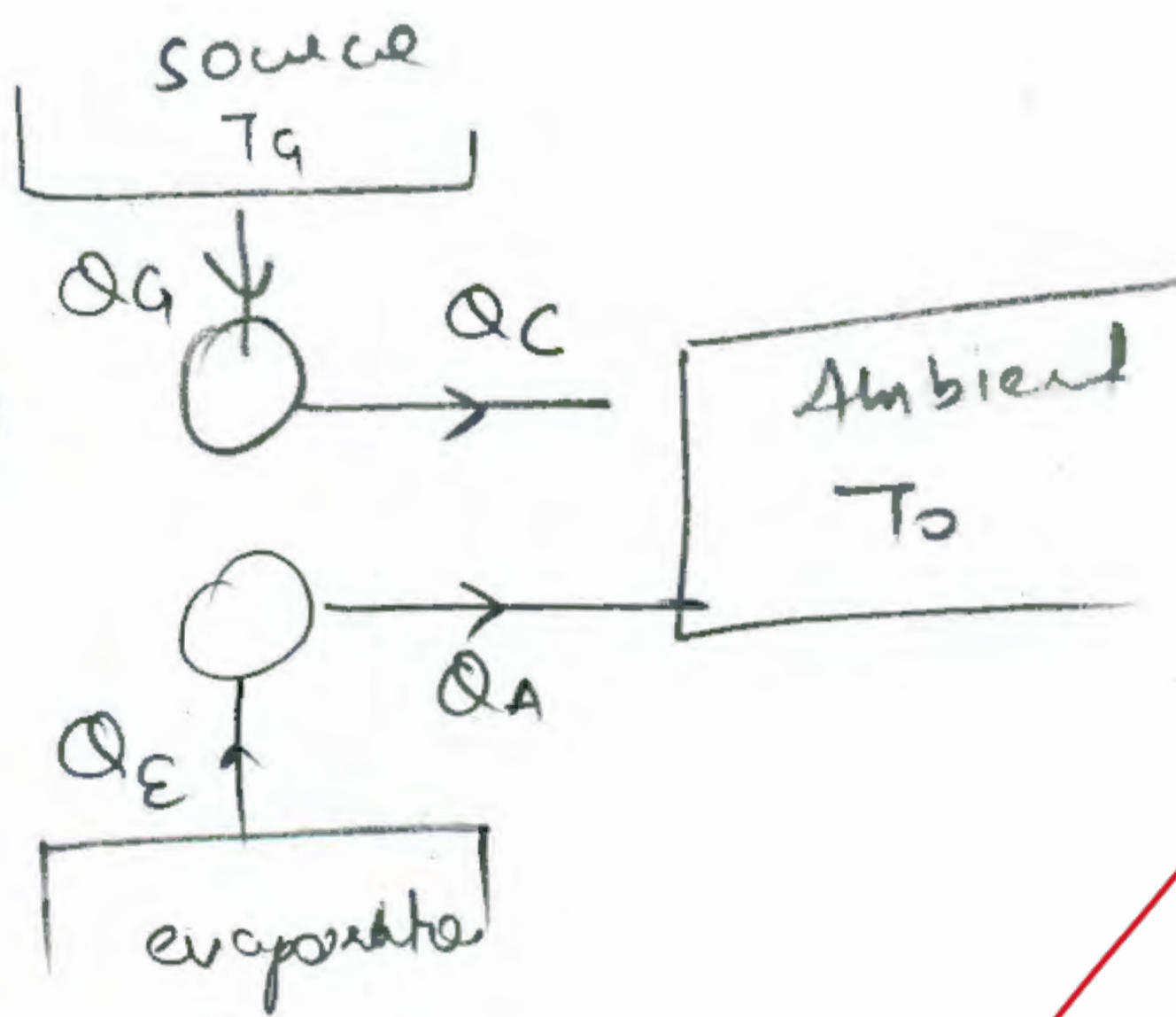
Q.8 (c) Discuss the working principle of practical vapour absorption system with a neat sketch. Derive the expression for its COP. Also discuss the desirable properties of an ideal refrigerant-absorbent pair and list the commonly used refrigerant-absorbent combinations in VARS.



VARS is a low grade energy operated Refrigerant system. In this system refrigerant & Absorbent pair used for creating the cooling effect. Generally  $NH_3-H_2O$  &  $H_2O-LiBr$  pair used for VARS system. In this Ammonia used as refrigerant & water used as absorbent.

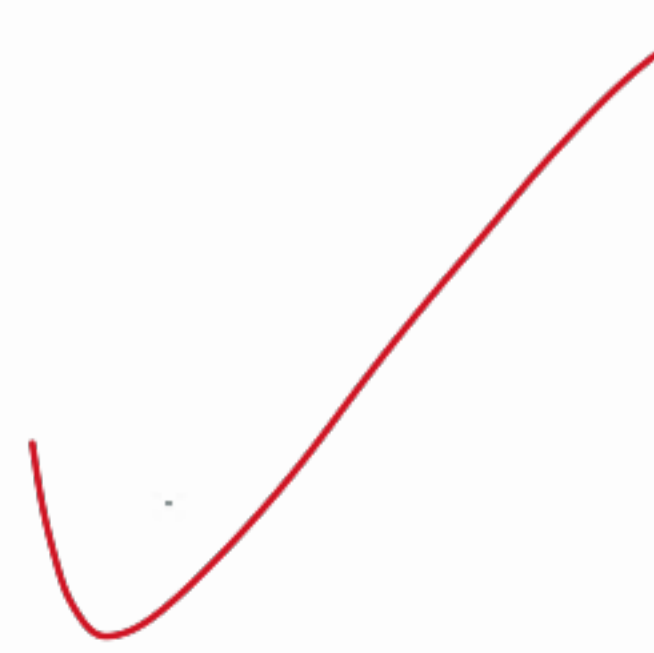
∴ By energy Balance

$$Q_G + Q_E = Q_C + Q_A \quad \text{--- (1)}$$



& Now by entropy principle

$$\frac{Q_G}{T_G} + \frac{Q_E}{T_E} = \frac{Q_C + Q_A}{T_0} \quad \text{--- (2)}$$



$$\text{COP} = \frac{DE}{W_{in}} = \frac{Q_E}{Q_G + Q_E} \quad (\text{energy})$$

$$= \frac{Q_E}{Q_G}$$

from (2)

$$\frac{Q_G}{T_G} + \frac{Q_E}{T_E} = \frac{Q_G + Q_E}{T_0}$$

$$\frac{Q_G}{T_G} - \frac{Q_G}{T_0} = \frac{Q_E}{T_0} - \frac{Q_E}{T_E}$$

$$Q_G \left( \frac{T_0 - T_G}{T_G T_0} \right) = \frac{Q_E (T_E - T_0)}{T_0 T_E}$$

$$Q_G \left( \frac{T_0 - T_G}{T_G} \right) = Q_E \left( \frac{T_E - T_0}{T_E} \right)$$

$$\frac{Q_E}{Q_G} = \frac{T_E}{T_G} \times \frac{T_0 - T_G}{T_E - T_0}$$

$$\frac{Q_E}{Q_G} = \frac{T_E}{T_G} \times \frac{(T_G - T_0)}{(T_0 - T_E)}$$

Hence

$$\text{COP} = \left( \frac{T_E}{T_0 - T_E} \right) \times \left( \frac{T_G - T_0}{T_G} \right)$$

Ans

Desired property of Ideal Refrigerant - absorbent pair :-

- ① It should be non toxic
- ② It should be non flammable
- ③ It should have lower operating temp.

④ It should be non reactive to the systems components

⑤ Refrigerant & Absorbent should be completely miscible & immiscible at particular temp<sup>r</sup> & pressure.

⑥ Easy leakage detection

~~⑦~~  
Commonly used Ref. absorbent pair

①  $\text{NH}_3 - \text{H}_2\text{O}$   
↓                      ↓  
Refrigerant           Absorbent

②  $\text{H}_2\text{O} - \text{LiBr}$   
↓                      ↓  
Refrigerant           Absorbent

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Saturated Water and Steam (Temperature-based)

T °C	p <sub>sat</sub> MPa	Volume, m <sup>3</sup> /kg		Energy, kJ/kg		Enthalpy, kJ/kg			Entropy, kJ/(kg K)		
		v <sub>f</sub>	v <sub>g</sub>	u <sub>f</sub>	u <sub>g</sub>	h <sub>f</sub>	h <sub>g</sub>	h <sub>fg</sub>	s <sub>f</sub>	s <sub>g</sub>	s <sub>fg</sub>
0.01	0.0006117	0.00100021	205.991	0	2374.9	0.00	2500.9	2500.9	0	9.1555	9.1555
1	0.0006571	0.00100015	192.439	4.18	2376.2	4.18	2502.7	2498.6	0.01526	9.1291	9.1138
2	0.0007060	0.00100011	179.758	8.39	2377.7	8.39	2504.6	2496.2	0.03061	9.1027	9.0720
3	0.0007581	0.00100008	168.008	12.60	2379.0	12.60	2506.4	2493.8	0.04589	9.0765	9.0306
4	0.0008135	0.00100007	157.116	16.81	2380.4	16.81	2508.2	2491.4	0.06110	9.0505	8.9894
5	0.0008726	0.00100008	147.011	21.02	2381.8	21.02	2510.1	2489.0	0.07625	9.0248	8.9486
6	0.0009354	0.00100011	137.633	25.22	2383.2	25.22	2511.9	2486.7	0.09134	8.9993	8.9080
7	0.0010021	0.00100014	128.923	29.43	2384.5	29.43	2513.7	2484.3	0.10637	8.9741	8.8677
8	0.0010730	0.00100020	120.829	33.63	2386.0	33.63	2515.6	2481.9	0.12133	8.9491	8.8278
9	0.0011483	0.00100026	113.304	37.82	2387.3	37.82	2517.4	2479.6	0.13624	8.9243	8.7881
10	0.0012282	0.00100035	106.303	42.02	2388.6	42.02	2519.2	2477.2	0.15109	8.8998	8.7487
11	0.0013130	0.00100044	99.787	46.22	2390.0	46.22	2521.0	2474.8	0.16587	8.8754	8.7096
12	0.0014028	0.00100055	93.719	50.41	2391.4	50.41	2522.9	2472.5	0.18061	8.8513	8.6707
13	0.0014981	0.00100067	88.064	54.60	2392.8	54.60	2524.7	2470.1	0.19528	8.8274	8.6321
14	0.0015990	0.00100080	82.793	58.79	2394.1	58.79	2526.5	2467.7	0.20990	8.8037	8.5938
15	0.0017058	0.00100094	77.875	62.98	2395.5	62.98	2528.3	2465.4	0.22446	8.7803	8.5558
16	0.0018188	0.00100110	73.286	67.17	2396.9	67.17	2530.2	2463.0	0.23897	8.7570	8.5180
17	0.0019384	0.00100127	69.001	71.36	2398.2	71.36	2532.0	2460.6	0.25343	8.7339	8.4805
18	0.0020647	0.00100145	64.998	75.54	2399.6	75.54	2533.8	2458.3	0.26783	8.7111	8.4433
19	0.0021983	0.00100164	61.256	79.73	2400.9	79.73	2535.6	2455.9	0.28218	8.6884	8.4063
20	0.0023393	0.00100184	57.757	83.91	2402.3	83.91	2537.4	2453.5	0.29648	8.6660	8.3695
21	0.0024882	0.00100205	54.483	88.10	2403.7	88.10	2539.3	2451.2	0.31073	8.6437	8.3330
22	0.0026453	0.00100228	51.418	92.28	2405.1	92.28	2541.1	2448.8	0.32493	8.6217	8.2967
23	0.0028111	0.00100251	48.548	96.46	2406.4	96.46	2542.9	2446.4	0.33908	8.5998	8.2607
24	0.0029858	0.00100275	45.858	100.65	2407.8	100.65	2544.7	2444.0	0.35318	8.5781	8.2250
25	0.0031699	0.00100301	43.337	104.83	2409.1	104.83	2546.5	2441.7	0.36722	8.5566	8.1894
26	0.0033639	0.00100327	40.973	109.01	2410.5	109.01	2548.3	2439.3	0.38123	8.5353	8.1541
27	0.0035681	0.00100354	38.754	113.19	2411.8	113.19	2550.1	2436.9	0.39518	8.5142	8.1191
28	0.0037831	0.00100382	36.672	117.37	2413.2	117.37	2551.9	2434.6	0.40908	8.4933	8.0842
29	0.0040092	0.00100411	34.716	121.55	2414.5	121.55	2553.7	2432.2	0.42294	8.4725	8.0496
30	0.0042470	0.00100441	32.878	125.73	2415.9	125.73	2555.5	2429.8	0.43675	8.4520	8.0152
31	0.0044969	0.00100472	31.151	129.91	2417.2	129.91	2557.3	2427.4	0.45052	8.4316	7.9810
32	0.0047596	0.00100504	29.526	134.09	2418.7	134.09	2559.2	2425.1	0.46424	8.4113	7.9471
33	0.0050354	0.00100537	27.998	138.26	2420.0	138.27	2561.0	2422.7	0.47792	8.3913	7.9134
34	0.0053251	0.00100570	26.560	142.44	2421.4	142.45	2562.8	2420.3	0.49155	8.3714	7.8799
35	0.0056290	0.00100605	25.205	146.62	2422.6	146.63	2564.5	2417.9	0.50513	8.3517	7.8466
36	0.0059479	0.00100640	23.929	150.80	2424.0	150.81	2566.3	2415.5	0.51867	8.3321	7.8135
37	0.0062823	0.00100676	22.727	154.98	2425.3	154.99	2568.1	2413.1	0.53217	8.3127	7.7806
38	0.0066328	0.00100713	21.593	159.16	2426.7	159.17	2569.9	2410.8	0.54562	8.2935	7.7479
39	0.0070002	0.00100750	20.524	163.34	2428.0	163.35	2571.7	2408.4	0.55903	8.2745	7.7154
40	0.0073849	0.00100789	19.515	167.52	2429.4	167.53	2573.5	2406.0	0.57240	8.2555	7.6831

Continued ...

Saturated Water and Steam (Pressure-based)

$p_{tp} = 611.657 \text{ Pa} = 0.000611657 \text{ MPa}$

$p$ MPa	$T_{\text{sat}}$ °C	Volume, m <sup>3</sup> /kg		Energy, kJ/kg		Enthalpy, kJ/kg			Entropy, kJ/(kg K)		
		$v_f$	$v_g$	$u_f$	$u_g$	$h_f$	$h_g$	$h_{fg}$	$s_f$	$s_g$	$s_{fg}$
$p_{tp}$	<b>0.01</b>	0.00100021	205.991	<b>0</b>	2374.9	0.00	2500.9	2500.9	<b>0</b>	9.1555	9.1555
0.0007	1.881	0.00100011	181.217	7.89	2377.4	7.89	2504.3	2496.5	0.02878	9.1058	9.0770
0.0008	3.761	0.00100008	159.640	15.81	2380.1	15.81	2507.8	2492.0	0.05748	9.0567	8.9992
0.0009	5.444	0.00100009	142.757	22.89	2382.4	22.89	2510.9	2488.0	0.08297	9.0135	8.9305
0.0010	6.970	0.00100014	129.178	29.30	2384.5	29.30	2513.7	2484.4	0.10591	8.9749	8.8690
0.0012	9.654	0.00100032	108.670	40.57	2388.2	40.57	2518.6	2478.0	0.14595	8.9082	8.7623
0.0014	11.969	0.00100054	93.899	50.28	2391.3	50.28	2522.8	2472.5	0.18015	8.8521	8.6719
0.0016	14.010	0.00100080	82.743	58.83	2394.1	58.83	2526.5	2467.7	0.21004	8.8035	8.5935
0.0018	15.837	0.00100108	74.011	66.49	2396.7	66.49	2529.9	2463.4	0.23662	8.7608	8.5241
0.0020	17.495	0.00100136	66.987	73.43	2398.9	73.43	2532.9	2459.4	0.26056	8.7226	8.4620
0.0024	20.414	0.00100193	56.375	85.65	2402.9	85.65	2538.2	2452.5	0.30239	8.6567	8.3544
0.0028	22.935	0.00100249	48.729	96.19	2406.4	96.19	2542.8	2446.6	0.33816	8.6012	8.2631
0.0032	25.158	0.00100305	42.952	105.49	2409.4	105.49	2546.8	2441.3	0.36945	8.5533	8.1838
0.0036	27.152	0.00100358	38.430	113.83	2412.1	113.83	2550.4	2436.6	0.39729	8.5110	8.1138
0.0040	28.960	0.00100410	34.791	121.39	2414.5	121.39	2553.7	2432.3	0.42239	8.4734	8.0510
0.0045	31.012	0.00100473	31.131	129.96	2417.3	129.96	2557.4	2427.4	0.45069	8.4313	7.9806
0.0050	32.874	0.00100533	28.185	137.74	2419.8	137.75	2560.7	2423.0	0.47620	8.3938	7.9176
0.0055	34.581	0.00100590	25.762	144.87	2422.1	144.88	2563.8	2418.9	0.49945	8.3599	7.8605
0.0060	36.159	0.00100645	23.733	151.47	2424.2	151.48	2566.6	2415.2	0.52082	8.3290	7.8082
0.0065	37.627	0.00100699	22.009	157.60	2426.2	157.61	2569.3	2411.6	0.54060	8.3007	7.7601
0.0070	39.000	0.00100750	20.524	163.34	2428.0	163.35	2571.7	2408.4	0.55903	8.2745	7.7154
0.0075	40.290	0.00100800	19.233	168.74	2429.8	168.75	2574.0	2405.3	0.57627	8.2501	7.6738
0.0080	41.509	0.00100848	18.099	173.83	2431.4	173.84	2576.2	2402.4	0.59249	8.2273	7.6348
0.0085	42.663	0.00100895	17.095	178.66	2433.0	178.67	2578.3	2399.6	0.60780	8.2060	7.5982
0.0090	43.761	0.00100940	16.199	183.24	2434.4	183.25	2580.2	2397.0	0.62230	8.1858	7.5635
0.0095	44.807	0.00100984	15.396	187.62	2435.8	187.63	2582.1	2394.5	0.63607	8.1668	7.5308
0.010	45.806	0.00101027	14.670	191.80	2437.2	191.81	2583.9	2392.1	0.64920	8.1488	7.4996
0.011	47.683	0.00101110	13.412	199.64	2439.7	199.65	2587.2	2387.5	0.67372	8.1154	7.4417
0.012	49.419	0.00101188	12.358	206.90	2442.0	206.91	2590.3	2383.4	0.69628	8.0849	7.3887
0.013	51.034	0.00101263	11.462	213.66	2444.1	213.67	2593.1	2379.4	0.71717	8.0570	7.3398
0.014	52.547	0.00101335	10.691	219.98	2446.1	219.99	2595.8	2375.8	0.73664	8.0311	7.2945
0.016	55.313	0.00101471	9.4306	231.55	2449.7	231.57	2600.6	2369.1	0.77201	7.9846	7.2126
0.018	57.798	0.00101597	8.4431	241.94	2453.0	241.96	2605.0	2363.0	0.80355	7.9437	7.1402
0.020	60.058	0.00101716	7.6480	251.40	2455.9	251.42	2608.9	2357.5	0.83202	7.9072	7.0752
0.024	64.053	0.00101934	6.4453	268.13	2461.2	268.15	2615.9	2347.7	0.88191	7.8442	6.9623
0.028	67.518	0.00102131	5.5778	282.63	2465.6	282.66	2621.8	2339.2	0.92472	7.7912	6.8664
0.032	70.586	0.00102312	4.9215	295.49	2469.6	295.52	2627.1	2331.6	0.96228	7.7453	6.7830
0.036	73.345	0.00102480	4.4072	307.05	2473.1	307.09	2631.8	2324.7	0.99579	7.7050	6.7092
0.040	75.857	0.00102638	3.9930	317.58	2476.4	317.62	2636.1	2318.4	1.0261	7.6690	6.6429
0.045	78.715	0.00102821	3.5759	329.57	2480.0	329.62	2640.9	2311.2	1.0603	7.6288	6.5686
0.050	81.317	0.00102993	3.2400	340.49	2483.2	340.54	2645.2	2304.7	1.0912	7.5930	6.5018

Continued ...

Saturated Water and Steam (Pressure-based), Contd.

$p$ MPa	$T_{\text{sat}}$ °C	Volume, m <sup>3</sup> /kg		Energy, kJ/kg		Enthalpy, kJ/kg			Entropy, kJ/(kg K)		
		$v_f$	$v_g$	$u_f$	$u_g$	$h_f$	$h_g$	$h_{fg}$	$s_f$	$s_g$	$s_{fg}$
0.050	81.317	0.00102993	3.2400	340.49	2483.2	340.54	2645.2	2304.7	1.0912	7.5930	6.5018
0.055	83.709	0.00103154	2.9635	350.53	2486.2	350.59	2649.2	2298.6	1.1194	7.5606	6.4412
0.060	85.926	0.00103307	2.7317	359.85	2489.0	359.91	2652.9	2292.9	1.1454	7.5311	6.3857
0.065	87.993	0.00103452	2.5346	368.53	2491.6	368.60	2656.3	2287.7	1.1696	7.5040	6.3345
0.070	89.932	0.00103590	2.3648	376.68	2493.9	376.75	2659.4	2282.7	1.1921	7.4790	6.2869
0.075	91.758	0.00103723	2.2170	384.36	2496.1	384.44	2662.4	2277.9	1.2132	7.4557	6.2425
0.080	93.486	0.00103850	2.0871	391.63	2498.2	391.71	2665.2	2273.5	1.2330	7.4339	6.2009
0.085	95.125	0.00103972	1.9720	398.53	2500.2	398.62	2667.8	2269.2	1.2518	7.4135	6.1617
0.090	96.687	0.00104091	1.8694	405.11	2502.1	405.20	2670.3	2265.1	1.2696	7.3943	6.1246
0.095	98.178	0.00104205	1.7772	411.38	2503.9	411.48	2672.7	2261.2	1.2866	7.3761	6.0895
0.10	99.606	0.00104315	1.6939	417.40	2505.5	417.50	2674.9	2257.4	1.3028	7.3588	6.0561
0.11	102.292	0.00104527	1.5495	428.73	2508.8	428.84	2679.2	2250.3	1.3330	7.3269	5.9938
0.12	104.784	0.00104727	1.4284	439.23	2511.7	439.36	2683.1	2243.7	1.3609	7.2977	5.9367
0.13	107.109	0.00104917	1.3253	449.05	2514.3	449.19	2686.6	2237.5	1.3868	7.2709	5.8840
0.14	109.292	0.00105099	1.2366	458.27	2516.9	458.42	2690.0	2231.6	1.4110	7.2461	5.8351
0.15	111.349	0.00105273	1.1593	466.97	2519.2	467.13	2693.1	2226.0	1.4337	7.2230	5.7893
0.16	113.297	0.00105440	1.0914	475.21	2521.4	475.38	2696.0	2220.7	1.4551	7.2014	5.7463
0.17	115.148	0.00105600	1.0312	483.04	2523.5	483.22	2698.8	2215.6	1.4753	7.1812	5.7059
0.18	116.911	0.00105756	0.97747	490.51	2525.5	490.70	2701.4	2210.7	1.4945	7.1621	5.6676
0.19	118.596	0.00105906	0.92924	497.65	2527.3	497.85	2703.9	2206.0	1.5127	7.1440	5.6313
0.20	120.210	0.00106052	0.88568	504.49	2529.1	504.70	2706.2	2201.5	1.5302	7.1269	5.5967
0.21	121.759	0.00106193	0.84614	511.07	2530.8	511.29	2708.5	2197.2	1.5469	7.1106	5.5638
0.22	123.250	0.00106330	0.81007	517.40	2532.4	517.63	2710.6	2193.0	1.5628	7.0951	5.5323
0.23	124.686	0.00106464	0.77704	523.50	2534.0	523.74	2712.7	2188.9	1.5782	7.0803	5.5021
0.24	126.072	0.00106594	0.74668	529.38	2535.4	529.64	2714.6	2185.0	1.5930	7.0661	5.4731
0.25	127.411	0.00106722	0.71866	535.07	2536.8	535.34	2716.5	2181.1	1.6072	7.0524	5.4452
0.26	128.708	0.00106846	0.69273	540.59	2538.2	540.87	2718.3	2177.4	1.6210	7.0394	5.4184
0.27	129.965	0.00106968	0.66865	545.95	2539.5	546.24	2720.0	2173.8	1.6343	7.0268	5.3925
0.28	131.185	0.00107086	0.64624	551.14	2540.8	551.44	2721.7	2170.3	1.6471	7.0146	5.3675
0.29	132.370	0.00107203	0.62533	556.19	2542.0	556.50	2723.3	2166.8	1.6596	7.0029	5.3433
0.30	133.522	0.00107317	0.60576	561.11	2543.2	561.43	2724.9	2163.5	1.6717	6.9916	5.3199
0.31	134.644	0.00107429	0.58741	565.89	2544.3	566.22	2726.4	2160.2	1.6835	6.9807	5.2972
0.32	135.737	0.00107539	0.57017	570.56	2545.3	570.90	2727.8	2157.0	1.6949	6.9701	5.2752
0.33	136.802	0.00107647	0.55395	575.10	2546.5	575.46	2729.3	2153.8	1.7060	6.9598	5.2538
0.34	137.842	0.00107753	0.53864	579.54	2547.5	579.91	2730.6	2150.7	1.7168	6.9498	5.2330
0.35	138.857	0.00107857	0.52418	583.88	2548.5	584.26	2732.0	2147.7	1.7274	6.9401	5.2128
0.36	139.849	0.00107960	0.51050	588.13	2549.4	588.52	2733.2	2144.7	1.7377	6.9307	5.1931
0.37	140.819	0.00108061	0.49753	592.28	2550.4	592.68	2734.5	2141.8	1.7477	6.9216	5.1739
0.38	141.769	0.00108161	0.48522	596.34	2551.3	596.75	2735.7	2139.0	1.7575	6.9126	5.1551
0.39	142.698	0.00108259	0.47352	600.32	2552.2	600.74	2736.9	2136.2	1.7671	6.9040	5.1369
0.40	143.608	0.00108355	0.46238	604.22	2553.1	604.65	2738.1	2133.4	1.7765	6.8955	5.1190

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Saturated Water and Steam (Pressure-based), Contd.

$p$ MPa	$T_{\text{sat}}$ °C	Volume, m <sup>3</sup> /kg		Energy, kJ/kg		Enthalpy, kJ/kg			Entropy, kJ/(kg K)		
		$v_f$	$v_g$	$u_f$	$u_g$	$h_f$	$h_g$	$h_{fg}$	$s_f$	$s_g$	$s_{fg}$
0.40	143.608	0.00108355	0.46238	604.22	2553.1	604.65	2738.1	2133.4	1.7765	6.8955	5.1190
0.42	145.375	0.00108544	0.44165	611.79	2554.8	612.25	2740.3	2128.0	1.7946	6.8791	5.0846
0.44	147.076	0.00108729	0.42274	619.10	2556.4	619.58	2742.4	2122.8	1.8120	6.8636	5.0516
0.46	148.716	0.00108908	0.40542	626.14	2557.9	626.64	2744.4	2117.7	1.8287	6.8487	5.0199
0.48	150.300	0.00109084	0.38950	632.95	2559.3	633.47	2746.3	2112.8	1.8448	6.8344	4.9895
0.50	151.831	0.00109255	0.37481	639.54	2560.7	640.09	2748.1	2108.0	1.8604	6.8207	4.9603
0.52	153.314	0.00109423	0.36120	645.93	2562.1	646.50	2749.9	2103.4	1.8754	6.8075	4.9321
0.54	154.753	0.00109587	0.34858	652.13	2563.3	652.72	2751.5	2098.8	1.8899	6.7948	4.9049
0.56	156.149	0.00109748	0.33682	658.16	2564.5	658.77	2753.1	2094.4	1.9040	6.7825	4.8786
0.58	157.506	0.00109905	0.32585	664.01	2565.7	664.65	2754.7	2090.0	1.9176	6.7707	4.8531
0.60	158.826	0.00110060	0.31558	669.72	2566.8	670.38	2756.1	2085.8	1.9308	6.7592	4.8284
0.62	160.112	0.00110212	0.30596	675.28	2567.9	675.96	2757.6	2081.6	1.9437	6.7482	4.8045
0.64	161.365	0.00110362	0.29691	680.70	2568.9	681.41	2758.9	2077.5	1.9562	6.7374	4.7813
0.66	162.587	0.00110509	0.28840	686.00	2570.0	686.73	2760.3	2073.5	1.9684	6.7270	4.7587
0.68	163.781	0.00110654	0.28036	691.17	2570.9	691.92	2761.5	2069.6	1.9802	6.7169	4.7367
0.70	164.946	0.00110796	0.27277	696.22	2571.9	697.00	2762.8	2065.8	1.9918	6.7071	4.7153
0.72	166.086	0.00110936	0.26559	701.17	2572.7	701.97	2763.9	2062.0	2.0031	6.6975	4.6944
0.74	167.200	0.00111075	0.25879	706.02	2573.6	706.84	2765.1	2058.2	2.0141	6.6882	4.6741
0.76	168.291	0.00111211	0.25233	710.76	2574.4	711.61	2766.2	2054.6	2.0248	6.6791	4.6543
0.78	169.360	0.00111346	0.24618	715.41	2575.3	716.28	2767.3	2051.0	2.0354	6.6703	4.6349
0.80	170.406	0.00111478	0.24034	719.97	2576.0	720.86	2768.3	2047.4	2.0457	6.6616	4.6160
0.82	171.433	0.00111609	0.23477	724.44	2576.8	725.36	2769.3	2043.9	2.0557	6.6532	4.5975
0.84	172.440	0.00111739	0.22946	728.84	2577.6	729.78	2770.3	2040.5	2.0656	6.6449	4.5793
0.86	173.428	0.00111867	0.22438	733.15	2578.2	734.11	2771.2	2037.1	2.0753	6.6369	4.5616
0.88	174.398	0.00111993	0.21953	737.38	2578.9	738.37	2772.1	2033.8	2.0847	6.6290	4.5443
0.90	175.350	0.00112118	0.21489	741.55	2579.6	742.56	2773.0	2030.5	2.0940	6.6213	4.5272
0.92	176.287	0.00112242	0.21044	745.65	2580.3	746.68	2773.9	2027.2	2.1032	6.6137	4.5106
0.94	177.207	0.00112364	0.20617	749.67	2580.9	750.73	2774.7	2024.0	2.1121	6.6063	4.4942
0.96	178.112	0.00112485	0.20208	753.64	2581.5	754.72	2775.5	2020.8	2.1209	6.5991	4.4782
0.98	179.002	0.00112605	0.19814	757.55	2582.1	758.65	2776.3	2017.7	2.1296	6.5920	4.4624
1.00	179.878	0.00112723	0.19436	761.39	2582.7	762.52	2777.1	2014.6	2.1381	6.5850	4.4470
1.05	182.009	0.00113014	0.18552	770.75	2584.1	771.94	2778.9	2007.0	2.1587	6.5681	4.4095
1.10	184.062	0.00113299	0.17745	779.78	2585.4	781.03	2780.6	1999.6	2.1785	6.5520	4.3735
1.15	186.043	0.00113577	0.17006	788.51	2586.6	789.82	2782.2	1992.4	2.1976	6.5365	4.3390
1.20	187.957	0.00113850	0.16326	796.96	2587.8	798.33	2783.7	1985.4	2.2159	6.5217	4.3058
1.25	189.809	0.00114118	0.15699	805.15	2588.9	806.58	2785.1	1978.6	2.2337	6.5074	4.2737
1.30	191.605	0.00114380	0.15119	813.11	2590.0	814.60	2786.5	1971.9	2.2508	6.4936	4.2428
1.35	193.347	0.00114638	0.14580	820.84	2590.9	822.39	2787.7	1965.3	2.2674	6.4803	4.2129
1.40	195.039	0.00114892	0.14078	828.36	2591.7	829.97	2788.8	1958.9	2.2835	6.4675	4.1839
1.45	196.685	0.00115141	0.13609	835.68	2592.6	837.35	2789.9	1952.6	2.2992	6.4550	4.1559
1.50	198.287	0.00115387	0.13171	842.83	2593.4	844.56	2791.0	1946.4	2.3143	6.4430	4.1286

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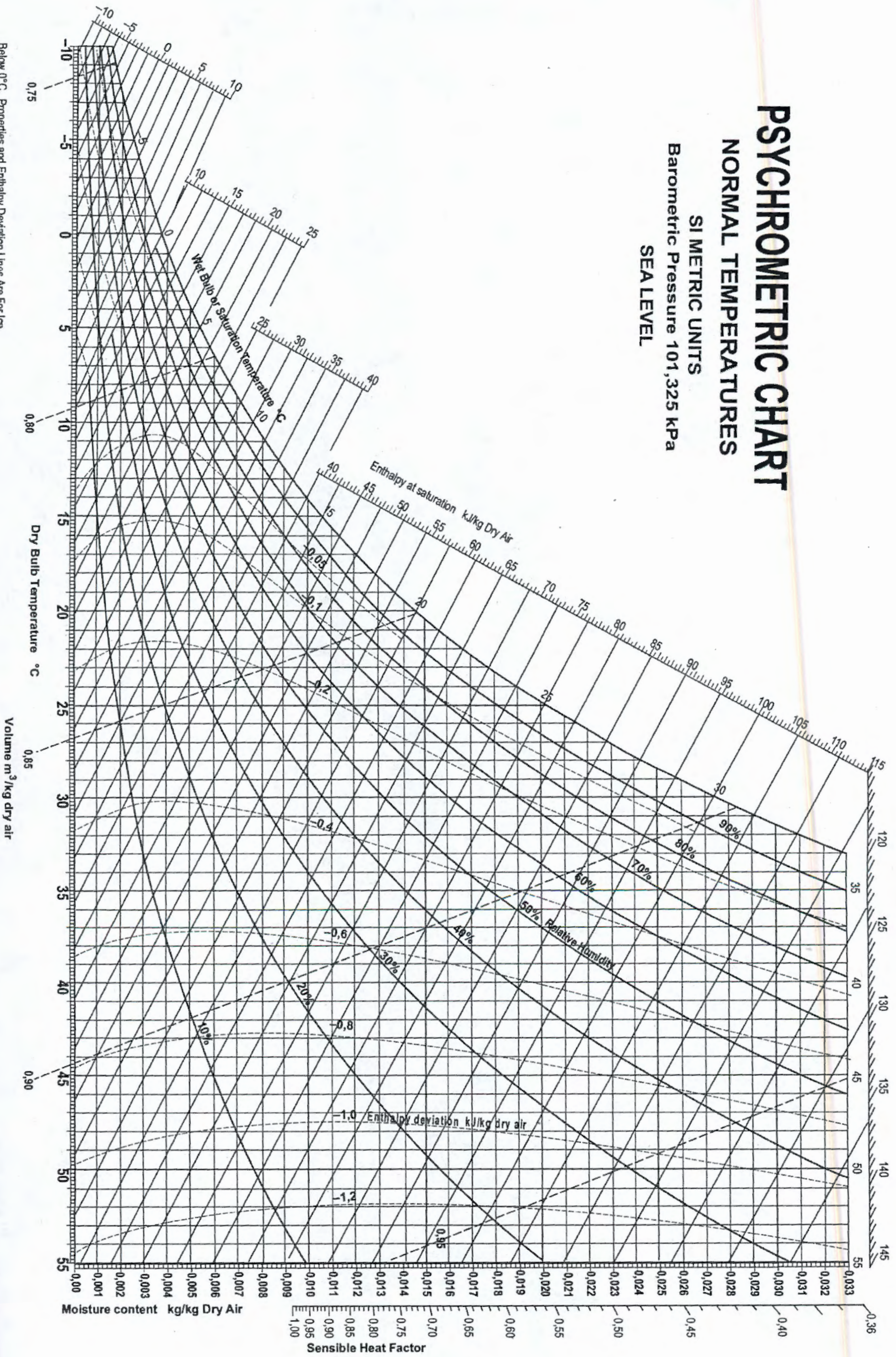
# PSYCHROMETRIC CHART

## NORMAL TEMPERATURES

SI METRIC UNITS

Barometric Pressure 101,325 kPa

SEA LEVEL



**Space for Rough Work**

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**Space for Rough Work**

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**Space for Rough Work**

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**Space for Rough Work**

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