



**MADE EASY**

Leading Institute for ESE, GATE & PSUs

## ESE 2025 : Mains Test Series

UPSC ENGINEERING SERVICES EXAMINATION

### Mechanical Engineering

#### Test-9 : Full Syllabus Test (Paper-I)

Name : .....

Roll No : .....

#### Test Centres

Delhi ☒ Bhopal ☐ Jaipur ☐  
Pune ☐ Kolkata ☐ Hyderabad ☐

#### Student's Signature

#### Instructions for Candidates

1. Do furnish the appropriate details in the answer sheet (viz. Name & Roll No).
2. There are Eight questions divided in TWO sections.
3. Candidate has to attempt FIVE questions in all in English only.
4. Question no. 1 and 5 are compulsory and out of the remaining THREE are to be attempted choosing at least ONE question from each section.
5. Use only black/blue pen.
6. The space limit for every part of the question is specified in this Question Cum Answer Booklet. Candidate should write the answer in the space provided.
7. Any page or portion of the page left blank in the Question Cum Answer Booklet must be clearly struck off.
8. There are few rough work sheets at the end of this booklet. Strike off these pages after completion of the examination.

#### FOR OFFICE USE

Question No.	Marks Obtained
Section-A	
Q.1	42+3=45
Q.2	—
Q.3	44
Q.4	—
Section-B	
Q.5	34+12=46
Q.6	36
Q.7	13
Q.8	—
<b>Total Marks Obtained</b>	<b>184</b>

Signature of Evaluator

Cross Checked by

*[Signature]*

*Keep up his constant effort*

## IMPORTANT INSTRUCTIONS

**CANDIDATES SHOULD READ THE UNDERMENTIONED INSTRUCTIONS CAREFULLY. VIOLATION OF ANY OF THE INSTRUCTIONS MAY LEAD TO PENALTY.**

### DONT'S

1. Do not write your name or registration number anywhere inside this Question-cum-Answer Booklet (QCAB).
2. Do not write anything other than the actual answers to the questions anywhere inside your QCAB.
3. Do not tear off any leaves from your QCAB, if you find any page missing do not fail to notify the supervisor/invigilator.
4. Do not leave behind your QCAB on your table unattended, it should be handed over to the invigilator after conclusion of the exam.

### DO'S

1. Read the Instructions on the cover page and strictly follow them.
2. Write your registration number and other particulars, in the space provided on the cover of QCAB.
3. Write legibly and neatly.
4. For rough notes or calculation, the last two blank pages of this booklet should be used. The rough notes should be crossed through afterwards.
5. If you wish to cancel any work, draw your pen through it or write "Cancelled" across it, otherwise it may be evaluated.
6. Handover your QCAB personally to the invigilator before leaving the examination hall.

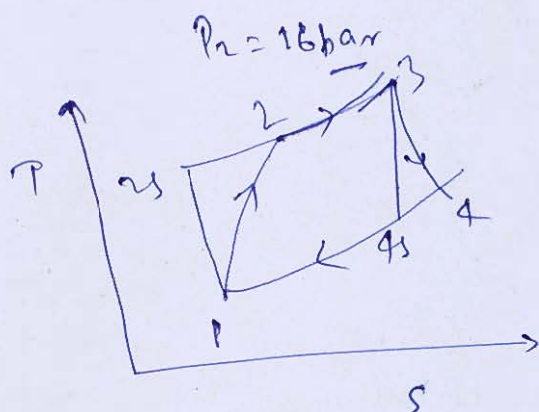


## Section : A

- Q.1 (a) A simple gas turbine admits air at atmospheric pressure (1.013 bar) and 15°C and compresses air in the compressor up to 16 bar. Then the air enters the combustion chamber and is heated to a maximum temperature of 1350°C, further it enters the turbine and expands to atmospheric pressure. The isentropic efficiency of compressor and turbine is 0.87, combustion efficiency 0.98, drop of pressure through the combustion chamber is 0.3 bar. Specific heat at constant pressure for both air and gases is 1.005 kJ/kg-K. Ratio of specific heats 1.4. Determine the flow of air for a net power of 200 MW developed.

[12 marks]

Solution —  $P_1 = 1.013 \text{ bar}$   
 $T_1 = 15^\circ\text{C} = 288 \text{ K}$



$\eta_{\text{combustion}} = 0.98$   
 $T_3 = 1350^\circ\text{C} = 1623 \text{ K}$   
 $P_3 = 15.7 \text{ bar}$

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}}$$

$$= \left(\frac{16}{1.013}\right)^{0.2857}$$

$$\Rightarrow T_2 = 633.5 \text{ K}$$

$$\eta_c = \frac{T_2 - T_1}{T_2 - T_1} \Rightarrow T_2 = \frac{633.5 - 288}{0.87} + 288$$

$$T_2 = 685.22 \text{ K}$$

$$\frac{T_3}{T_4} = \left(\frac{P_3}{P_4}\right)^{\frac{\gamma-1}{\gamma}} \Rightarrow T_4 = 741.74 \text{ K}$$

$$\eta_T = \frac{T_3 - T_4}{T_3 - T_4} \Rightarrow T_4 = 856.3 \text{ K}$$

$$W_T = 1.005 \times (T_3 - T_4) = 1.005 \times (1623 - 856.3)$$

$$= 770.53 \text{ kJ/kg}$$

$$W_C = 1.005 \times (T_2 - T_1) = 1.005 \times (685.22 - 288)$$

$$= 399.21 \text{ kJ/kg}$$

$$W_{\text{net}} = W_T - W_C = 371.32 \text{ kJ/kg}$$

$$m_{\text{air}} = \frac{200 \times 10^3}{371.32} = 538.61 \text{ kg/sec}$$

- Q.1 (b) A cylindrical buoy, diameter 1.5 m and 1.1 m high weighing 4500 N is floating in sea water with its axis vertical. Find the maximum permissible height above the top of the buoy, of the centre of gravity of a 500 N load which is placed centrally on top of the buoy. Take specific gravity of sea water as 1.025.

[12 marks]

$$D = 1.5 \text{ m}, \quad H = 1.1 \text{ m}$$

$$\text{Weight} = 4500 \text{ N}$$



$$F_B = \rho V g$$

$$4500 = 1025 \times V \times 9.81$$

$$V = \frac{4500}{1025 \times 9.81} = 0.4425 \text{ m}^3$$

$$\frac{\pi}{4} \times D^2 \times h = 0.4425$$

$$\Rightarrow 0.205 \times 1.5^2 \times h = 0.4425$$

$$\Rightarrow h = 0.2533 \text{ m}$$



when load of 500 N

$$5000 = 1024 \times 0.215 \times 1.5^2 \times h \times 9.8$$

$$h = 0.2815 \text{ m}$$

$$I_2 = \frac{\pi d^4}{64} = \frac{3.14}{64} \times 1.5^4$$

$$= 0.24832 \text{ m}^4$$

Volume displaced

$$= 0.215 \times 1.5^2 \times 0.2815$$

$$= 0.4971 \text{ m}^3$$

$$I/V = \frac{0.24832}{0.4971} = 0.5 \text{ m}$$

12

C.G. of 4500 N weight from bottom =  $\frac{1.1}{2}$

$$= 0.55 \text{ m}$$

let C.G. of 500 N from bottom =  $y$

$$\text{resultant C.G.} = \frac{0.55 \times 4500 + 500y}{5000}$$

$$= 0.495 + 0.1y$$

Centre of buoyancy from bottom =  $h/2$

$$= 0.2815$$

$$= 0.1407 \text{ m}$$

distance b/w centre of buoyancy and  
centre of gravity

$$0.3543 + 0.1y = 0.5$$

2)

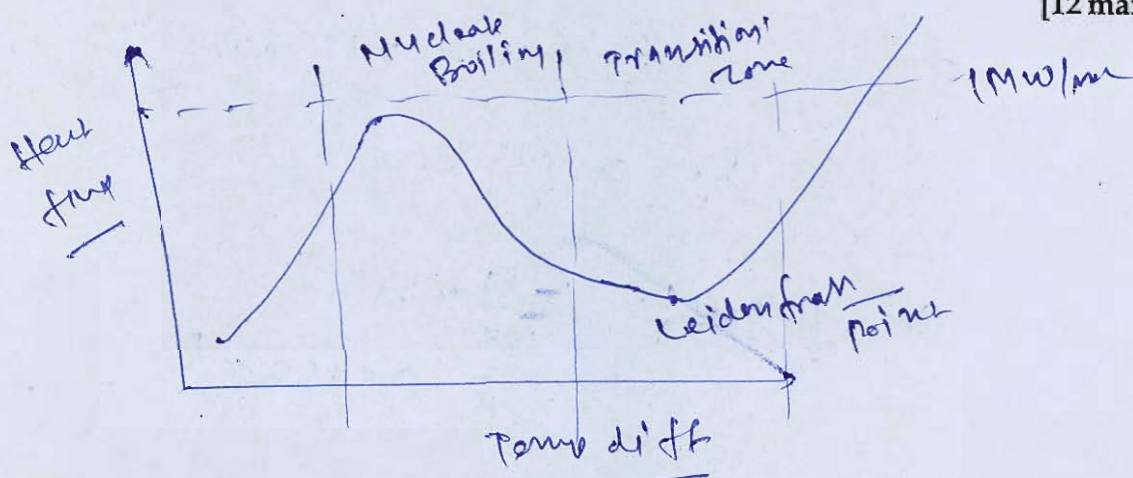
$$y = 1.452 \text{ m}$$

Hence 500 N weight = 0.352 m from buoyancy

$$\text{B.U.} = 0.495 + 0.1y = 0.1407$$

$$= 0.3543 + 0.1y$$

- Q.1 (c) Draw the boiling curve and identify the different boiling regimes. Also, explain the characteristics of each regime. [12 marks]



~~Boiling~~ Boiling may be film boiling or ~~a~~ in which due to evaporation of water, water vapour film is formed near boundary which prevents the heat transfer. When  $\Delta T$  increases upto certain level Heat flux decreases due to less heat convection transfer rate but after a point when  $\Delta T$  value is high radiation prevails and again Heat flux increases.

6



- Q.1 (d) An inward flow turbine (reaction type with radial discharge) with an overall efficiency of 85% is required to develop 160 kW. The head is 8 m; peripheral velocity of the wheel is  $0.96\sqrt{2gH}$ ; the radial velocity of the flow is  $0.36\sqrt{2gH}$ . The wheel is to make 180 rpm, and the hydraulic losses in the turbine are 25% of the available energy. Determine:
- the angle of the guide blade at inlet.
  - the wheel vane angle blade at inlet.
  - the diameter of the wheel.
  - the width of the wheel at inlet.

[12 marks]

$$\eta_o = 85\% \quad , \quad P = 160 \text{ kW} \quad , \quad H = 8 \text{ m}$$

$$u = 0.96 \sqrt{2gH} \quad , \quad N = 180 \text{ rpm}$$

$$= 0.96 \times \sqrt{19.6 \times 8} = 12.03 \text{ m/sec}$$

$$v_f = 0.36 \sqrt{2gH} = 4.51 \text{ m/sec}$$

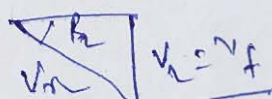
$$\text{Power} = \eta_o \rho g H Q$$

$$160 = 0.85 \times 1 \times 8 \times 9.81 \times Q$$

$$\Rightarrow Q = 2.4 \text{ m}^3/\text{sec}$$

$$u = \frac{2.94}{60} \Rightarrow 12.03 = \frac{3.14 \times D \times 10^3}{60}$$

$$D = 1.277 \text{ m} \quad (\text{Ans})$$



$$0.75 = \frac{v_w \times 4}{gH}$$

$$0.75 = \frac{v_w \times 12.03}{9.81 \times 8}$$

$$\Rightarrow v_w = 4.893 \text{ m/s}$$

$$\tan \alpha_1 = \frac{v_f}{v_w} = \frac{4.51}{4.893}$$

$$\alpha_1 = 42.65^\circ \quad (\text{Ans})$$

$$\tan(\theta - \beta_1) = \frac{v_f}{v_w - v_w} = \frac{4.51}{12.03 - 4.893}$$

$$\Rightarrow \beta_1 = 142.21^\circ \quad (\text{Ans})$$

$$Q = \pi D_1 \beta_1 \times v_f$$

$$2.4 = 3.14 \times 1.277 \times \beta_1 \times 4.51$$

$$\Rightarrow \beta_1 = 0.1327 \text{ m} \quad (\text{Ans})$$

12



- 2.1 (e) A gas of mass 1.5 kg undergoes a quasi-static expansion which follows a relationship  $p = a + bV$ , where  $a$  and  $b$  are constants. The initial and final pressures are 1000 kPa and 200 kPa respectively and the corresponding volumes are  $0.20 \text{ m}^3$  and  $1.20 \text{ m}^3$ . The specific internal energy of the gas is given by the relation.

$$u = 1.5pv - 85 \text{ kJ/kg}$$

Where  $p$  is in kPa and  $v$  is in  $\text{m}^3/\text{kg}$ . Calculate the net heat transfer and the maximum internal energy of the gas attained during expansion.

[Take ratio of specific heat  $\gamma = 1.20$ ]

[12 marks]

$$P_1 = 1000 \text{ kPa}, P_2 = 200 \text{ kPa}$$

$$V_1 = 0.2 \text{ m}^3, V_2 = 1.2 \text{ m}^3$$

$$u_1 = 1.5 \times p_1 v_1 - 85 = 1.5 \times 1000 \times \frac{0.2}{1.5} - 85$$

$$= 19.99 \text{ kJ/kg}$$

$$u_2 = 1.5 \times 200 \times \frac{1.2}{1.5} - 85 = 155 \text{ kJ/kg}$$

$$\Delta u = u_2 - u_1 = 155 - 19.99 = 135.01 \text{ kJ/kg}$$

$$Q = \Delta u + W$$

$$dQ = du + p dv$$

$$Q = \Delta u + \int p dv$$

$$= 1.5 \times 40 \int_{0.2}^{1.2} (1160 - 800v) dv$$

$$= 60 + (1160v - 400v^2) \Big|_{0.2}^{1.2}$$

$$= 60 + 1160 \times 1 - 400 \times (1.2^2 - 0.2^2)$$

$$= 1200 - 560$$

$$= 640 \text{ kJ}$$

$$(Ans)$$

$$p = a + bv$$

$$1000 = a + b \times 0.2$$

$$200 = a + 1.2b$$

$$b = -800$$

$$a = 1160$$

$$p = 1160 - 800v$$

$$y = 1.5PV - 8V$$

$$= \frac{1.5 \times P \times V}{1.5} - 8V$$

$$= PV - 8V$$

$$= (1160 - 800V) V - 8V$$

$$y = 1160V - 800V^2 - 8V$$

For maximum  $y$

$$\frac{dy}{dV} = 0$$

$$1160 - 1600V = 0$$

$$2) V = 0.725 \text{ m}^3$$

$$P = 1160 - 800 \times 0.725$$

$$= 580 \text{ kPa}$$

$$y_{\max} = PV - 8V$$

$$= 580 \times 0.725 - 8V$$

$$= 335.5 \text{ kJ/kg (Ans)}$$



- Q.2 (a) A total of 15 litres per second of oil is pumped through two pipes in parallel, one 10 cm in diameter and the 12 cm in diameter, both pipes 1000 metres long. The specific gravity of the oil is 0.95 and the kinematic viscosity  $9 \text{ cm}^2$  per second. Calculate the flow rate through each time and the horse-power of the pump.

[20 marks]





- 2 (b) Explain the construction and working of turbojet engine with the help of neat sketch and derive the expression for its thermal efficiency.

[20 marks]





- 2 (c) The nose section of a missile is formed of a 6 mm thick stainless plate and is held initially at uniform temperature of  $88^{\circ}\text{C}$ . The missile enters the denser layers of the atmosphere at very high velocity. The effective temperature of air surrounding the nose region attains the value  $2200^{\circ}\text{C}$  and the surface convective coefficient is estimated at  $3400 \text{ W/m}^2\text{-K}$ . Make calculations for the maximum permissible time in these surroundings if the maximum metal temperature is not to exceed  $1095^{\circ}\text{C}$ . Also work out the inside surface temperature under these conditions.

The properties for steel are:  $\rho = 7800 \text{ kg/m}^3$ ,  $k = 51 \text{ W/m-}^{\circ}\text{C}$ ,  $C_p = 465 \text{ J/kg-K}$ .

[Take,  $x/L_c = 1$ , outside surface from nose section]

[Use Heisler chart attached at the end]

[20 marks]





- 2.3 (a) Explain the basic function of refrigerants in a refrigeration cycle and how they are classified? Also discuss the desirable properties of refrigerants and the basic difference between primary and secondary refrigerants.

[20 marks]

→ Refrigerant is used to extract heat from the refrigerated place (the place where desired temperature, humidity and air motion is required) compress in the compressor and then reject that heat to atmosphere then expand in the expander again extract heat in evaporator and this process continues.

refrigerant are classified on the basis of many aspects -

saturated refrigerant of  $\text{C}_n\text{H}_m\text{F}_p\text{Cl}_2$

ex -  $\text{R}_{12}$ ,  $\text{R}_{22}$ ,  $\text{R}_{134a}$  etc.

electroflux refrigerant - there no pumps used.

primary refrigerant is the refrigerant which completes vapour compression cycle.

secondary refrigerant absorbs heat from the refrigerated space and then rejects that heat to the primary refrigerant in the evaporator for ex - in Air Air conditioning

Air act as ~~prim~~ secondary refrigerant and refrigerant inside A.C act as secondary refrigerant.

Desirable property of refrigerant -

1) Low ~~fusion temperature~~

2) High ~~degree of~~ enthalpy of vapourisation.

- 3) High critical temperature.
- 4) low freezing point.
- 5) specific ~~enthalpy~~ heat low for liquid phase and high for vapour phase.
- 6) refrigerant should be Non Toxic.
- 7) refrigerant should be ~~too~~ Non inflammable.
- 8) if leak occurs then refrigerant should be easily detectable.
- 9) ~~correct~~ specific volume of refrigerant should be low otherwise large size compressor would be required.



Q.3 (b) The velocity components in a two-dimensional flow field for an incompressible fluid are expressed as  $u = \frac{y^3}{3} + 2x - x^2y$ ;  $v = xy^2 - 2y - \frac{x^3}{3}$

- Show that these functions represent a possible case of an irrotational flow.
- Obtain an expression for stream function  $\psi$ .
- Obtain an expression for velocity potential  $\phi$ .

[20 marks]

$$u = \frac{y^3}{3} + 2x - x^2y, \quad v = xy^2 - 2y - \frac{x^3}{3}$$

$$\omega_z = \frac{1}{2} \left[ \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right]$$

$$= \frac{1}{2} \left[ \frac{\partial}{\partial x} (xy^2 - 2y - \frac{x^3}{3}) - \frac{\partial}{\partial y} (\frac{y^3}{3} + 2x - x^2y) \right]$$

$$= \frac{1}{2} \left[ y^2 - \frac{\partial y^2}{\partial x} - \frac{\partial (xy^2)}{\partial y} + 2 \right]$$

$$\omega_z = 0$$

Hence irrotational flow

$$u = -\frac{d\phi}{dy}$$

$$-\frac{d\phi}{dy} = \frac{y^3}{3} + 2x - x^2y$$

$$\frac{d\phi}{dy} = -\frac{y^3}{3} - 2x + x^2y$$

$$\phi = -\frac{y^4}{12} - 2xy + \frac{x^2y^2}{2} + \text{finite c}$$

$$\text{or } v = \frac{d\phi}{dx}$$

$$\Rightarrow \frac{d\phi}{dx} = xy^2 - 2y - \frac{x^3}{3}$$

$$\psi = \frac{uxy^2}{2} - uxy - \frac{u^2}{12} + f(y) + c$$

combining both

$$\psi = -\frac{(u^2 + y^4)}{12} + \frac{uxy^2}{2} - uxy + c$$

for velocity potential

$$u = -\frac{d\phi}{dx}$$

$$-\frac{d\phi}{dx} = y^3/3 + ux - uxy$$

$$\frac{d\phi}{dx} = -y^3/3 - ux + uxy$$

$$\phi = -\frac{uy^3}{3} - u^2x + \frac{u^3}{3}y + f(y) + c$$

$$v = -\frac{d\phi}{dy}$$

$$\frac{d\phi}{dy} = -ux^2 + uy + u^3/3$$

$$\phi = -\frac{ux^3}{3} + y^2 + \frac{u^3}{3}y + f(y) + c$$

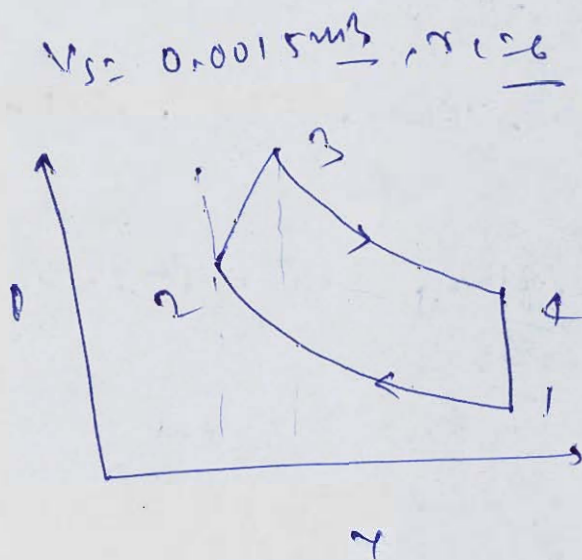
$$\therefore \phi = -\frac{ux^3}{3} - u^2x + y^2 + \frac{u^3}{3}y + c$$

20

(Ans)

- Q.3 (c) A gasoline engine has a stroke volume of  $0.0015 \text{ m}^3$  and a compression ratio of 6. At the end of compression stroke, the pressure is 8 bar and temperature  $350^\circ\text{C}$ . Ignition is set so that the pressure rises along a straight line during combustion and attains its highest value of 25 bar after the piston has travelled  $\frac{1}{30}$  of the stroke. The charge consists of a gasoline-air mixture in proportion by mass 1 to 16. Take  $R = 287 \text{ J/kgK}$ , Calorific value of fuel as  $42 \text{ MJ/kg}$  and  $C_p = 1 \text{ kJ/kgK}$ . Calculate the heat lost per kg of charge during combustion.

[20 marks]



$$r_c = \frac{V_1}{V_2}$$

$$2 V_2 = V_c$$

$$r_c = \frac{V_c + V_s}{V_c}$$

$$2 + \frac{V_s}{V_c}$$

$$2 + \frac{V_s}{V_c} = 6 \Rightarrow \frac{V_s}{V_c} = 4$$



$$\therefore V_c = \frac{V_s}{5} = \frac{15 \times 10^{-4}}{5} = 3 \times 10^{-4} \text{ m}^3$$

$$\begin{aligned} V_3 &= V_c + V_{30} \times V_s \\ &= V_c + \frac{8}{706} V_c = \frac{716}{706} V_c = 3.5 \times 10^{-4} \text{ m}^3 \end{aligned}$$

$$T_2 = 350^\circ \text{C} = 623 \text{ K}$$

$$P_2 = 8 \text{ bar}$$

$$A/P = \frac{16}{1}, \quad P_3 = 25 \text{ bar}$$

$$m = \frac{P_1 V_1}{R T_1} \Rightarrow \frac{P_2 V_2}{R T_2} = \frac{P_3 V_3}{R T_3}$$

$$\Rightarrow \frac{8 \times 3 \times 10^{-4}}{623} = \frac{25 \times 3.5 \times 10^{-4}}{T_3}$$

$$\Rightarrow T_3 = 2271.35 \text{ K}$$

$$W_{2-3} = \frac{1}{2} \times (P_2 + P_3) \times (V_3 - V_2)$$

$$\begin{aligned} &= \frac{1}{2} \times (2500 + 800) \times (3.5 - 3) \times 10^{-4} \\ &= 0.085 \text{ kJ/cycle} \end{aligned}$$

$$\cancel{W_{2-3}} \quad m = \frac{P_1 V_1}{R T_1} = \frac{800 \times 3 \times 10^{-4}}{0.287 \times 623} = 1.392 \times 10^{-3} \text{ kg/cycle}$$

$$\begin{aligned} W_{2-3} &= 1.392 \times 10^{-3} \times 0.212 \times (2271.35 - 623) \\ &= 1.556 \text{ kJ/cycle} \end{aligned}$$

$$DQ = Dv + \phi w_2 - 3$$

$$= 1.586 + 0.08825 = 1.6685 \text{ kg/kg}$$

for 1 kg

$$DQ = \frac{1.6685}{1.3 \times 10^3} = 21243.38 \text{ kJ/kg}$$

$$\text{Heat addition} = 1/16 \times 42000 = 2625 \text{ kJ}$$

$$\begin{aligned} \text{Heat loss} &= 2625 - 1243.12 \\ &= 1381.56 \text{ kJ/kg of air} \end{aligned}$$

Q.4 (a) In a Francis turbine, prove that hydraulic efficiency  $\eta_h$  of the turbine can be expressed as

$$\eta_h = \frac{2}{2 + \frac{k_1 + k_2 + k_3 + k_4}{(\cot \alpha - \cot \theta) \{ \cot \alpha (1 + n^2) - n((\cot \phi + n \cot \theta)) \}}}$$

where  $k_1$ ,  $k_2$ ,  $k_3$  and  $k_4$  represent the fraction of the losses in the guide vanes, runner vanes, draft tube and at exit respectively expressed in terms of the velocity of flow head;  $\alpha$ ,  $\theta$  and  $\phi$  are the guide vane angle, the runner vane angle at inlet and the runner vane angle at outlet respectively and  $n$  is the ratio of the inner to outer diameter of the runner. Assume the velocity of flow to remain constant in the runner.

[20 marks]







Q.4 (b) Castor oil at 25°C flows at a velocity of 0.1 m/s past a flat plate in a certain process. If the plate is 4.5 m long and is maintained at a uniform temperature of 95 °C. Calculate the following using exact solution :

- (i) The hydrodynamic and thermal boundary layer thickness on one side of the plate.
- (ii) The total drag force per unit width on one side of the plate.
- (iii) The local heat transfer coefficient at the trailing edge, and the heat transfer rate.

[Take  $\nu = 0.65 \times 10^{-4} \text{ m}^2/\text{s}$ ,  $\alpha = 7.2 \times 10^{-8} \text{ m}^2/\text{s}$ ,  $k = 0.213 \text{ W/m}^\circ\text{C}$ ,  $\rho = 956.8 \text{ kg/m}^3$ ]

[20 marks]





- Q.4 (c) A horizontal cylinder is separated into two compartments by an adiabatic frictionless piston. One side contains  $0.2 \text{ m}^3$  of nitrogen and the other side contains  $0.1 \text{ kg}$  of helium, both initially at  $20^\circ\text{C}$  and  $95 \text{ kPa}$ . The curved surface of the cylinder and the helium end are insulated. Now heat is added to the nitrogen side from a reservoir at  $500^\circ\text{C}$  until the pressure of the helium rises to  $120 \text{ kPa}$ . Determine:
- (a) the final temperature of the helium,
  - (b) the final volume of the nitrogen,
  - (c) the heat transferred to the nitrogen, and
  - (d) the entropy generation during this process.

The properties of nitrogen at room temperature are:  $R = 0.2968 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K}$ ,  $c_p = 1.039 \text{ kJ/kg} \cdot \text{K}$ ,  $c_v = 0.743 \text{ kJ/kg} \cdot \text{K}$ ,  $k = 1.4$ . The properties for helium are  $R = 2.0769 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K}$ ,  $c_p = 5.1926 \text{ kJ/kg} \cdot \text{K}$ ,  $c_v = 3.1156 \text{ kJ/kg} \cdot \text{K}$ ,  $k = 1.667$

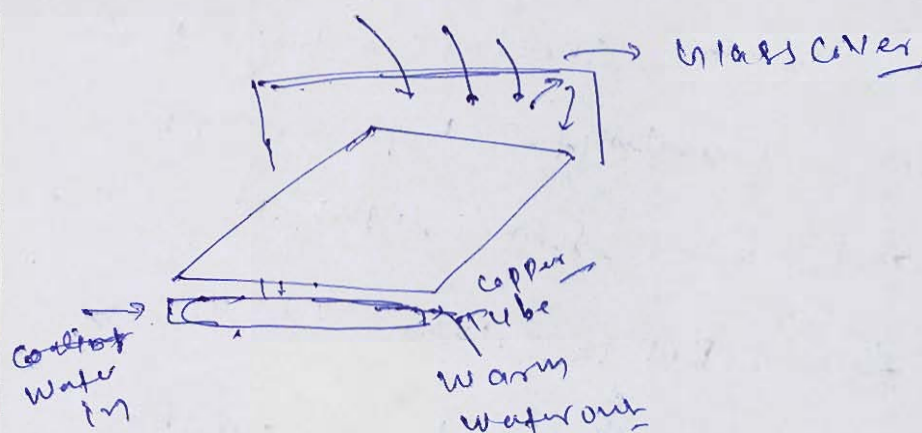
[20 marks]



Section : B

Q.5 (a) Explain the working of liquid flat plate collector with suitable diagrams.

[12 marks]



Flat plate collector is used to collect incident solar radiation. It is flat in shape & it may be tilted to a particular direction or ~~fix~~ maybe in horizontal place. It absorbs incident solar radiation then by using that heat water heating can be done and used for commercial or household purpose. generally no tracking mechanism is used for flat plate collector. It is one fixed does not trace the solar radiation direction. The concentration ratio of flat ~~plate~~ plate collector is one. glass glazing



is used <sup>above</sup> ~~on~~ the upper surface of F.P.C with special coating which absorbs low wavelength high energetic light and when some light is reflected from F.P.C then it again reflects the high wavelength ~~radiation~~ rays back to plate in this way heat gain increases.

Efficiency of F.P.C is denoted by how much useful energy ~~are~~ generated divided by the irradiation.

F.P.C not able to create much temperature of water hence generally used for household purposes to heat water in summer.

7

- Q.5 (b) At a point in a turbulent flow field the instantaneous values of  $u$  and  $v$  velocity components measured at an interval of 0.05 seconds are listed below.

$u$ (mm/s)	+105	+110	+84	+89	+102	+94	+111	+101	+87	+95	+89
$v$ (mm/s)	-3	-16	+11	+25	-6	-20	-20	+4	+21	-2	+6

Determine  $\bar{u}$ ,  $\bar{v}$ ,  $\overline{u'v'}$  and local value of Reynolds' shear stress. Take  $\bar{\rho} = 1.23 \text{ kg/m}^3$ .

[12 marks]

$$\bar{u} = \frac{105 + 110 + 84 + 89 + 102 + 94 + 111 + 101 + 87 + 95 + 89}{11} = 92 \text{ mm/s}$$

$$\bar{v} = \frac{-3 - 16 + 11 + 25 - 6 - 20 - 20 + 4 + 21 - 2 + 6}{11} = 0 \text{ m/s}$$

$$\overline{u'v'} = \frac{105 \times (-3) + 110 \times (-16) + 84 \times 11 + 89 \times 25 + 102 \times (-6) + 94 \times (-20) + 111 \times (-20) + 101 \times 4 + 87 \times 21 + 95 \times (-2) + 89 \times 6}{11}$$

$$= -96.63$$

$$\text{Shear stress} = \bar{\rho} \times \overline{u'v'} = 1.23 \times 96.63 \times 10^{-6} = 118.36 \times 10^{-6} \text{ N/mm}^2$$

12



- Q.5 (c) Derive the relation for the percentage variation in air standard efficiency of Otto cycle with percentage variation of  $c_v$ . Also determine percentage change in efficiency of Otto cycle if compression ratio is 8, and specific heat at constant volume increases by 2%.

[12 marks]

$$\eta = 1 - \frac{1}{(r)^{\gamma-1}}$$

$$\gamma = \frac{C_p}{C_v}$$

$$C_p = C_v + R$$

$$\gamma = \frac{C_v + R}{C_v} = 1 + \frac{R}{C_v}$$

$$\eta = 1 - \frac{1}{(r)^{R/C_v}}$$

$$\gamma - 1 = \frac{R}{C_v} \Rightarrow 2 \frac{R}{C_v}$$

$$\frac{d\eta}{dC_v} = \frac{R}{C_v^2} \times (r)^{R/C_v} \quad R = 0.287 \text{ kJ/kgK}$$

$$C_{v1} = 0.717 \text{ kJ/kgK}$$

$$\eta_1 = 1 - \frac{1}{(8)^{0.287/0.717}} = 0.5647 = 56.47\%$$

$$C_{v2} = 1.02 C_{v1} = 0.73132 \text{ kJ/kgK}$$

$$\eta_2 = 1 - \frac{1}{(8)^{0.287/0.73132}} = 1 - \frac{1}{0.3924} = 0.5527 = 55.27\%$$

∴ change in efficiency

$$= \frac{\eta_2 - \eta_1}{\eta_1} \times 100$$

$$= \frac{55.27 - 56.47}{56.47} \times 100$$

$$= -0.02139 = -1.239\%$$

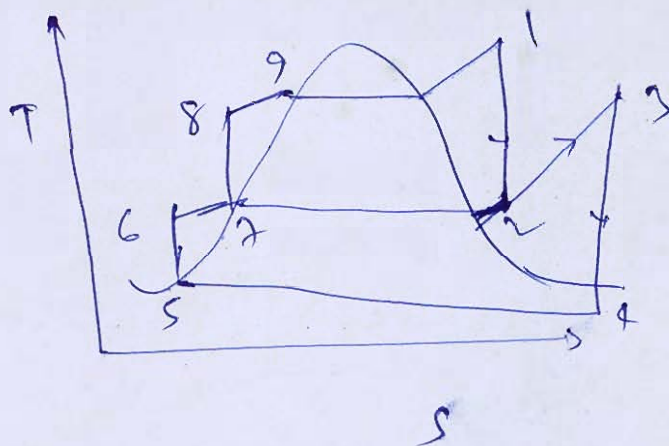


$\therefore$  by increasing  $c_r$  by 2%  
efficiency decreases by 1.239%

12

- Q.5 (d) A passout two stage turbine receives steam at 50 bar and 350°C. At 2.0 bar the high-pressure stage exhausts and 12000 kg of steam per hour are taken at this stage for process heating. The remainder is reheated at 2.0 bar to 250°C and then expanded through the low pressure turbine to condenser pressure of 0.05 bar. The power output from the turbine unit is 3750 kW. Take isentropic efficiency of high pressure and low pressure turbine stage as 0.81. Calculate the boiler capacity.

[12 marks]



Power output  
= 3750 kW

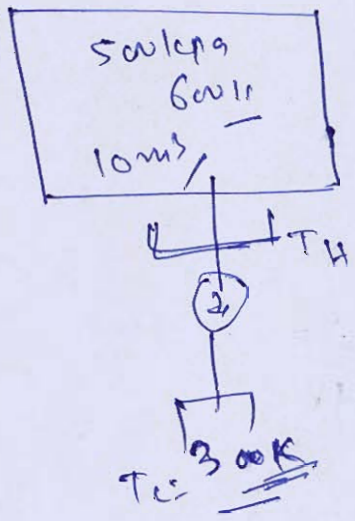
12

As table is not  
provided



Q.5 (e) A  $10\text{ m}^3$  tank of air at  $500\text{ kPa}$ ,  $600\text{ K}$  acts as the high temperature reservoir for a Carnot heat engine that rejects heat at  $300\text{ K}$ . A temperature difference of  $25^\circ\text{C}$  between the air tank and the Carnot cycle high temperature is needed to transfer the heat. The heat engine runs until the air temperature has dropped to  $400\text{ K}$  and then stops. Assume constant specific heat for air and find how much work is given out by the heat engine?

[12 Marks]



$T_H = T_{\text{tank}} - 25^\circ\text{C}$   
Initially,  $T_1 = 600 - 25 = 575\text{ K}$   
 $T_2 = 400 - 25 = 375\text{ K}$

Heat  $Q = m \cdot C_p \cdot \frac{P_1}{P_2}$   
 $= \frac{500 \times 10}{0.287 \times 600} = 29.04\text{ kg}$

$\eta = 1 - \frac{T_C}{T_H}$   
 $= 1 - \frac{375}{575}$   
 $= 0.3478$

Heat by tank ( $Q$ )  
 $= m \cdot C_p \cdot (T_1 - T_2)$   
 $= 29.04 \times 0.287 \times (600 - 400)$   
 $= 810.25\text{ kJ}$

$W = \eta \times Q$   
 $= 0.3478 \times 810.25$   
 $= 281.75\text{ kJ}$



- Q.6 (a) (i) Explain the working principle of thermo electric refrigeration with schematic diagram.
- (ii) A tracking mechanism for the solar heating purpose needs to be installed in Kolkata ( $22^\circ\text{N}$ ,  $88^\circ 22'\text{E}$ ), West-Bengal. Determine the sunshine hour angle on 28th of May and also determine the global radiation in ( $\text{kJ}/\text{m}^2$  day) by using modified angstroms equation.

$$\frac{H_g}{H_o} = a + b \left( \frac{L_a}{L_m} \right); \text{ where } a = 0.28, b = 0.48, \frac{L_a}{L_m} = 0.7944$$

$$I_n = I_{sc} \left\{ 1 + 0.033 \cos \left( \frac{360}{365} \times n \right) \right\}$$

[20 marks]

(11) For 28th May,  $\phi = 22^\circ$

$$n = 31 + 24 + 31 + 30 + 24 = 140$$

$$\delta = 23.45 \sin \left\{ \frac{360}{365} (284 + n) \right\}$$

$$= 21.43^\circ$$

$$H_o = \frac{294}{\pi} \int_0^{\omega_s} I_{sc} \left\{ 1 + 0.033 \cos \left( \frac{360}{365} \times 140 \right) \right\} \left\{ \sin \delta \cdot \sin \phi + \cos \delta \cdot \cos \phi \cdot \cos \omega \right\} d\omega$$

$$\omega_s = \cos^{-1} \left\{ -\tan \phi \cdot \tan \delta \right\}$$

$$= \cos^{-1} \left\{ -\tan 22^\circ \cdot \tan 21.43^\circ \right\}$$

$$\omega_s = 99.12^\circ = 1.729 \text{ radian}$$

$$H_o = 4890 \times 0.9226 \times \frac{24}{\pi} \left\{ \omega_s \sin 21.43^\circ \cdot \sin 22^\circ + \cos 21.43^\circ \cdot \cos 22^\circ \cdot \sin 99.12^\circ \right\}$$

$$= 36351.2 \times (0.2366 + 0.854)$$

$$= 39528.71 \text{ kJ/m}^2 \text{ day}$$

$$\frac{H_g}{H_0} = a + b \left( \frac{V_g}{V_m} \right)$$

$$= 0.24 + 0.48 \times 0.7942$$

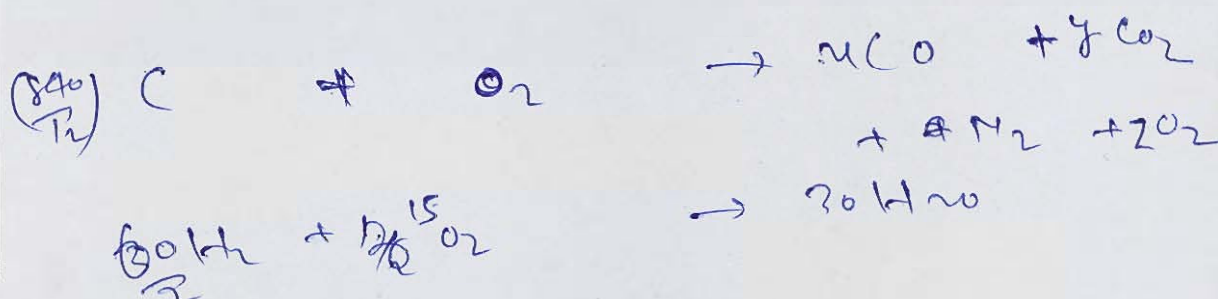
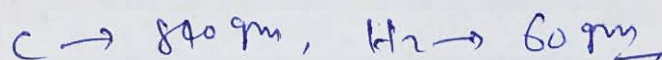
$$= 0.6613$$

$$H_g = \underline{26123.87 \text{ kg/m}^2 \text{ day (Ans)}}$$

Q.6 (b) Percentage volumetric analysis of a sample of dry flue gases of a coal fired boiler gave 10.4%  $\text{CO}_2$ , and 2% of  $\text{CO}$ . Gravimetric percentage analysis of coal was 84% Carbon, 6% Hydrogen and 10% incombustible. Estimate (consider oxygen also in combustion product)

- Weight of dry flue gases per kg of fuel.
- Weight of air supplied per kg of fuel.
- Weight of water vapour formed per kg of fuel.

[20 marks]



$$\begin{aligned} \text{mole of O}_2 \text{ required} &= \frac{x}{2} + y + 15 + 2 \\ 12x + 12y &= 840 \\ x + y &= \frac{840}{12} = 70 \end{aligned}$$



$$\begin{aligned}
 \text{Mole of } N_2 &= \frac{79}{28} \times \text{mole of } O_2 \\
 &= \frac{79}{28} \times (2x/2 + y + 15 + 2) \\
 &= 1.881x + 3.762y + 3.7622 + 56.43
 \end{aligned}$$

Total moles in ~~combustion~~ exhaust

$$\begin{aligned}
 &= x + y + 2 + 1.881x + 3.762y + 3.7622 + 56.43 \\
 &= 70 + 2 + 1.881 \times 70 + 1.88y + 3.7622 + 56.43 \\
 &= 258.1 + 1.88y + 4.7622
 \end{aligned}$$

$$\text{of } CO_2 = \frac{y}{258.1 + 1.88y + 4.7622} = 10.4\%$$

$$\text{of } CO = \frac{x}{258.1 + 1.88y + 4.7622} = 2\%$$

$$y/x = \frac{10.4}{2} = 5.2$$

$$x + y = 70$$

$$6.2x = 70$$

$$\Rightarrow x = 11.29$$

$$y = 58.71$$

$$\frac{58.71}{0.104} = 258.1 + 1.88 \times 58.71 + 4.7622$$

$$\begin{aligned}
 \Rightarrow 4.7622 &= 196.09 \\
 z &= \underline{41.16}
 \end{aligned}$$

$$\begin{aligned} \text{mass of } \text{CO in exhaust gas} &= x \times 28 \\ &= 11.29 \times 28 = 316.12 \text{ gm} \end{aligned}$$

$$\begin{aligned} \text{CO}_2 &= y \times 44 = 58.71 \times 44 \\ &= 2583.24 \text{ gm} \end{aligned}$$

$$\begin{aligned} \text{O}_2 &\rightarrow z \times 32 \\ &= 41.16 \times 32 = 1317.12 \text{ gm} \end{aligned}$$

$$\begin{aligned} \text{mass of N}_2 &= (1.881x + 3.202y + 3.202z + 56.43) \times 28 \\ &= 12694.56 \text{ gm} \quad (A) \end{aligned}$$

$$\begin{aligned} \text{Total mass of exhaust gases} &= 16911.05 \text{ gm} \\ &\quad (Ans) \end{aligned}$$

$$\begin{aligned} \text{mass of air supplied} &= \left( \frac{x}{2} + y + 15 + z \right) \times 32 \times \frac{100}{23} \\ &= 16762.13 \text{ gm} \end{aligned}$$

$$\begin{aligned} &= 16.76213 \text{ kg of fuel} \\ &\quad (Ans) \end{aligned}$$

20

weight of water vapour  
formed

$$\begin{aligned} &= 30 \times 18 \\ &= 540 \text{ gm} \quad (Ans) \end{aligned}$$



Q.6 (c) Air enters an air-conditioning system that use refrigerant R-134a at 30°C and 70% R.H. at a rate of 4 m<sup>3</sup>/min. The refrigerant enters the cooling section at 700 kPa with a quality of 20% and leaves as saturated vapour. The air is cooled at 20°C and 20% RH at a pressure of 1 atm. Determine :

- the rate of dehumidification
- the rate of heat transfer
- the mass flow rate of the refrigerant

Assume the condensate temperature as 20°C. Use the following data for water and refrigerant R-134a.

Water :

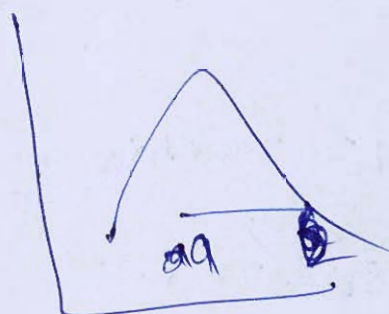
T(°C)	P <sub>sat</sub> (kPa)	Sp. Volume (m <sup>3</sup> /kg)		Sp. Enthalpy (kJ/kg)	
		v <sub>f</sub>	v <sub>g</sub>	h <sub>f</sub>	h <sub>g</sub>
20	2.3392	0.001002	57.762	83.915	2537.4
30	4.2469	0.001004	32.879	125.74	2555.6

R-134a:

T(°C)	P <sub>sat</sub> (kPa)	Sp. Volume (m <sup>3</sup> /kg)		Sp. Enthalpy (kJ/kg)	
		v <sub>f</sub>	v <sub>g</sub>	h <sub>f</sub>	h <sub>g</sub>
26.72	700	0.0008328	0.0292	86.78	175.07

[20 marks]

at 30°C, 70% RH  
 $\phi = 0.7$



$$h_1 = 86.78 + 0.2 \times 175.07$$

$$= 121.81 \text{ kJ/kg}$$

$$h_2 = 261.85 \text{ kJ/kg}$$

mass of air =  $m_2 \frac{P_a}{P_T}$

$$(P_v) = 0.7 \times P_v$$

$$= 0.7 \times 4.2469$$

$$= 2.973 \text{ kPa}$$

$$P_{a2} = P_{atm} - 2.973$$

$$= 100 - 2.973$$

$$= 97.027 \text{ kPa}$$



$$m_a = \frac{92.022 \times 4}{60 \times 0.287 \times 203} = 0.0243 \text{ kg/sec}$$

$$w_1 = \frac{0.622 \times p_v}{p - p_v} = \frac{0.622 \times 2.923}{92.022} = 0.01906 \text{ gm/kg of dry air}$$

$$h_1 = 1.005 \times 30 + 0.01906 \times (2500 + 1.88 \times 30) = 28.8814 \text{ kJ/kg}$$

$$p_{h2} = 0.2 \times 2.339 = 0.42 \text{ kPa}$$

$$w_2 = \frac{0.622 \times 0.42}{100 - 0.42} = 2.924 \times 10^{-3} \text{ gm/kg of dry air}$$

$$h_2 = 1.005 \times 20 + 2.924 \times 10^{-3} \times (2500 + 1.88 \times 20) = 22.52 \text{ kJ/kg}$$

$$m_a \times (h_1 - h_2) = \dot{m}_{\text{ref}} \times (h_b - h_a)$$

$$0.0243 \times (28.88 - 22.52) =$$

$$\dot{m}_{\text{ref}} \times (26.85 - 12.8)$$

$$\Rightarrow \dot{m}_{\text{ref}2} = 0.02221 \text{ kg/sec}$$

$$= 1.635 \text{ kg/min (Ans)}$$

rate of dehumidification

$$= m_a \times (w_1 - w_2)$$

$$= 0.0243 \times (0.01906 - 2.924 \times 10^{-3})$$

$$= 1.199 \times 10^3 \text{ g/s}$$

$$= 1.199 \text{ gm/sec (Ans)}$$

rate of heat transfer

$$= \dot{m}_{\text{air}} \times (h_1 - h_2)$$

$$= 0.0243 \times (75.46 - 22.52)$$

$$= 3.816 \text{ kW}$$

- Q.7 (a) (i) Explain the working principle of a flooded type evaporator used in refrigeration system with the help of neat and labelled diagram.
- (ii) A centrifugal compressor running at 18000 rpm takes in air at  $25^\circ\text{C}$  and compresses it through a pressure ratio of 4.0 with an isentropic efficiency of 80%. Guide vane at inlet, guides the air, at an angle of pre-whirl of  $20^\circ$  to the axial direction. The mean diameter of impeller eye is 225 mm. Absolute air velocity at inlet is 130 m/s and slip factor is 0.9. If at exit the blades are radially inclined, calculate the impeller tip diameter.

[20 marks]

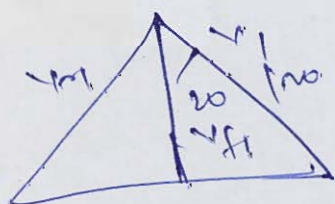
(11)  $N = 18000 \text{ rpm}$  ,  $\phi = 0.9$   
 $T_1 = 25^\circ\text{C} = 298 \text{ K}$   
 $r_p = 4$   
 $\eta_c = 0.8$

$$T_{2s} = 298 \times 4^{0.2857} = 442.81 \text{ K}$$

$$0.8 = \frac{T_{2s} - T_1}{T_2 - T_1} \Rightarrow T_2 = 479.02 \text{ K}$$

$$u_1 = \frac{3.14 \times 0.225 \times 18000}{60}$$

$$= 211.95 \text{ m/s}, V_1 = 130$$



$V_1 \sin 20$

$$100 \text{ kJ} \times (T_2 - T_1) = \dot{m} \dot{W}_2 - \dot{m} \dot{W}_1$$

where

$$\dot{W}_1 = \dot{m} u_1 \sin 20$$

$$= 41.02 \text{ m/s}$$

$$1005 \times (479.02 - 298) =$$

$$1005 \times 0.9 \times u_2^2$$

$$41.02 \times 211.95$$



$$742 = 460.22$$

$$460.22 = \frac{3.14 \times D_2 \times 18000}{60}$$

$$D_2 = 0.488 \text{ m} \quad (\text{Ans})$$

10



- Q.7 (b) Water is pumped rapidly from the ocean into the basin at high tide to give an increased water level of 1.2 m in a tidal power basin. If tidal range is 6 m and the efficiency of pump and generator system is only 50%. Find the energy gain due to use of pumping. [20 marks]



Q.7 (c) In a constant speed CI engine operating on 4-stroke cycle and fitted with a band brake, the following observations were recorded:

Brake wheel diameter = 60 cm;

Band thickness = 5 mm;

Speed = 450 rpm;

Load on band = 210 N;

Spring balance reading = 30 N;

Area of indicator diagram = 4.15 cm<sup>2</sup>;

Length of indicator diagram = 6.25 cm;

Spring constant = 11 bar/cm;

Bore = 10 cm;

Stroke = 15 cm;

Specific fuel consumption = 0.3 kg/kW-hr;

Calorific value of fuel = 41800 kJ/kg

Determine the brake power, indicated power, mechanical efficiency, the indicated thermal efficiency and the brake thermal efficiency.

[20 marks]

$$\text{Actual load} = 210 - 30 = 180 \text{ N}$$

$$r = \frac{60 + 0.5}{2} = 30.25 \text{ cm}$$

$$T = \frac{180 \times 30.25}{100} = 54.45 \text{ Nm}$$

$$B.P = \frac{2\pi r T}{60} = \frac{2 \times 54.45 \times 2\pi}{60} = 2564.6 \text{ W} = 2.564 \text{ kW}$$

$$S.F.C = 0.3 \text{ kg/kW-hr}$$

$$\eta = 0.3 = \frac{3600 \times \text{m.f.}}{B.P}$$

$$2) \text{ ~~6600~~ } 0.3 = \frac{3600 \times \dot{m}_f}{2.564}$$

$$2) \dot{m}_f = 2.137 \times 10^{-4} \text{ kg/sec}$$

$$\begin{aligned} H \cdot A &= \dot{m}_f \times CV_f \\ &= 2.132 \times 10^{-4} \times 41800 \\ &= 8.93 \text{ kW} \end{aligned}$$

$$\begin{aligned} \textcircled{B} \eta_{B-T.E} &= \frac{B.P}{H.A} \\ &= \frac{2.564}{8.93} \\ &= 0.2821 \\ &= 28.21\% \end{aligned}$$

$$\begin{aligned} I.P &= \text{~~11~~ } 11 \times 6.25 \times 4.15 \text{ ~~Bar-m~~} \\ &= 285.31 \times 10^5 \times 10^{-4} \\ &= 2853.13 \text{ W} = 2.8531 \text{ kW} \end{aligned}$$

$$\begin{aligned} \eta_{m.e} &= \frac{B.P}{I.P} = \frac{2564.6}{2853.13} \\ &= 0.8988 \\ &= 89.88\% \end{aligned}$$

$$\begin{aligned} \eta_{C-T.E} &= \frac{I.P}{H.A} = \frac{2.853}{8.93} = 0.3194 \\ &= 31.94\% \end{aligned}$$

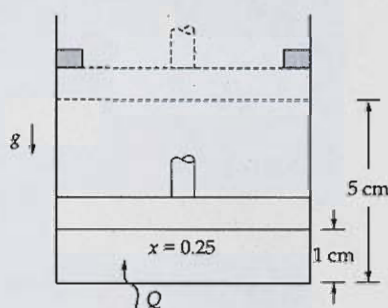
Q.8 (a) Explain thermo-chemical and bio-chemical biomass conversion technologies.

[20 marks]





- Q.8 (b) Two phase water vapour of dryness fraction equal to 0.25 is contained in a cylinder and cylinder arrangement as shown in figure. The mass of the piston is 40 kg and its diameter is 10 cm. The barometric pressure is 1 bar. The position of the piston in the initial and final stage is 1 cm and 5 cm. The water is heated with pressure maintained constant inside the cylinder till it reaches the stops. The addition of heat continues till the pressure inside the cylinder is 3 bar. Estimate the total heat transfer. Also draw p-V diagram.



The following data for steam may be used:

Saturated steam

$p$ bar	Specific volume $\text{m}^3/\text{kg}$		Specific entropy $\text{kJ}/\text{kgK}$		Specific enthalpy $\text{kJ}/\text{kg}$	
	$v_f$	$v_g$	$s_f$	$s_g$	$h_f$	$h_g$
1.5	0.001053	1.1593	1.4336	7.2233	467.11	2693.6

Superheated steam

$T$ $^{\circ}\text{C}$	$v$ $\text{m}^3/\text{kg}$	$h$ $\text{kJ}/\text{kg}$	$s$ $\text{kJ}/\text{kgK}$
$p = 3 \text{ bar } (133.55^{\circ}\text{C})$			
Sat.	0.6058	2725.3	6.9919
200	0.6339	2761.0	7.0778
600	1.3414	3703.2	8.5892
700	1.4957	3927.1	8.8319

[20 marks]







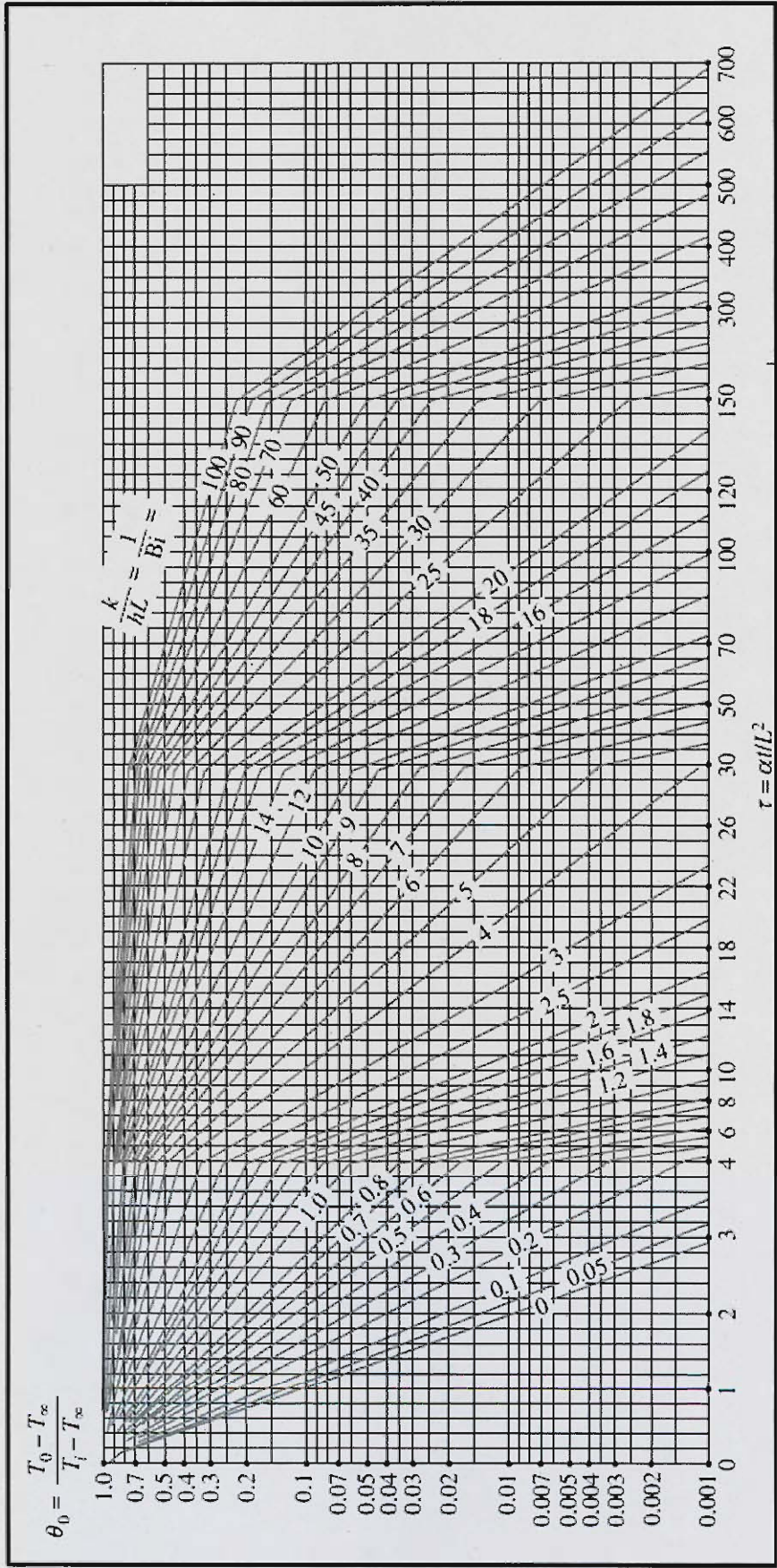
- 8 (c) The draft tube of a Kaplan turbine has inlet diameter 2.6 m and inlet is set at 2.9 m above the tail race. When the turbine develops 1545 kW of power under a net head of 6.5 m, it is found that the vacuum gauge fitted at inlet to draft tube indicates a negative head of 4 m. If the turbine efficiency is 85%, determine the draft tube efficiency. If the turbine output is reduced to half with the same head, speed and draft tube efficiency, what would be the reading of the vacuum gauge?  
Atmospheric pressure is 10.3 m of water and specific weight is  $1000 \text{ kg/m}^3$ .

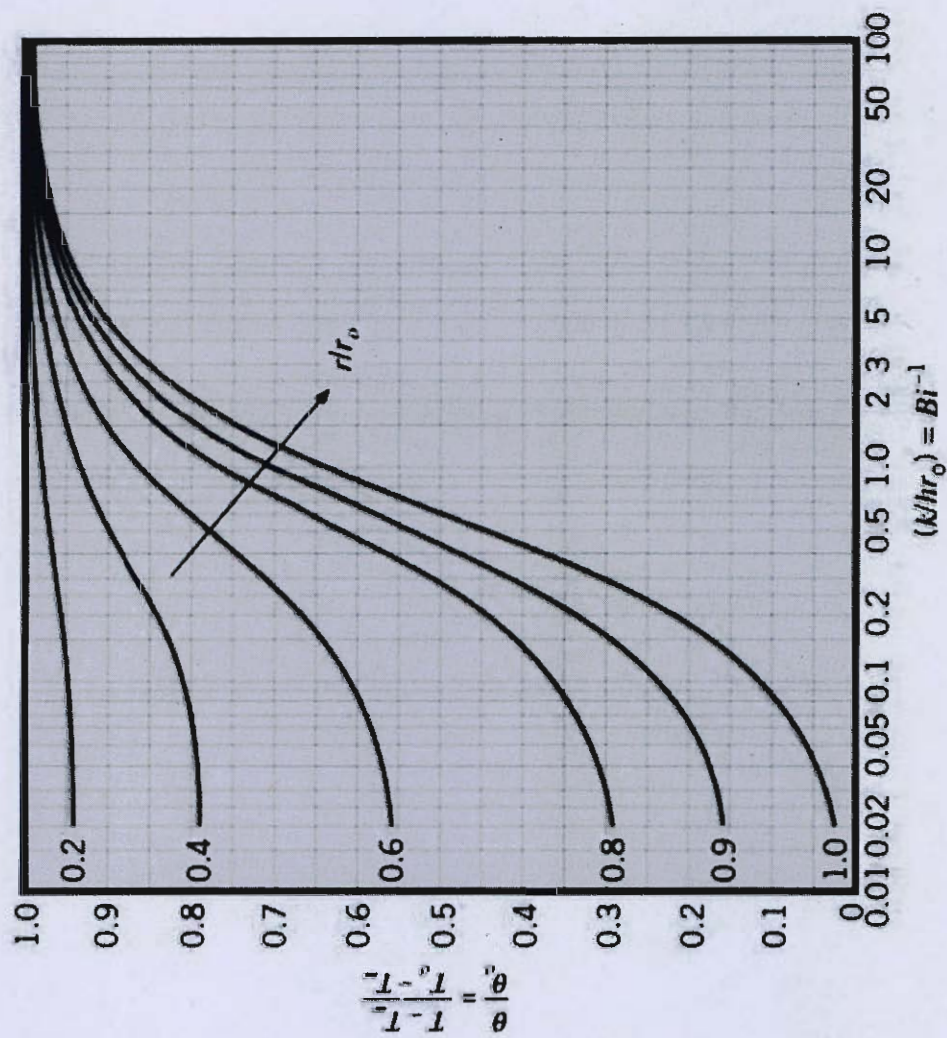
[20 marks]













## Space for Rough Work

---

## Space for Rough Work

---

$\vec{r} = \vec{r}_0 + \vec{v}t$   
 $\vec{v} = \frac{d\vec{r}}{dt}$   
 $\vec{a} = \frac{d\vec{v}}{dt}$

$\vec{r} = \vec{r}_0 + \vec{v}t$   
 $\vec{v} = \frac{d\vec{r}}{dt}$   
 $\vec{a} = \frac{d\vec{v}}{dt}$   
 $\vec{r} = \vec{r}_0 + \vec{v}t$   
 $\vec{v} = \frac{d\vec{r}}{dt}$   
 $\vec{a} = \frac{d\vec{v}}{dt}$   
 $\vec{r} = \vec{r}_0 + \vec{v}t$   
 $\vec{v} = \frac{d\vec{r}}{dt}$   
 $\vec{a} = \frac{d\vec{v}}{dt}$