

# CLASS TEST

S.No. : 04 GH1\_ME\_F\_250919

Fluid Mechanics & Machinery



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# CLASS TEST 2019-2020

## MECHANICAL ENGINEERING

Date of Test : 25/09/2019

### ANSWER KEY > Fluid Mechanics & Machinery

- |        |         |         |         |         |
|--------|---------|---------|---------|---------|
| 1. (b) | 7. (b)  | 13. (c) | 19. (b) | 25. (b) |
| 2. (b) | 8. (c)  | 14. (b) | 20. (a) | 26. (c) |
| 3. (a) | 9. (a)  | 15. (a) | 21. (b) | 27. (d) |
| 4. (b) | 10. (b) | 16. (a) | 22. (a) | 28. (a) |
| 5. (a) | 11. (a) | 17. (c) | 23. (d) | 29. (d) |
| 6. (b) | 12. (b) | 18. (b) | 24. (a) | 30. (b) |

## Detailed Explanations

1. (b)

For soap bubble,  $\Delta P = \frac{8\sigma}{d}$

where,  $\Delta P$  is pressure difference,

$\sigma$  is surface tension,  $\Delta P = \frac{8 \times 0.072}{0.001} = 576 \text{ N/m}^2$

3. (a)

We know, equation of an stream-line is

$$\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{\omega}$$

$\therefore$  The flow is 2-dimensional,

$$\therefore \frac{dx}{u} = \frac{dy}{v}, \frac{dx}{x} = \frac{dy}{-y}$$

On integrating,  $\ln x = \ln\left(\frac{c}{y}\right), x = \frac{c}{y} \Rightarrow xy = c$

As it passing through 1, 1

$$\therefore c = 1$$

$\therefore$  Equation of stream-line is  $xy - 1 = 0$

4. (b)

Let  $V$  is total volume of Iceberg and let  $x$  is the volume of Iceberg inside water.

According to floatation principle,

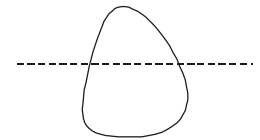
$$\text{Weight of body} = \text{Weight of liquid displaced}$$

$$\therefore 8 \text{ kN} \times V = x \times 10.05 \text{ kN}$$

$$x = 0.796 V$$

$\therefore$  Percentage of total volume of Icerberg above water surface will be

$$= \frac{(V - x)}{V} \times 100 = \frac{(0.2039 V)}{V} \times 100 = 20.39\%$$



5. (a)

$$d = 50 \text{ mm}$$

$$\theta = 30^\circ$$

$$F_x = 1471.5 \text{ N}$$

$$F_x = \rho AV^2 \sin^2 \theta$$

$$A = \frac{\pi}{4} \times 0.05^2 = 0.001963 \text{ m}^2$$

$$1471.5 = 1000 \times 0.001963 \times V^2 \times \sin^2(30^\circ)$$

$$V = 54.7583 \text{ m/s}$$

$$Q = AV = 0.001963 \times 54.7583 = 0.1075 \text{ m}^3/\text{s} = 107.5 \text{ liters/s}$$

6. (b)

Force on piston = Shear force due to oil viscosity

$$18 = \tau \cdot A$$

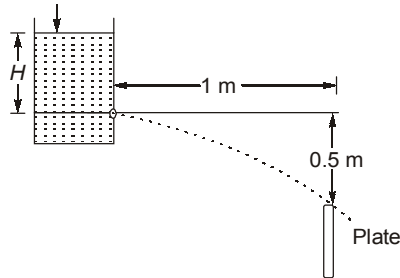
$$18 = \frac{\mu V}{h} \times \pi \times d \times L$$

$$\Rightarrow 18 = \frac{3 \times 0.1 \times V \times \pi \times 0.0795 \times 0.3}{0.025 \times 10^{-2}}$$

$$\Rightarrow V = 0.2001 \text{ m/s}$$

$$\Rightarrow V = 20 \text{ cm/s}$$

7. (b)



For a point on the trajectory.

$$\therefore x = u_1 t \quad \dots(i)$$

$$z = \frac{1}{2} g t^2 \quad \dots(ii)$$

For,  $C_V = 1, u_1 = \sqrt{2gH}$

From Eq. (i) and (ii)

$$\therefore z = \frac{x^2}{4H} \Rightarrow H = \frac{x^2}{4z} \Rightarrow \frac{(1)^2}{4 \times 0.5} = 0.5 \text{ m}$$

8. (c)

During cavitation, the vapour bubbles starts forming where the pressure of the liquid falls below the vapour pressure and sudden collapsing of these vapour bubbles in a region of higher pressure. When they collapse, a very high pressure is created. This causes pitting action on the surfaces over which they collapse. Hence during, cavitation and subsequent, pitting, pre-dominant forces are compressive forces.

9. (a)

Power available at the nozzle is

$$P = \frac{\rho g Q H}{1000} \text{ kW} = \frac{1000 \times 9.81 \times 0.1 \times 700}{1000} = 686.7 \text{ kW}$$

11. (a)

$$a_x = \frac{du}{dt} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \Rightarrow 2t + (t^2 + 3y)0 + (4t + 5x)(3)$$

$$a_y = \frac{dv}{dt} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \Rightarrow 4t + (t^2 + 3y)5 + (4t + 5x)0$$

$$= 4 + 5t^2 + 15y$$

At point (5, 3),

$$a_x = (14 \times 2) + (15 \times 5) = 103$$

$$a_y = 4 + (5 \times 2^2) + (15 \times 3) = 69$$

$$a = \sqrt{103^2 + 69^2} = 123.97 \text{ units}$$

12. (b)

$$Q = A_1 V_1 = A_2 V_2$$

$$\Rightarrow \frac{\pi}{4} \times 0.3 \times V_1 = \frac{\pi}{4} \times 0.15^2 \times V_2$$

$$\Rightarrow V_2 = 4V_1$$

Applying Bernoulli equation at point 1 and 2,

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

But  $Z_1 = Z_2$  for the same horizontal level

$$\frac{P_1 - P_2}{\rho g} + \frac{V_1^2}{2g} = \frac{V_2^2}{2g}$$

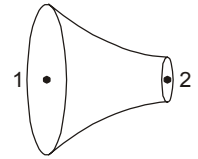
$$\frac{0.05 \times 13.6 \times 1000 \times g}{1000 \times g} = \frac{V_2^2}{2g} - \frac{V_1^2}{2g}$$

$$0.68 = \frac{16V_1^2 - V_1^2}{2g}$$

$$\Rightarrow V_1 = 0.943 \text{ m/s}$$

$$\Rightarrow Q = A_1 V_1 = \pi \times 0.25 \times 0.3^2 \times 0.943 = 0.06666 \text{ m}^3/\text{s}$$

$$\Rightarrow Q = 66.66 \approx 67 \text{ l/s}$$



13. (c)

At stagnation point,  $u = 0, v = 0$ 

$$\Rightarrow x + 2y + 2 = 0, 2x - y = 3.5$$

On solving above equations,

$$x = 1, y = -1.5$$

$$D = \sqrt{(x-0)^2 + (y-0)^2} = 1.8027 \text{ m}$$

$$D = \sqrt{(1-0)^2 + (-1.5-0)^2} = 1.8027 \text{ m}$$

14. (b)

For similar turbines, specific power will be same

$$H_m : H_p = 1 : 4$$

$$P_p = 300 \text{ kW}$$

$$\frac{N_m D_m}{\sqrt{H_m}} = \frac{N_p D_p}{\sqrt{H_p}}$$

$$\frac{N_m D_m}{\sqrt{10}} = \frac{N_p D_p}{\sqrt{40}}$$

$$\frac{1000 \times D_p}{\sqrt{40}} = \frac{N_m D_m}{\sqrt{10}}$$

$$\therefore N_m = \frac{1000 \times 4 \times \sqrt{10}}{\sqrt{40}}$$

$$\Rightarrow N_m = 2000$$

Now, for the same specific speeds

$$\frac{N_m \sqrt{P_m}}{H_m^{5/4}} = \frac{N_p \sqrt{P_p}}{H_p^{5/4}}$$

$$\Rightarrow P_m = 2.34 \text{ kW}$$

15. (a)

For the condition of verge of tipping, the centre of pressure must be at C.

$$\therefore \text{Height of C above B} = \frac{H}{3} = \frac{9.5}{3} = 3.16 \text{ m}$$

[ $\therefore$  for a rectangular plane surface of height H, just completely inside fluid, the centre of pressure is at  $\frac{H}{3}$  from base.]

16. (a)

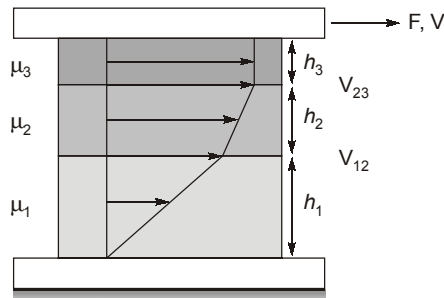
The specific speed for turbines is given by

$$N_s = \frac{N\sqrt{Q}}{H^{5/4}}$$

The specific speed for pumps is given by

$$N_s = \frac{N\sqrt{Q}}{H^{3/4}}$$

17. (c)



Area of each plate =  $1 \text{ m}^2$

$\therefore$  Shear stress on each plate and layer will be,

$$\tau = F/A = \frac{100}{1} = 100 \text{ N/m}^2$$

$\therefore$  Let  $V_{12}$  be the velocity of intermediate layer between fluid 1 and 2 and  $V_{23}$  be the corresponding velocity for layer between 2 and 3.

Then,

$$\tau = \frac{\mu_1 V_{12}}{h_1}$$

$$\Rightarrow 100 = \frac{0.15 \times V_{12}}{0.5 \times 10^{-3}} \Rightarrow V_{12} = 0.333$$

Also,

$$\tau = \mu_2 \times \frac{(V_{23} - V_{12})}{h_2}$$

$$\therefore 100 = \frac{0.5 \times (V_{23} - 0.333)}{0.25 \times 10^{-3}} \Rightarrow V_{23} = 0.383$$

Also, 
$$\tau = \mu_2 \times \frac{(V_{23} - V_{12})}{h_2}$$

$$\therefore 100 = \frac{0.2 \times (V - 0.383)}{0.2 \times 10^{-3}} \Rightarrow V = 0.483 \text{ m/s}$$

18. (b)

$$\text{Speed } (v) = \sqrt{2gH}$$

$$\therefore U \propto H^{1/2}$$

$$\text{Discharge } (Q) = AV$$

$$\therefore Q \propto D^2 \sqrt{H}$$

$$\therefore Q \propto H^{1/2}$$

Now,

$$\text{Power } (P) = \rho QgH$$

$$P \propto \sqrt{H} \times H$$

$$P \propto H^{3/2}$$

19. (b)

Diameter of Jet = 60 mm

$$\therefore \text{Area} = \frac{\pi}{4} \times (0.06)^2 = 2.827 \times 10^{-3} \text{ m}^2$$

Velocity of Jet = 50 m/s

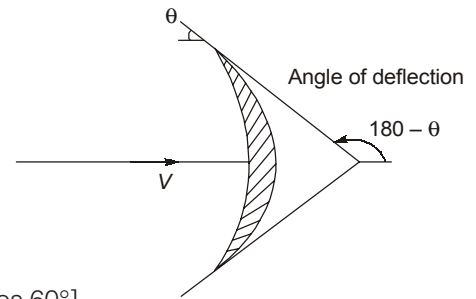
Angle of direction =  $120^\circ$

$$\therefore \theta = 180^\circ - 120^\circ = 60^\circ$$

$$F = \rho a v^2 [1 + \cos \theta]$$

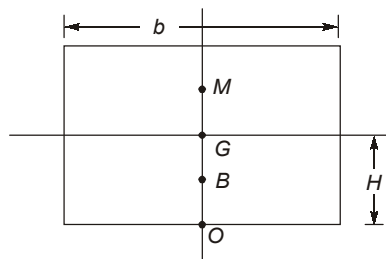
$$F = 1000 \times 2.827 \times 10^{-3} \times 50^2 [1 + \cos 60^\circ]$$

$$F = 10601.25 \text{ N} \quad \text{or} \quad 10.6 \text{ kN}$$



20. (a)

Let  $B$ ,  $G$  and  $M$  be the centre of buoyancy, centre of gravity and meta-centre of the plate.



$$OB = \frac{H}{2}, \quad OG = H$$

$$BG = OG - OB = \frac{H}{2}$$

$$BM = \frac{I}{V} = \frac{Lb^3}{12 \times L \times b \times H} = \frac{b^2}{12H}$$

where,  $L$  = Length of the plate in a direction perpendicular to the plane of the figure.

$$\therefore GM = BM - BG = \frac{b^2}{12H} - \frac{H}{2}$$

For stable equilibrium of plate,  $MG \geq 0$ .

$$\therefore \frac{b^2}{12H} - \frac{H}{2} \geq 0$$

$$\Rightarrow \frac{b}{H} \geq \sqrt{6}$$

$$\Rightarrow H = \sqrt{6}$$

$$\Rightarrow b \geq 6$$

21. (b)

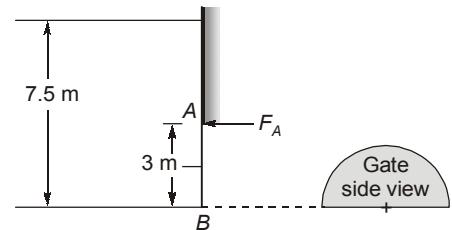
$$F = \rho g A \bar{h}$$

$$\bar{h} = 7.5 - \frac{4R}{3\pi} \Rightarrow 6.226 \text{ m}$$

$$h^* = \frac{I_g}{A\bar{h}} + \bar{h}$$

$$I_g = \frac{\pi}{128} D^4 - \frac{\pi D^2}{8} \times \left(\frac{2D}{3\pi}\right)^2 \Rightarrow 8.8912$$

$$h^* = \frac{8.8912 \times 8}{\pi \times 6^2 \times 6.226} + 6.226 \Rightarrow 6.327$$



Taking moments from point B, we have

$$F_A \times 3 = F \times (7.5 - h^*)$$

$$F_A \times 3 = 1000 \times 9.81 \times \frac{\pi}{2} \times (3)^2 \times 6.226 \times (7.5 - 6.327)$$

$$\Rightarrow F_A = 337611.52 \text{ N}$$

$$F_A = 337.611 \text{ kN} \approx 337.61 \text{ kN}$$

22. (a)

As the Reynolds number,  $Re > 10^5$  (turbulent flow)

$$C_d = \frac{0.074}{(Re_L)^{1/5}}$$

$$F_D = C_d \times \frac{1}{2} \rho V^2 \times A$$

$$\therefore F_D = \frac{0.074}{Re_L^{1/5}} \times \frac{1}{2} \rho V^2 \times L \times b$$

$$F_D = KL^{4/5}$$

Where,  $K$  is a constant

$$\therefore F_{D_1} = KL^{4/5}$$

$$F_{D_2} = K(L + 0.1L)^{4/5}$$

$$\therefore \frac{F_{D_2} - F_{D_1}}{F_{D_1}} = \frac{K(1.1)^{4/5} L^{4/5} - KL^{4/5}}{KL^{4/5}}$$

$$\begin{aligned} \text{\% change in drag force} &= (1.1)^{4/5} - 1 \\ \text{\% change in drag force} &= 0.07923 \times 100 \\ &= 7.923 \% \simeq 8\% \end{aligned}$$

23. (d)

∴ Continuity equation holds,

$$\begin{aligned} \therefore \quad \frac{\pi}{4} \times (5)^2 \times 2 &= \frac{\pi}{4} \times 3^2 \times x \\ x &= 5.55 \text{ m/s} \end{aligned}$$

Mass flow rate

$$\Rightarrow \quad \dot{m} = \int_{\dot{m}} A_1 V_1 = 100 \times \frac{\pi}{4} \times 0.05^2 \times 2 = 3.9269 \text{ kg/s}$$

Let  $F_x$  and  $F_y$  be the force in Right and vertically upward diversion respectively to hold the box in position.

$$\therefore \text{ Now, } \quad \Sigma F_x = 0 \quad \text{[Box is stationary after applying force]}$$

$$-\dot{m} \times V_1 \cos 65^\circ + F_x = -\dot{m} \times V_2 \cos 0^\circ$$

$$-3.9269 \times 2 \times \cos 65^\circ + F_x = -3.9269 \times 5.55 \times 1$$

$$F_x = -18.475 \text{ N.}$$

 $F_x$  must be in left as  $F_x$  comes out to be negative.Similarly for vertical direction  $\Sigma F_y = 0$ 

$$F_y - 3.9269 \times 2 \times \sin 65^\circ = 0$$

$$F_y = 7.11 \text{ N}$$

∴ It is towards vertically upward direction.

24. (a)

$$\text{Break power, } \quad \text{B.P.} = \frac{mgh}{\eta_m} = \frac{80 \times 9.81 \times 30}{0.8} = 29.4 \text{ kW}$$

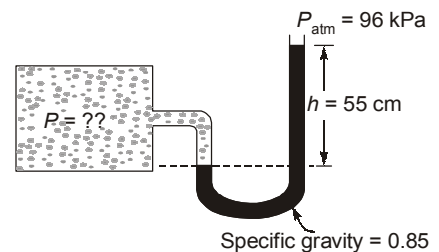
25. (b)

$$P = P_{\text{atm}} + \rho gh$$

$$P = 96 \text{ kPa} + \frac{(850 \times 9.81 \times 0.55)}{1000} \text{ kPa}$$

$$= 96 + 4.586$$

$$= 100.5861 \simeq 100.6 \text{ kPa}$$



26. (c)

The continuity equation is given by

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

$$\text{Now, } \quad \rho = \rho_0 e^{-2t}$$

$$\frac{\partial \rho}{\partial t} = -2\rho_0 e^{-2t} = -2\rho$$

$$\frac{\partial(\rho u)}{\partial x} = 5\rho$$

$$\frac{\partial(\rho v)}{\partial y} = 5\rho$$



$$\frac{\partial(\rho w)}{\partial z} = \lambda \rho$$

$$\therefore -2\rho + 5\rho + 5\rho + \lambda \rho = 0$$

$$8 + \lambda = 0$$

$$\lambda = -8$$

27. (d)

The drag force on the automobile may be given as

$$F_D = C_D A \times \frac{\rho V^2}{2}$$

Here

$$C_D = 0.30,$$

$$A = 2.6 \text{ m}^2$$

$$\rho = 1.2 \text{ kg/m}^3$$

$$V = 120 \text{ kmph}$$

$$\therefore F_D = \frac{0.30 \times 2.6 \times 1.2 \times (120 \times 10^3)^2}{2 \times (60 \times 60)^2}$$

$$F_D = 520 \text{ N}$$

28. (a)

Consider a strip of thickness  $dr$  at a distance  $r$  from centre

$$\therefore \tau = \mu \frac{du}{dy}$$

$$\Rightarrow \tau = \frac{\mu \times r \omega}{h}$$

$$\therefore dF = \tau \cdot dA = \frac{\mu r \omega}{h} \times 2\pi r \cdot dr$$

$$\therefore dT = dF \cdot r \Rightarrow \frac{\mu r \omega}{h} \times 2\pi r \cdot dr \cdot r$$

$\therefore$  On integrating from 0 to  $R$

$$T = \int_0^R dT = \frac{2\mu\pi\omega}{h} \times \int_0^R r^3 \cdot dr$$

$$\Rightarrow = \frac{2\mu\pi\omega \times R^4}{24h} \Rightarrow T = \frac{\mu\pi R^4 \omega}{2h}$$

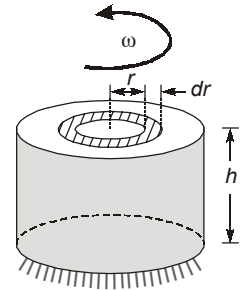
Substituting value

$$\Rightarrow T = \frac{1.6 \times \pi \times 0.1^4 \times 2\pi \times 600}{2 \times 0.001 \times 60} = 15.79 \text{ m}$$

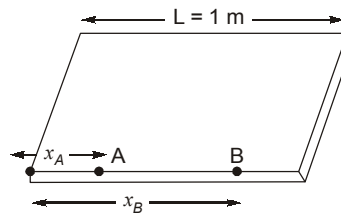
$$P = \frac{2\pi NT}{60}$$

$$\Rightarrow P = \frac{2\pi \times 600 \times 15.79}{60}$$

$$P = 992.114 \text{ W} \approx 992.11 \text{ W}$$



29. (d)



$$\delta \propto \sqrt{x}$$

$$\frac{\delta_B}{\delta_A} = \sqrt{3}$$

Moreover,

$$\frac{\delta_B}{\delta_A} = \sqrt{\frac{x_B}{x_A}} = \sqrt{3}$$

 $\Rightarrow$ 

$$x_B = 3x_A$$

Also,

$$x_B + x_A = 1$$

 $\Rightarrow$ 

$$3x_A + x_A = 1$$

 $\Rightarrow$ 

$$x_A = 0.25$$

 $\Rightarrow$ 

$$x_B = 0.75$$

30. (b)

$$\eta_{\text{Overall}} = \frac{\text{Shaft power}}{gQH}$$

$$Q = \frac{500}{0.53} \times \frac{1}{9.81} \times \frac{1}{30} = 2.0469 \text{ m}^3/\text{s}$$

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