

CLASS TEST

S.No. : 12 GH_ME_J_190919

Thermodynamics



MADE EASY

India's Best Institute for IES, GATE & PSUs

Delhi | Noida | Bhopal | Hyderabad | Jaipur | Lucknow | Indore | Pune | Bhubaneswar | Kolkata | Patna

Web: www.madeeasy.in | E-mail: info@madeeasy.in | Ph: 011-45124612

CLASS TEST 2019-2020

MECHANICAL ENGINEERING

Date of Test : 19/09/2019

ANSWER KEY > Thermodynamics

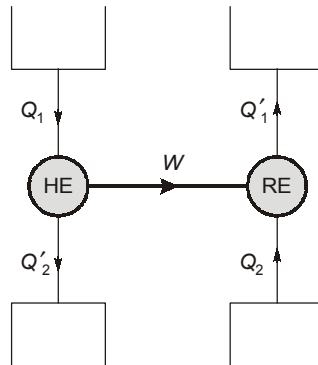
1. (c)	7. (a)	13. (c)	19. (b)	25. (c)
2. (b)	8. (b)	14. (b)	20. (c)	26. (d)
3. (d)	9. (a)	15. (a)	21. (a)	27. (c)
4. (d)	10. (d)	16. (c)	22. (b)	28. (d)
5. (a)	11. (b)	17. (c)	23. (a)	29. (a)
6. (a)	12. (a)	18. (c)	24. (a)	30. (b)

DETAILED EXPLANATIONS

2. (b)

$\int PdV$ work is only valid for a quasi-static process.

3. (d)



$$\frac{W}{Q_1} = \eta_{\text{engine}} = 0.3 \quad \dots(1)$$

$$\frac{Q_2}{W} = \text{COP}_{\text{ref}} = 5 \quad \dots(2)$$

Multiplying equation (1) and (2)

$$\Rightarrow \frac{Q_2}{Q_1} = 0.3 \times 5 = 1.5$$

$$\Rightarrow Q_1 = \frac{Q_2}{1.5} = \frac{1000}{1.5} \text{ kJ} = 666.67 \text{ kJ}$$

4. (d)

The mixture of air and liquid air is not a pure substance, because the relative proportions of oxygen and nitrogen differ in gas and liquid phases in equilibrium.

6. (a)

If temperature is constant, U will remain unchanged as internal energy for an ideal gas is the function of temperature only.

7. (a)

At steady state fluid properties doesn't change with respect to time at any given point.

8. (b)

$$\begin{aligned} \text{Efficiency, } \eta &= \frac{\text{Area } 1-2-3-1}{\text{Area } a-b-1-3-a} = \frac{\frac{1}{2}(T_3 - T_1)(s_1 - s_2)}{\frac{1}{2}(T_3 + T_1)(s_1 - s_2)} = \frac{T_3 - T_1}{T_3 + T_1} \\ &= \frac{600 - 200}{600 + 200} = \frac{400}{800} = 0.5 \end{aligned}$$

11. (b)

Given: $P_C = 20 \text{ kPa}$; $v_C = 0.002 \text{ m}^3/\text{kg}$; $T_C = 300 \text{ K}$

$$\text{We know, } R = \frac{8P_C v_C}{3T_C} = \frac{8 \times 20 \times 1000 \times 0.002}{3 \times 300} = 0.355 \text{ J/kgK}$$

12. (a)

Given; $P = 200 \text{ kN/m}^2$; $W_1 = -150 \text{ kJ}$; $Q = 50 \text{ kJ}$ We know, $H = U + PV$

$$H_1 = U_1 + P_1 V_1$$

$$H_2 = U_2 + P_2 V_2$$

 \therefore Change in enthalpy $\Delta H = H_2 - H_1 = (U_2 - U_1) + P(V_2 - V_1)$

Work done by the system,

$$W_2 = P(V_2 - V_1) = 200 \times (5 - 2) = 600 \text{ kJ}$$

From 1st law of thermodynamics,

$$\Delta Q = \Delta U + \Delta W$$

$$\Delta U = \Delta Q - \Delta W = 50 - (-150 + 600) = 50 - 450 = -400 \text{ kJ}$$

So,

$$\Delta H = \Delta U + P(V_2 - V_1)$$

 \therefore

$$\Delta H = -400 + 200(5 - 2) = -400 + 600 = 200 \text{ kJ}$$

13. (c)

$$c_p = 1 \text{ kJ/kgK}$$

$$c_v = 0.75 \text{ kJ/kgK}$$

$$T = 27^\circ\text{C} = (27 + 273) \text{ K} = 300 \text{ K}$$

$$p = 1 \text{ bar} = 100 \text{ kPa}$$

Gas constant:

$$R = c_p - c_v$$

$$= 1 - 0.75 = 0.25 \text{ kJ/kgK}$$

Applying equation of state in term of density,

$$p = \rho R T$$

$$100 = \rho \times 0.25 \times 300$$

$$1 = 0.75 \rho$$

or

$$\rho = \frac{1}{0.75} = \frac{100}{75} = 1.33 \text{ kg/m}^3$$

14. (b)

Heat loss by $m_1 =$ Heat gained by $m_2 +$ Heat gained by m_3

So,

$$m_1 S(T_1 - T) = m_2 S(T - T_2) + m_3 S(T - T_3)$$

$$m_1 T_1 - m_1 T = m_2 T - m_2 T_2 + m_3 T - m_3 T_3$$

$$T(m_1 + m_2 + m_3) = m_1 T_1 + m_2 T_2 + m_3 T_3$$

 \therefore

$$T = \frac{m_1 T_1 + m_2 T_2 + m_3 T_3}{m_1 + m_2 + m_3}$$

15. (a)

Heat required to melt 1 kg of iron at 15°C to molten metal at $1650^\circ\text{C} =$ Heat required to raise temperature from 15°C to $1535^\circ\text{C} +$ Latent heat $+$ Heat required to raise the temperature from 1535°C to 1650°C .

$$= 0.502 \times [1535 - 15] + 270 + 0.534 [1650 - 1535]$$

$$= 1094.5 \text{ kJ/kg}$$

$$\text{Melting rate} = 5 \times 10^3 \text{ kg/hr}$$

Rate of heat supply required = $1094.5 \times 5 \times 10^3 \text{ kJ/hr}$

$$\text{kW rating of furnace required} = \frac{\text{Heat Rate}}{\text{Furnace Efficiency}} = \frac{1094.5 \times 5 \times 10^3}{0.7} \text{ kJ/hr}$$

$$= \frac{1094.5 \times 5 \times 10^3}{0.7 \times 3600} \text{ kJ/s}$$

$$= 2171.6 \text{ kW} = 2.17 \text{ MW}$$

16. (c)

Maximum work obtainable from a body and TER,

$$W_{\max} = m \left[c_p (T - T_0) + T_0 c_p \ln \left(\frac{T_0}{T} \right) \right]$$

$$= 2 \left[1 \times (600 - 300) + 300 \times 1 \times \ln \left(\frac{300}{600} \right) \right]$$

$$= 184.2 \text{ kJ}$$

17. (c)

$$\frac{P}{P_a} = 100 \times \left(\frac{\rho}{\rho_a} \right)^7 - 99$$

$$\Rightarrow \frac{1}{P_a} \frac{dP}{d\rho} = 7 \times 100 \times \frac{\rho^6}{\rho_a^7}$$

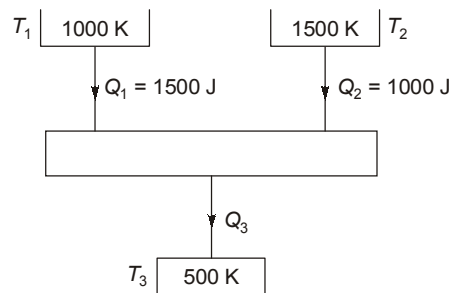
$$\Rightarrow \frac{dP}{d\rho} = 7 \times 100 \times P_a \times \left(\frac{\rho^6}{\rho_a^7} \right)$$

$$\Rightarrow \rho \times \frac{dP}{d\rho} = 7 \times 100 \times P_a \times \left(\frac{\rho}{\rho_a} \right)^7$$

Now, the isothermal bulk modulus (E) is,

$$E = \rho \times \frac{dP}{d\rho} = 7P_a \left[\frac{P}{P_a} + 99 \right]$$

18. (c)



For maximum efficiency, $\Delta S = 0$

$$\Rightarrow \oint \frac{dQ}{T} = 0$$

$$\Rightarrow \Delta S = \sum \frac{Q}{T}$$

$$\Rightarrow 0 = \frac{Q_1}{T_1} + \frac{Q_2}{T_2} - \frac{Q_3}{T_3}$$

$$\Rightarrow 0 = \frac{1500}{1000} + \frac{1000}{1500} - \frac{Q_3}{500}$$

$$\Rightarrow Q_3 = 1083.33 \text{ J}$$

$$\Rightarrow W_{\max} = Q_1 + Q_2 - Q_3 = 1500 + 1000 - 1083.33 = 1416.67 \text{ J}$$

19. (b)

From heat balance,

$$Q_1 + W_{\text{input}} = Q_2$$

$$\Rightarrow Q_1 = Q_2 - W_{\text{input}} = 40 - 10 = 30 \text{ kW}$$

Also, $\oint \frac{dQ}{T} = 0$ [Reversible]

$$\therefore \frac{-Q_1}{T_L} + \frac{Q_2}{T_H} = 0$$

$$\Rightarrow \frac{T_H}{T_L} = \frac{Q_2}{Q_1} = \frac{40}{30} = \frac{4}{3}$$

20. (c)

We know,

$$I = W_{\text{maximum}} - W_{\text{actual}}$$

Now, $W_{\text{maximum}} = \left(1 - \frac{T_2}{1000}\right) \times 500$

$$\therefore 150 = \left(1 - \frac{T_2}{1000}\right) \times 500 - 200$$

$$\Rightarrow 1 - \frac{T_2}{1000} = \frac{350}{500} = 0.7$$

$$\Rightarrow T_2 = (1 - 0.7) \times 1000 = 0.3 \times 1000 = 300 \text{ K}$$

21. (a)

$$(s_2 - s_1) = c_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}$$

$$= 1.005 \ln \frac{400}{290} - 0.287 \ln \frac{350}{140}$$

$$= 0.0602 \text{ kJ/Kg-K}$$

Minimum reversible work input required

$$\begin{aligned} W_{\text{Rev}} &= \Delta h + \Delta KE - T_0 \Delta s \\ &= 110.55 + 3.6 - 280 \times 0.0602 \\ &= 97.29 \text{ kJ/kgK} \end{aligned}$$

Alternate Method

$$W_{\min} = (h_1 - h_2) + \frac{(V_1^2 - V_2^2)}{2} - T_0 (s_1 - s_2)$$

$$= -110.55 - 3.6 + 280 \times 0.0602$$

$$= -97.294 \text{ kJ/kg}$$

$$W_{\min (\text{input})} = 97.294 \text{ kJ/kg}$$

22. (b)

$$\begin{aligned} h_1 &= h_a + x_1(h_b - h_a) \\ \Rightarrow h_1 &= 25 + 0.6(200 - 25) \\ h_1 &= 25 + 105 = 130 \text{ kJ/kg} \end{aligned}$$

As throttling is an isenthalpic process, so

$$\begin{aligned} \Rightarrow h_1 &= h_2 \\ h_2 &= 130 \text{ kJ/kg} \end{aligned}$$

23. (a)

All points as mentioned above may cause irreversibility in a system.

24. (a)

$$\text{As flow work} = pV = 18 \text{ kW}$$

$$\Rightarrow \rho \times \frac{0.6}{60} = 18000 \text{ J/s}$$

$$\text{or } \rho = 18 \text{ bar} = \mathbf{1800 \text{ kPa}}$$

25. (c)

The metal at T_1 K will come in equilibrium with the lake at temperature T_2 K.

$$(\Delta S)_{\text{metal}} = \int_{T_1}^{T_2} \frac{mcdT}{T} = C \ln \frac{T_2}{T_1}$$

$$(\Delta S)_{\text{lake}} = \frac{mgZ}{T_2} + \frac{mc(T_1 - T_2)}{T_2}$$

(As potential energy of block dissipates into internal energy of lake)

$$= \frac{gz}{T_2} + \frac{C(T_1 - T_2)}{T_2}$$

$$\Rightarrow (\Delta S)_{\text{universe}} = \frac{CT_2 \ln \frac{T_2}{T_1} + gz + C(T_1 - T_2)}{T_2}$$

27. (c)

Only one is required to identify the saturation state because in wet region as well as at saturation state both temperature and pressure are dependent property.

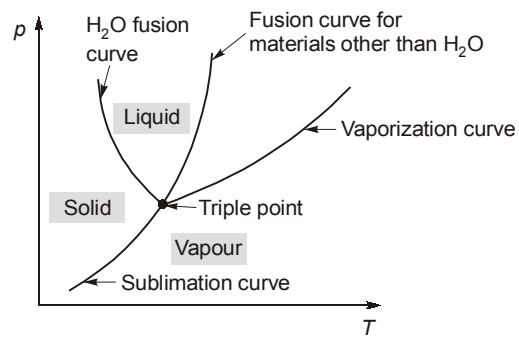
29. (a)

$$\begin{aligned} \text{Initial availability } (A_1) &= Q \left(1 - \frac{T_0}{T_1} \right) \\ &= 400 \left(1 - \frac{300}{1000} \right) = 280 \text{ kJ} \end{aligned}$$

availability when heat supplied at 800K

$$A_2 = 400 \left(1 - \frac{300}{800} \right) = 250 \text{ kJ}$$

30. (b)



- Slope of fusion curve of water is negative.
- Slope of vaporization curve for all materials is positive.

