

**ESE GATE PSUs**

**State Engg. Exams**

**MADE EASY  
workbook 2025**



**Detailed Explanations of  
Try Yourself Questions**

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**Mechanical Engineering**  
**Refrigeration and Air-conditioning**



# 1

## Heat Engine, Heat Pump, Refrigerator & Reversed Carnot Cycle



### Detailed Explanation of Try Yourself Questions

#### T1 : Solution

$$(COP)_{RE} = (COP)_{HP} - 1 = 4 - 1 = 3$$

$$(COP)_{RE} = \frac{\text{Required cooling effect}}{\text{Power input}}$$

$$\Rightarrow \text{Required cooling effect} = 3 \times 3 = 9 \text{ kW} = 9 \times 60 \text{ kJ/min} \\ = 540 \text{ kJ/min}$$

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# 2

## Vapour Compression Refrigeration System



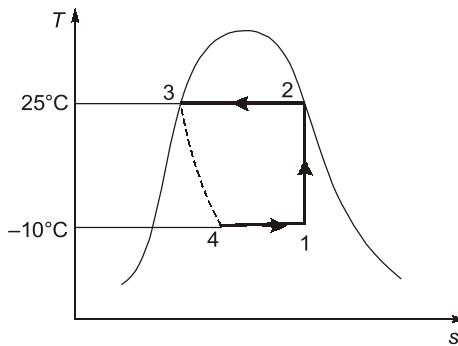
### Detailed Explanation of Try Yourself Questions

#### T1 : Solution

$$h_3 = h_4 = 298.9 \text{ kJ/kg}$$

$$h_2 = h_{g@25^\circ\text{C}} = 1465.84 \text{ kJ/kg}$$

$$\text{COP} = \frac{h_1 - h_4}{h_2 - h_1} \quad \dots(i)$$



Compression process 1-2:

$$s_1 = s_2$$

$$s_f + x s_{fg} = s_2 \quad \left[ s_g = s_f + \frac{h_{fg}}{T} \right]$$

$$0.5443 + x \times \frac{(1433.05 - 135.37)}{263} = 1.1242 + \frac{(1465.84 - 298.9)}{298}$$

$$x = 0.911$$

$$\begin{aligned} h_1 &= h_f + x h_{fg} \\ &= 135.37 + 0.911(1433.05 - 135.37) \end{aligned}$$

$$h_1 = 1317.556 \text{ kJ/kg}$$

From equation (i)  $\text{COP} = \frac{1317.556 - 298.9}{1465.84 - 1317.556} = 6.87$

**T2 : Solution (a)**

Given: Rated capacity = 140.7 kW, Mass flow rate =  $4 \times 10^{-3} \times 10^3 = 4 \text{ kg/sec}$ , Water inlet temperature ( $T_i$ ) = 30°C, Water outlet temperature ( $T_o$ ) = 40°C, Power input to motor = 48 kW, Motor efficiency ( $\eta$ ) = 95%

$$\text{Heat rejected in condenser } (Q_c) = \dot{m}c_w \times (T_o - T_i)$$

$$\begin{aligned} Q_c &= 4 \times 4.1868 \times (40 - 30) \\ &= 167.472 \text{ kW} \end{aligned}$$

Actual refrigeration capacity ( $RC_a$ )

$$\begin{aligned} RC_a &= Q_c - P \times \eta \\ &= 167.472 - 48 \times 0.95 \\ &= 121.872 \text{ kW} = 34.82 \text{ TR} \end{aligned}$$

**T3 : Solution (b)**

Given:  $h_1 = 250 \text{ kJ/kg}$ ,  $h_2 = 300 \text{ kJ/kg}$ ,  $h_{f/\text{evap}} = 50 \text{ kJ/kg}$

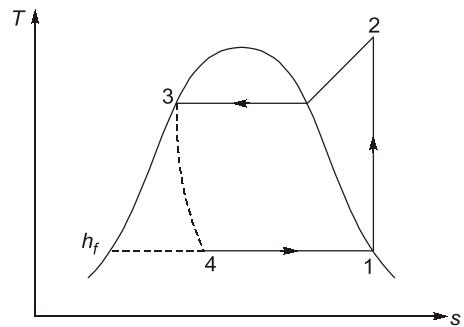
$$\text{COP} = \frac{h_1 - h_4}{h_2 - h_1} - \frac{250 - h_1}{300 - 250}$$

$$h_4 = 100 \text{ kJ/kg}$$

For dryness fraction at point 4,

$$\begin{aligned} h_4 &= h_{f/\text{evap}} + x(h_1 - h_2) \\ 100 &= 50 + x(250 - 50) \end{aligned}$$

$$\text{or, } x = 0.25$$



# 3

## Vapour Absorption Refrigeration System



### Detailed Explanation of Try Yourself Questions

#### T1 : Solution

$$\text{COP} = \frac{T_G - T_0}{T_G} \times \frac{T_R}{T_0 - T_R}$$

$T_R$  = Evapourator Temperature

$T_G$  = Generator Temperature

$T_0$  = Ambient Temperature (condenser temperature)

$$\begin{aligned}\text{COP} &= \frac{360 - 310}{360} \times \frac{260}{310 - 260} \\ &= 0.72\end{aligned}$$

$$0.72 = \frac{T_G - 310}{T_G} \times \frac{250}{310 - 250}$$

$$T_G = 374.9 \text{ K}$$

#### T2 : Solution (b)

- The vapour absorption system uses heat energy to change the condition of the refrigerant from the evaporator. The vapour compression system uses mechanical energy to change the condition of refrigerant from the evaporator.
- The load variation do not affect the performance of a vapour absorption system. The load variations are met by controlling the quantity of steam supplied to the generator. The performance of vapour compression system at partial loads is however, poor.



# 4

## Refrigerants



### Detailed Explanation of Try Yourself Questions

#### T1 : Solution (a)

then,

$$R_{114} = R_{(m-1)(n+1)p}$$

$$m - 1 = 1, m = 2$$

$$n + 1 = 1, n = 0$$

$$p = 4$$

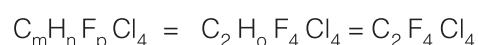
We know,

$$n + p + q = 2m + 2$$

$$0 + 4 + q = 2 \times 2 + 2$$

$$q = 2$$

So, the formula is



# 5

# Refrigeration Equipment & Gas Refrigeration



**Detailed Explanation  
of  
Try Yourself Questions**

## T1 : Solution (b)

- Gas cycle refrigeration is used in aircraft.

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# 6

## Air-conditioning



### Detailed Explanation of Try Yourself Questions

#### T1 : Solution

$$P_{atm} = 1 \text{ bar} = 100 \text{ kPa}$$

$$\text{DBT} = 30^\circ\text{C}$$

$$\phi = 70\% = 0.7$$

$$P_{vs} = 4.25 \text{ kPa}$$

Specific humidity,  $\omega$  = ?

$$\phi = \frac{P_v}{P_{vs}}$$

$$0.7 = \frac{P_v}{4.25}$$

$$P_v = 2.975 \text{ kPa}$$

Specific humidity,

$$\begin{aligned}\omega &= 0.622 \times \frac{P_v}{P - P_v} = 0.622 \times \frac{2.975}{100 - 2.975} \\ &= 0.0191 \frac{\text{kg water vapour}}{\text{kg dry air}}\end{aligned}$$

#### T2 : Solution

$$\text{Wet bulb depression at the inlet} = (t_{db} - t_{wb})_{\text{inlet}} = (38 - 18)_{\text{inlet}} = 20^\circ\text{C}$$

$$\text{Wet bulb depression at the outlet} = (24 - 18) = 6^\circ\text{C}$$

( $\because t_{wb \text{ inlet}} = t_{wb \text{ exit}}$ )

$$\text{Percentage change} = \frac{20 - 6}{20} = 70\%$$

**T3 : Solution**

In cooling tower:

We know,

$$\text{Approach} = T_{c2} - T_{WB}$$

$$\text{Range} = T_{c1} - T_{c2}$$

$$\text{Wet bulb depression} = T_{DB} - T_{WB}$$

Where,

$T_{c2}$  : Cooling water exit temperature

$T_{WB}$  : Wet bulb temperature of air

$T_{DB}$  : Dry bulb temperature of air

$T_{c1}$  : Incoming warm water temperature

As given in question,

$$W_{BD} = A + R$$

$$T_{DB} - T_{WB} = T_{c2} - T_{WB} + T_{c1} - T_{c2}$$

$$\text{or, } T_{c1} - T_{DB} = 0$$

